

Behavior of Bromotrifluoropropene and Pentafluoroethane When Subjected to a Simulated Aerosol Can Explosion

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16. Abstract This technical note presents the data from simulated aerosol can explosion tests while using bromotrifluoropropene (BTP) and pentafluoroethane (HFC-125) as fire suppression agents for aircraft cargo compartments. These explosion tests were conducted at below inert volumetric concentrations to determine the agent's explosion attenuation performance. The tests were conducted inside a 402-ft ³ pressure vessel. The collected data showed that BTP and HFC-125, at these below inert concentrations, enhanced the explosion (acted as fuel) instead of mitigating it.					
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TABLE OF CONTENTS

	Page
EXECUTIVE SUMMARY	v
INTRODUCTION	1
Agent	1
Environmental	1
Toxicology	1
Technical Approach	1
Pressure Vessel	1
Instrumentation	2
Test Procedure	2
RESULTS	3
CONCLUDING REMARKS	5

LIST OF FIGURES

Figure		Page
1	Plan View of Pressure Vessel Setup	6
2	Comparison of Agent Explosion Suppression Capability at Below Inert Concentrations	6
3	Gas and Temperature Traces for Test 2	7
4	The BTP Pressure Pulse at 2.5% (Test 2)	7
5	Gas and Temperature Traces for Test 3	8
6	No Agent Pressure Pulse (Test 3)	8
7	Gas and Temperature Traces for Test 4	9
8	No Agent Pressure Pulse (Test 4)	9
9	Gas and Temperature Traces for Test 5	10
10	The BTP Pressure Pulse at 3.0% (Test 5)	10

11	Gas and Temperature Traces for Test 6	11
12	The BTP Pressure Pulse at 4.0% (Test 6)	11
13	Gas and Temperature Traces for Test 9	12
14	The BTP Pressure Pulse at 5.0% (Test 9)	12
15	Gas and Temperature Traces for Test 13	13
16	The BTP Pressure Pulse at 6.0% (Test 13)	13
17	Gas and Temperature Traces for Test 16	14
18	The Halon 1301 Pressure Pulse at 2.5% (Test 16)	14
19	Gas and Temperature Traces for Test 17	15
20	The HFC-125 Pressure Pulse at 8.9% (Test 17)	15
21	Gas and Temperature Traces for Test 19	16
22	The HFC-125 Pressure Pulse at 11.0% (Test 19)	16
23	Gas and Temperature Traces for Test 23	17
24	The HFC-125 Pressure Pulse at 6.2% (Test 23)	17
25	Gas and Temperature Traces for Test 25	18
26	The HFC-125 ($P_o=15$ psig) Pressure Pulse at 11.3% (Test 25)	18

LIST OF TABLES

Table	Page
1 Summary of Test Results	19

EXECUTIVE SUMMARY

This technical note presents the results of simulated aerosol can explosion tests conducted to evaluate the explosion suppression performance of bromotrifluoropropene (BTP) and pentafluoroethane (HFC-125). BTP was selected by members of the International Aircraft Systems Fire Protection Working Group as a possible candidate to replace Halon 1301 as the suppression agent used in an aircraft cargo compartment. Since HFC-125 is an acceptable halon replacement agent for some applications, the explosion suppression performance of this agent was also investigated.

The simulated aerosol can explosion test is one of four fire test scenarios required by the Federal Aviation Administration (FAA's) Minimum Performance Standard for Aircraft Cargo Compartment Halon Replacement Fire Suppression Systems (DOT/FAA/AR-TN03/6). Before running this particular minimum performance standard (MPS) test with BTP in the required 2000 ft³ aircraft cargo compartment, a preliminary test series was conducted at the FAA William J. Hughes Technical Center Pressure Fire Modeling Facility. The objective of this test series was to determine if BTP had any unusual behavior before proceeding to conduct the required MPS tests inside the FAA's 2000 ft³ aircraft cargo compartment.

Baseline tests were conducted to establish a comparison benchmark. These baseline tests were conducted by letting the simulated aerosol can explode without the presence of a suppression agent. The results showed overpressures between 23 and 25 psig. A second benchmark test was conducted using 2.5% volumetric concentration Halon 1301, which is below its inerting concentration. At this volumetric concentration, a subdued explosion event occurred, resulting in an overpressure of 4 psig.

The reported inert concentration of BTP, when evaluated against propane, is 8.5% volumetric concentration. It was decided by the testing team that the initial agent volumetric concentrations should be below this reported number to determine if BTP would be as effective as Halon 1301 in this particular test scenario. Testing at the FAA Technical Center has shown that Halon 1301 is capable of suppressing this particular propane explosion with as little as 3.1% volumetric concentration (The published inert concentration value for Halon 1301 is 6.7% at stoichiometric fuel (propane) to air ratio). The initial volumetric concentration selected for the first explosion test was 2.5% BTP. This first explosion test resulted in an estimated overpressure of 49.3 psig (pressure transducer was saturated). After replacing the pressure transducer, other tests were conducted that included 3%, 4%, 5%, and 6% volumetric concentrations. Their associated overpressures were 63, 63, 100, 93 psig, respectively. Thus, BTP enhanced the explosion event (as much as 4 times greater pressures than the unsuppressed event and 23 times greater than the Halon 1301 benchmark concentration).

After experiencing the BTP explosion events, HFC-125 was evaluated to determine if it would behave in the same fashion. HFC-125 also enhanced the explosion event when it was below its inert concentration (15.6%). The agent produced explosion overpressures of 53 psig, at 9% and 11%, respectively. When the pressure vessel was pressurized with air to 15 psig and sustained a volumetric concentration of 11.3% HFC-125, a reduced explosion event of 6 psig occurred. Prior to activating the simulated aerosol can, the arc-producing electrodes were energized to

determine if an explosive mixture was present at this particular vessel pressure and HFC-125 concentration. The results were negative. This type of test was repeated at an internal vessel pressure of 20 psig and a volumetric concentration of 6.3%; once again, the results were negative (no event). Another test was conducted with 13.5% of HFC-125 at ambient pressure, but there was no explosion event after the simulated aerosol can was activated. Thus, HFC-125 prevented the blast at 13.5%, even though its reported inert concentration for a propane explosion is 15.6% (at a stoichiometric fuel-to-air ratio).

In summary, at concentrations below the inerting level, both BTP and HFC-125 enhanced explosions by creating higher overpressures than measured in air alone. In contrast, Halon 1301, the currently used aircraft cargo compartment fire suppression agent, mitigated the explosion, even though it was below its inert concentration. It reduced the overpressure of the event. Since aircraft cargo compartment suppression agents may be present at subinerting design concentrations, because of stratification or larger than normal leakage, it is important that replacement agents be selected that do not increase the overpressure caused by an exploding aerosol can at concentrations below the inerting value.

Aircraft cargo compartment fire suppression agents may be present at subinerting concentrations due to leakage of agent from the bottle or delivery tubing, or stratification, or larger than normal air leakage in the compartment. Therefore, it is important that replacement agents be selected that do not increase the overpressure caused by an exploding aerosol can at concentrations below the inerting value. Unless a means can be found to avoid the problem of subinerting concentrations of extinguishing agent, BTP and HFC-125 would not be suitable candidates for halon replacement extinguishing agents in the cargo compartment.

INTRODUCTION

The objective of this project was to determine the explosion suppression performance of bromotrifluoropropene (BTP) and pentafluoroethane (HFC-125) at concentrations below the inerting level when challenged against the simulated aerosol can explosion test.

AGENT.

The agents used during the tests were BTP and HFC-125. According to the BTP Material Safety Data Sheet (MSDS), this chemically acting agent is a colorless volatile liquid that has a slight ether-like odor. It has a boiling point of 93°F, a liquid density of 99.9 lb/ft³ (1.60 kg/l) at 77°F, and a molecular weight of 174.95. The HFC-125 MSDS describes this agent as clear, colorless, having a boiling point of -55°F, a liquid density of 77.9 lbm/ft³ (1.248 g/cc) at 68°F, and a molecular weight of 120.

ENVIRONMENTAL.

At the time of this testing, bromotrifluoropropene (CH₂BrCF₃) was not on the Environmental Protection Agency (EPA), Clean Air Act, Significant New Alternatives Policy (SNAP) program, or other international governmental-approving program list as a Halon 1301 replacement. However, laboratory work has been conducted to determine the primary environmental characteristics of this new agent. For example, it was determined that the agent has an ozone depletion potential (ODP) of 0.0028, no global warming potential (GWP) reported yet, and has an atmospheric lifetime (ALT) of 0.008 year, or 2.9 days. As a reference, the values for Halon 1301 (CF₃Br) are 16 ODP, 5800 GWP, and 100 years ALT. On the other hand, HFC-125 (CF₃CHF₂) is on the EPA SNAP list. It has an ODP of 0, a GWP of 3800, and an ALT of 32.6 years.

TOXICOLOGY.

The only toxicology data reported in the BTP MSDS was its lethal concentration or LC₅₀. The LC₅₀ is determined by exposing (inhalation) rats to the agent for 4 hours. The LC₅₀ reported, for a 4-hour exposure, was estimated to be within the range of 5.1% to 9.7% volume. The fire suppression concentration of BTP is also within that range. For HFC-125, the MSDS indicates the LC₅₀ as 709,000 ppm for 4 hours. The lowest observed adverse effect level (LOAEL) reported was 100,000 ppm, and the no observed adverse effect level (NOAEL) was 50,000 ppm.

TECHNICAL APPROACH.

PRESSURE VESSEL. The tests were conducted with an exploding aerosol can simulator that was developed by the Federal Aviation Administration (FAA) to simulate the worst-case effects of an exploding aerosol can in a repeatable manner. The simulator was housed in a pressure vessel located in the Pressure Fire Modeling Facility at the FAA William J. Hughes Technical Center. The pressure vessel has a volume of 402 ft³ and a maximum working pressure rating of 600 psig (see figure 1). The pressure vessel was instrumented with thermocouples, pressure transducers, gas analyzers, and a video camera. Since the pressure vessel is air tight, the

overpressure associated with the explosive reaction is captured and retained until the pressure vessel cools.

INSTRUMENTATION. Multiple sensors were installed inside the pressure vessel during the evaluation, which included thermocouples, gas sampling probes, pressure transducers, and a video camera (see figure 1).

Temperature was measured with two Type K chromel/alumel 22-gauge thermocouples near the arcing electrodes and on the surface of the simulator.

Two gas analyzers, with a continuous real-time display, were used to measure the volumetric concentrations of the extinguishing agent (BTP or HFC-125) and oxygen (O₂). A comparative test between the signal output (concentration reading) of the NDIR and Statham analyzers were conducted prior to testing to determine their correlation. The results were excellent; their readings match almost exactly ($\pm 0.1\%$).

- A Rosemount 880A (NDIR) analyzer was used to determine the volumetric concentration of BTP and HFC-125.
- The oxygen concentration was detected with a Rosemount OM11EA gas analyzer.

The gas-sampling probe was installed 24 inches laterally to the arcing electrode and 36 inches forward of the simulator. The sampling probe simultaneously disconnected just before striking the arc to protect the analyzing equipment from the overpressures.

The data-sampling rate for all the temperature measurements and the gas concentrations was 1 Hz.

An Omega PX951-200G5V pressure transducer was used to record the overpressure pulses during the explosions. The pressure transducer's frequency response was 3000 Hz, and it provided a pressure range of 0 to 200 psig. The pressure transducer was mounted on the aft wall of the pressure vessel. The pressure data was collected at a sampling rate of 1000 data points per second.

TEST PROCEDURE. The following procedures were used during the simulated aerosol can explosion test.

1. Prior to commencing the test, the analyzers were calibrated against a calibration gas, the instrumentation was checked for functionality and accuracy, and the support equipment was activated to check for normal operation.
2. To identify the test, a test sign, with the test identification number, was displayed in front of the video camera and recorded.
3. The data acquisition systems were configured and readied.

4. The fire bottle was filled with the required amount of agent, and the aerosol can simulator was charged with propane, water, and alcohol.
5. The pressure vessel door was shut after plumbing the fire bottle to the pressure vessel's discharge lines, after cleaning the discharge nozzles, and after mounting the aerosol can simulator inside the vessel.
6. All the valves on the pressure vessel were closed to seal it, with the gas-sampling probe creating the only temporary leak. At this point, the setup was ready for testing.
7. Before the countdown, the fan inside the pressure vessel was turned on.
8. After the countdown, the test was initiated by starting the 1-Hz data acquisition system and discharging the agent. The agent was introduced, either at a low or high rate of discharge, in the pressure vessel until the desired volumetric concentration was reached.
9. Once the desired concentration was reached, the aerosol can simulator was heated to increase its pressure to 240 psig, which is the design failure pressure of a DOT-2P aerosol can.
10. When the required pressure was achieved, a second countdown was initiated to activate the aerosol can simulator. During the second countdown, the video camera was started, the high-speed data acquisition was tripped, the fan was turned off, the arcing electrodes were energized, and the aerosol can simulator pneumatic valve was opened.
11. After the test, the data was saved, all the equipment was turned off (with the exception of video camera), and the pressure vessel ventilated and monitored.

Two tests were conducted to determine if a reaction would occur with the agents under pressure. In these tests, the pressure vessel was pressurized to 15 and 20 psig. The pressurization step was performed after the agent was discharged. To pressurize the vessel, the air service valve was opened until the required pressure was achieved. After that, the same steps were followed as described above.

RESULTS

Table 1 presents a summary of the test results and figure 2 shows a comparison of representative data of each agent's explosion suppression capabilities. A total of 25 tests were conducted in the pressure vessel. Out of the 25 tests, 21 were conducted successfully and 4 tests had to be aborted due to equipment failure (tests 7, 11, 12, and 18). The explosion event stressed the equipment and sometimes destroyed it.

Test 1 was a pre-explosion test that compared the output of the NDIR and Statham gas analyzers, when measuring BTP, using two different methods of creating calibration gas. The agreement between the outputs of these two gas-measuring devices and the two calibration gas production methods were excellent. Since one of the methods used to produce the calibration gas is proprietary information, they are not discussed in this report.

Test 2 was the first simulated aerosol can explosion test, using a concentration of 2.5% BTP in the pressure vessel. An explosion event occurred and produced a peak temperature of 368°F (figure 3) and an overpressure in excess of 49.3 psig (figure 4). Since the pressure transducer was saturated, it was replaced with one rated for higher pressures (200 psig).

Tests 3 and 4 were baseline explosion tests without any extinguishing agent present. Test 3 was an explosion event with a peak temperature of 387°F (figure 5) and an overpressure of 25.4 psig (figure 6). The explosion of test 4 gave a peak temperatures of 328°F (figure 7) and an overpressure of 23.4 psig (figure 8).

Tests 5 through 13 were simulated aerosol can explosion tests using BTP volumetric concentrations of 3%, 4%, 5%, and 6%. At these concentrations, the resulting peak pressures were 63, 63, 100, and 93 psig, respectively. As observed at 2.5% BTP concentration, the overpressures were significantly higher than the overpressure measured in air without the presence of an extinguishing agent (23-25 psig). The associated peak temperatures were 1056°, 1095°, 1251°, and 1467°F, respectively (see figures 9 through 16). Test 12 experienced a partial explosion event at 6% BTP. There were some flames near the ceiling area, but no significant trace of elevated pressure or temperature. During this test, the arc-producing electrodes were placed 2 inches below their required normal position.

Tests 14 and 15 were studies conducted to determine if the heat gun, used to heat up the aerosol can simulator, was influencing the volumetric concentration of the BTP. The heat gun was replaced for tests conducted after test 8. On previous tests, it was noticed that when the heat gun was turned on to increase the pressure in the aerosol can simulator, the concentration of BTP dropped. These tests showed that the heat gun did not affect the concentration of the agent after running it for 10 and 30 minutes. Nevertheless, it was replaced with heat tape.

Test 16 used Halon 1301 as the extinguishing agent with a volumetric concentration of 2.5%. This low concentration demonstrated that even though the agent was below its inert concentration (6.7%), the agent was still able to attenuate the explosion pulse. The pressure transducer recorded an overpressure of 4 psig with a temperature of 65°F (see figures 17 and 18). Thus, unlike BTP, Halon 1301 reduces the overpressure caused by an exploding aerosol can at concentrations below the inerting level.

Tests 17 through 25 were conducted with HFC-125. In tests 21, 22, 23, and 25, the internal pressure of the pressure vessel was increased to determine if the agent was explosive without the activation of the aerosol can simulator. The internal pressure of the pressure vessel was increased by injecting compressed air. The concentrations tested at ambient pressure were 6.2%, 8.9%, 11%, and 13.5%. When the internal pressure of the pressure vessel was increased, the concentrations were 6.1%, 6.3%, and 11.3%. The internal pressure of the pressure vessel was increased to 15 and 20 psig. The explosion event peak pressures recorded, when the pressure vessel was at ambient pressure, were 52, 53, 52, and 0 psig, respectively, with associated temperatures of 1026°, 1227°, 1067°, and 50°F. Thus, concentrations of HFC-125 below the inerting level (6.2%, 8.9%, and 11%) also produced overpressures greater than in air alone. No explosion occurred when the concentration was 13.5%. During test 24, the internal pressure of the pressure vessel was increased to 15 psig. When the concentration of HFC-125 was 11.3%,

the arcing electrodes were energized without the activation of the aerosol can simulator. At this time, there was no explosion event, but when the aerosol can simulator was activated, a minor explosion event occurred with the pressure increase of only 6 psig. The peak temperature during this event was 32°F (up from 24°F). When the internal pressure of the pressure vessel was increased to 20 psig and the HFC-125 concentrations (6.1%) was below the cup burner concentrations (8.8%), energizing the arc-producing electrodes produced no explosions. (Refer to the charts in figures 19 through 26.)

CONCLUDING REMARKS

The following conclusions can be inferred from the results presented in this report.

1. The overpressure pulse of the explosion event is enhanced significantly when bromotrifluoropropene (BTP) is used at a subinerting concentration of 6% or below.
2. The overpressure pulse of the explosion event is enhanced significantly when pentafluoroethane (HFC-125) is used at a subinerting concentration of 11% or below.
3. Halon 1301 mitigated the pressure pulse of an aerosol explosion at a concentration of 2.5% which is below its inert value.
4. Unless a means can be found to avoid the problem of introducing subinerting concentrations of extinguishing agent in the cargo compartment, BTP and HFC-125 would not be suitable candidates for halon replacement extinguishing agents for this application in airplanes.
5. When the internal pressure of the pressure vessel is increased to 15 and 20 psig and HFC-125 is present in concentrations of 6.1% and 11.3%, the environment is not explosive when an electrical arc is introduced.
6. The agreement between the gas-sampling readout of the NDIR and Statham gas analyzers and between the two methods used to produce calibration gas were excellent.

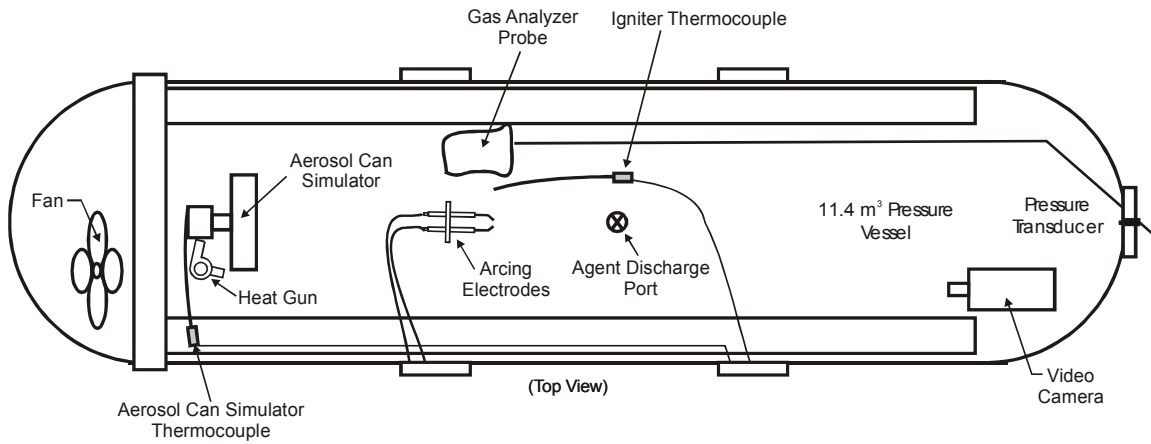


FIGURE 1. PLAN VIEW OF PRESSURE VESSEL SETUP

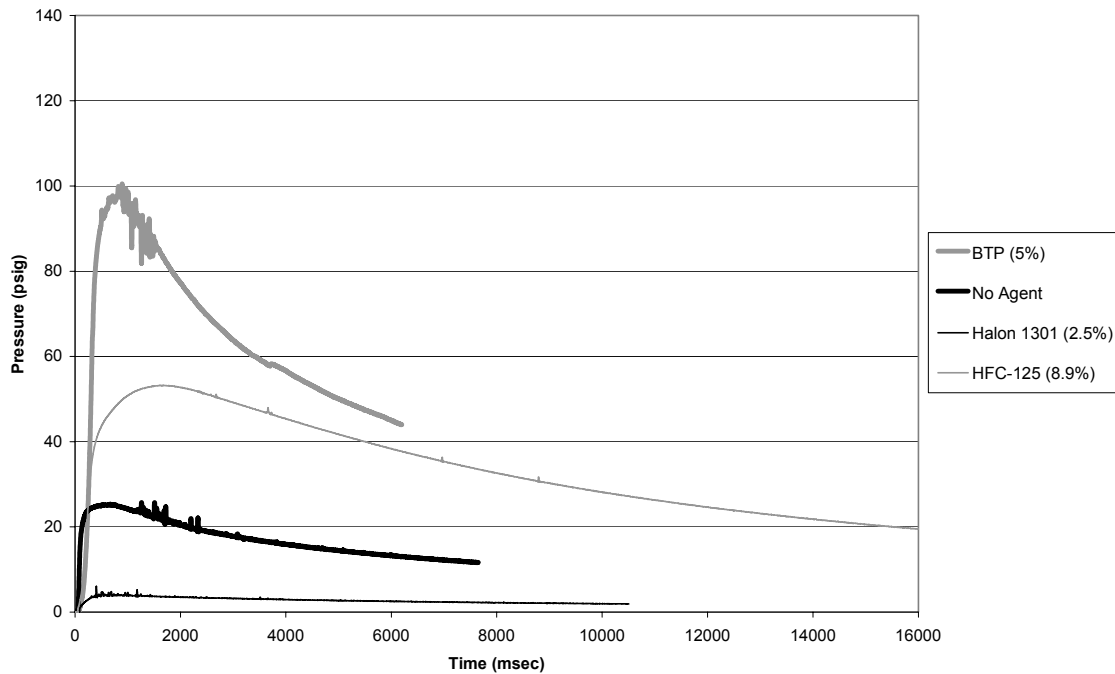


FIGURE 2. COMPARISON OF AGENT EXPLOSION SUPPRESSION CAPABILITY AT BELOW INERT CONCENTRATIONS

AEROSOL CAN SIMULATOR EXPLOSION TESTS 112503T1
Concentration: 2.5% BTP

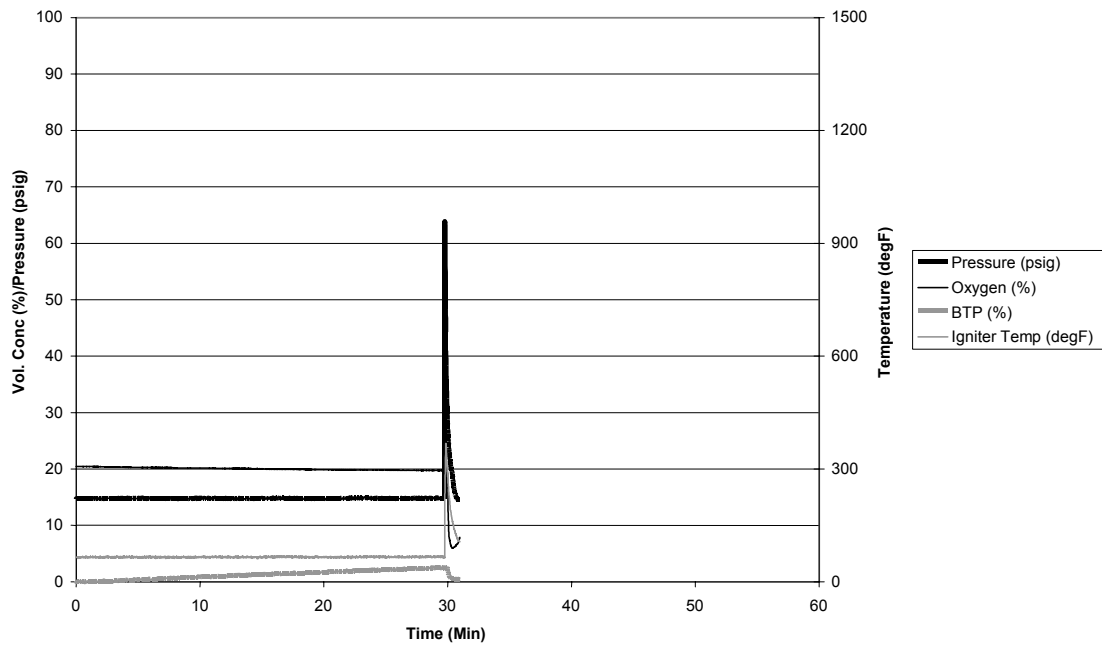


FIGURE 3. GAS AND TEMPERATURE TRACES FOR TEST 2

AEROSOL CAN SIMULATOR EXPLOSION TEST 112503T1
Concentration: 2.5% BTP

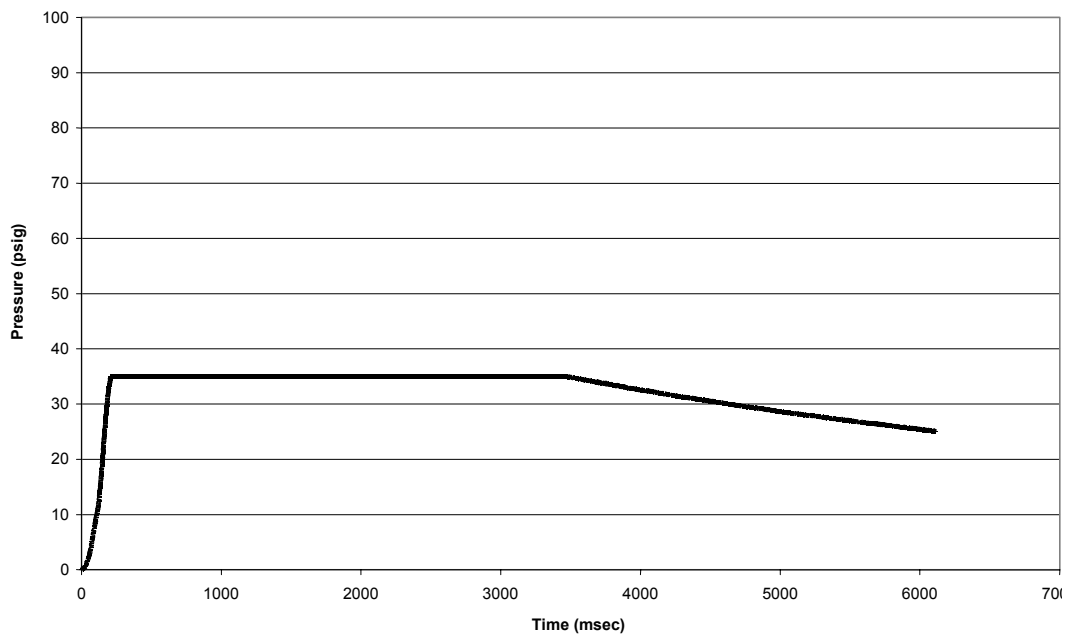


FIGURE 4. THE BTP PRESSURE PULSE AT 2.5% (TEST 2)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 120203T1
Concentration: No Agent

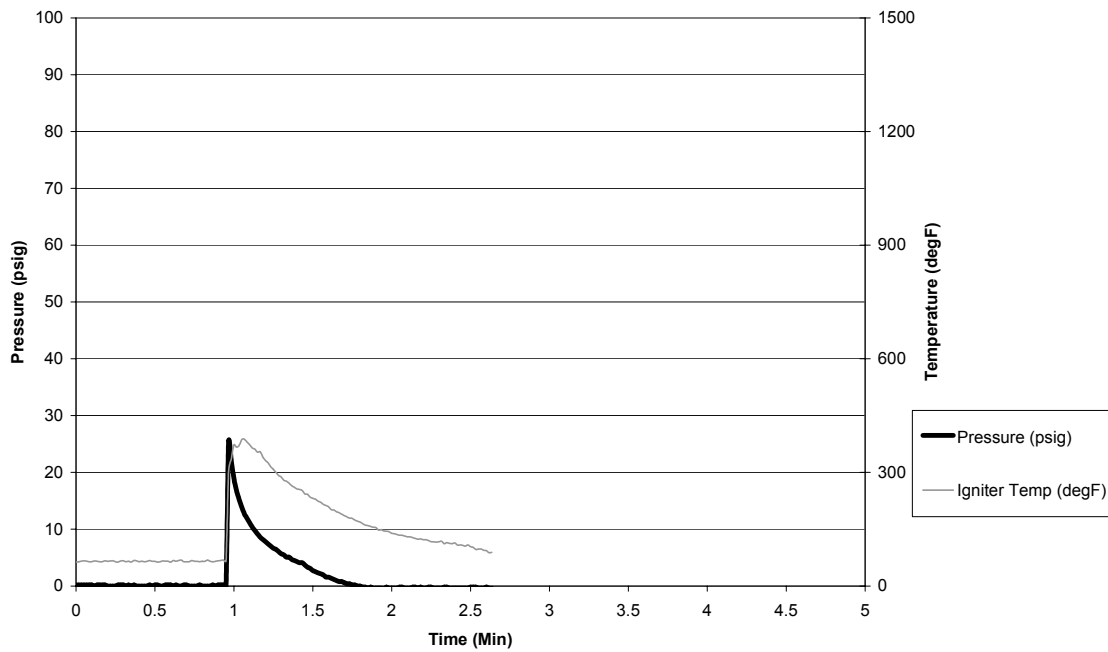


FIGURE 5. GAS AND TEMPERATURE TRACES FOR TEST 3

AEROSOL CAN SIMULATOR EXPLOSION TEST 120203T1
Concentration: No Agent

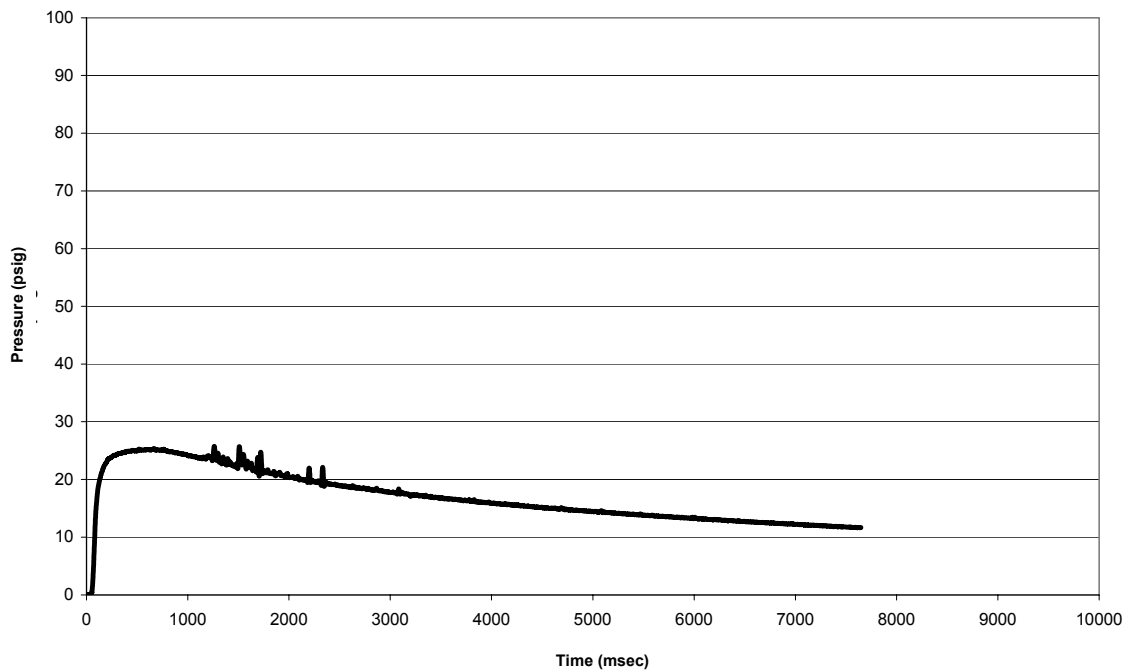


FIGURE 6. NO AGENT PRESSURE PULSE (TEST 3)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 120203T2
Concentration: No Agent

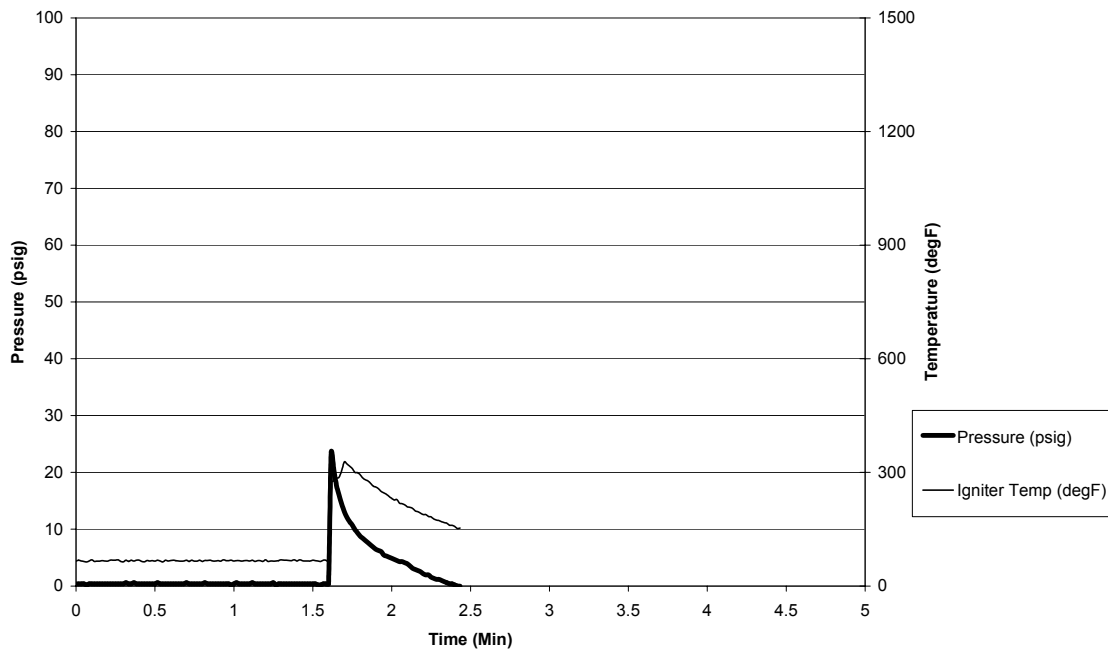


FIGURE 7. GAS AND TEMPERATURE TRACES FOR TEST 4

AEROSOL CAN SIMULATOR EXPLOSION TEST 120203T2
Concentration: No Agent

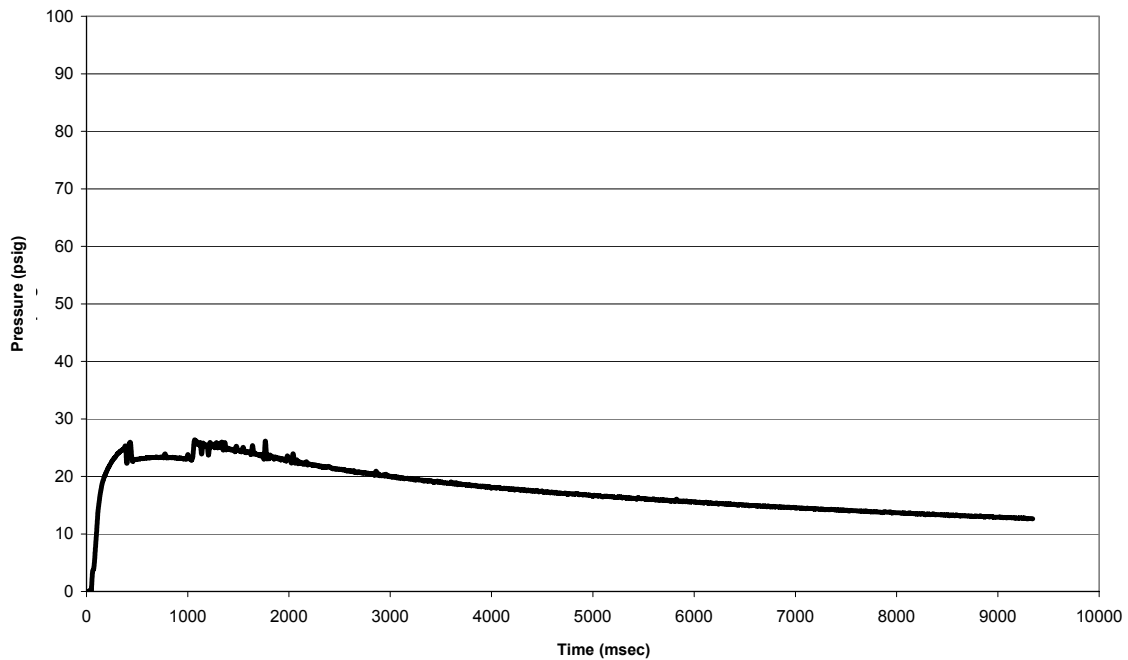


FIGURE 8. NO AGENT PRESSURE PULSE (TEST 4)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 120203T3
Concentration: 3% BTP

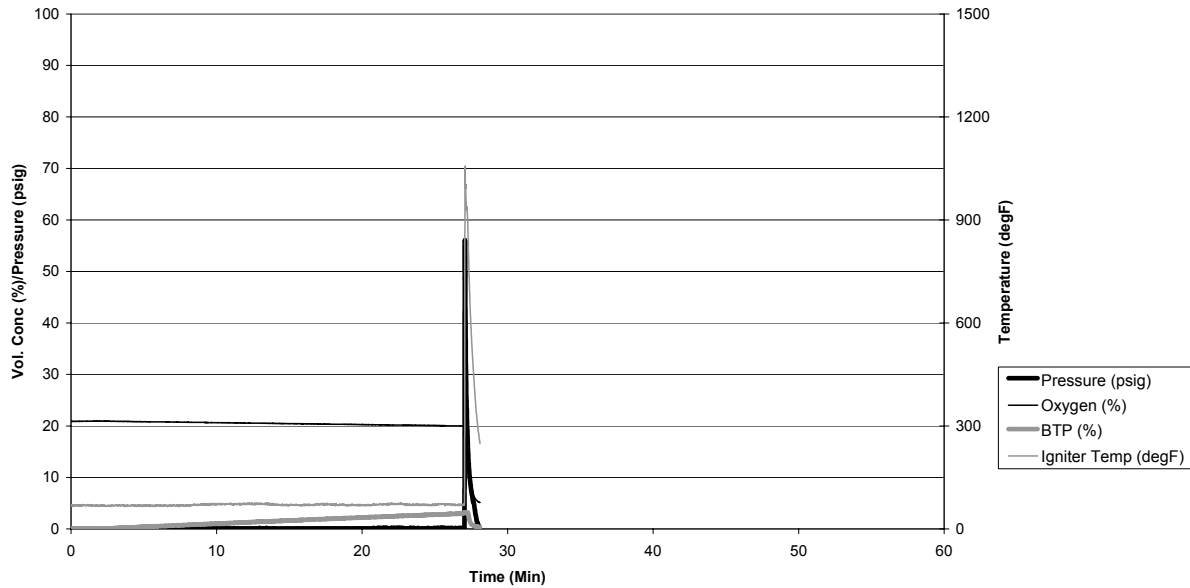


FIGURE 9. GAS AND TEMPERATURE TRACES FOR TEST 5

AEROSOL CAN SIMULATOR EXPLOSION TEST 120203T3
Concentration: 3% BTP

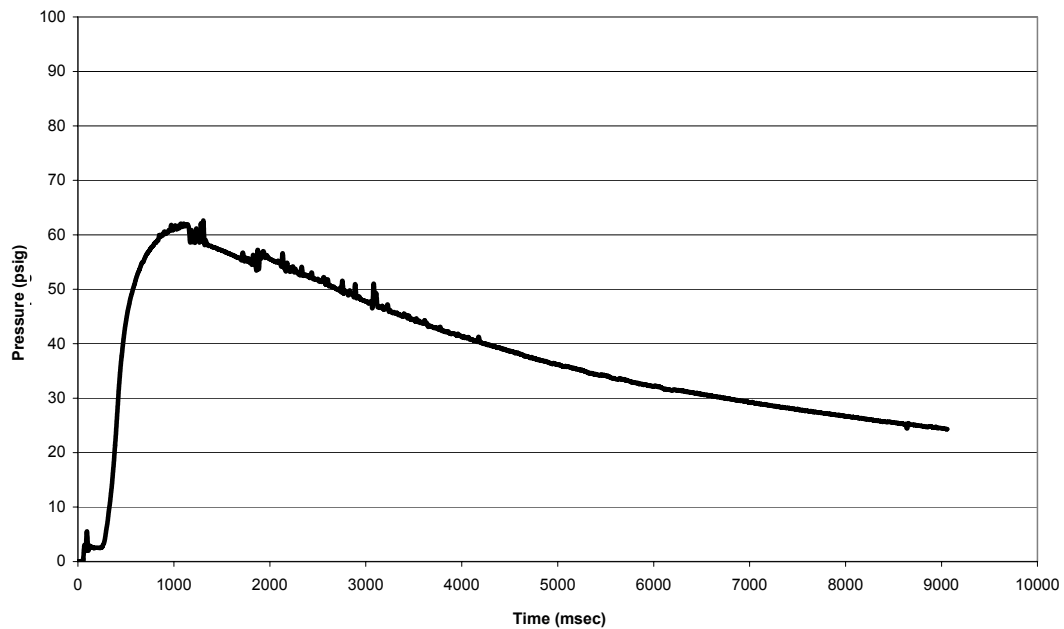


FIGURE 10. THE BTP PRESSURE PULSE AT 3.0% (TEST 5)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 120303T1
Concentration: 4% BTP

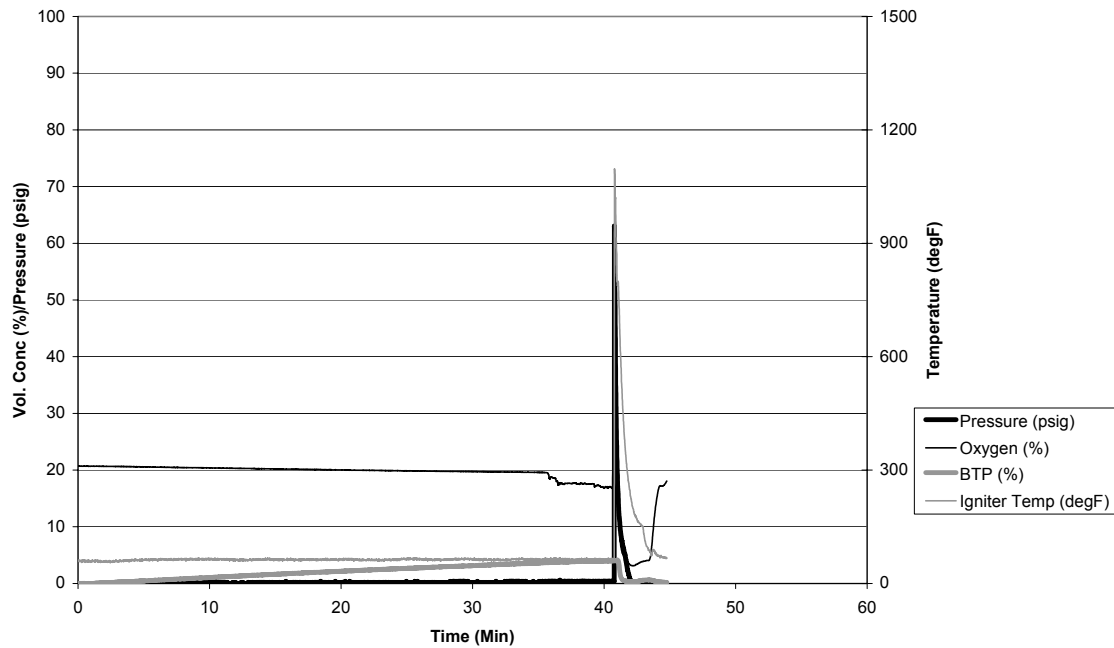


FIGURE 11. GAS AND TEMPERATURE TRACES FOR TEST 6

AEROSOL CAN SIMULATOR EXPLOSION TEST 120303T1
Concentration: 4% BTP

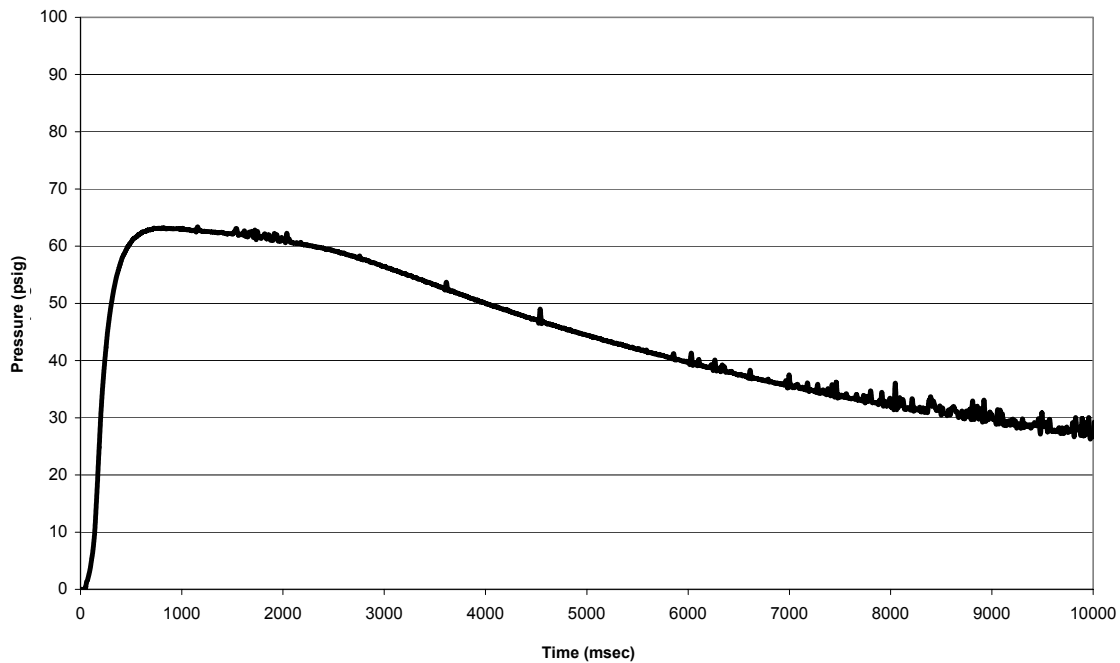


FIGURE 12. THE BTP PRESSURE PULSE AT 4.0% (TEST 6)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 120803T1
Concentration: 5% BTP

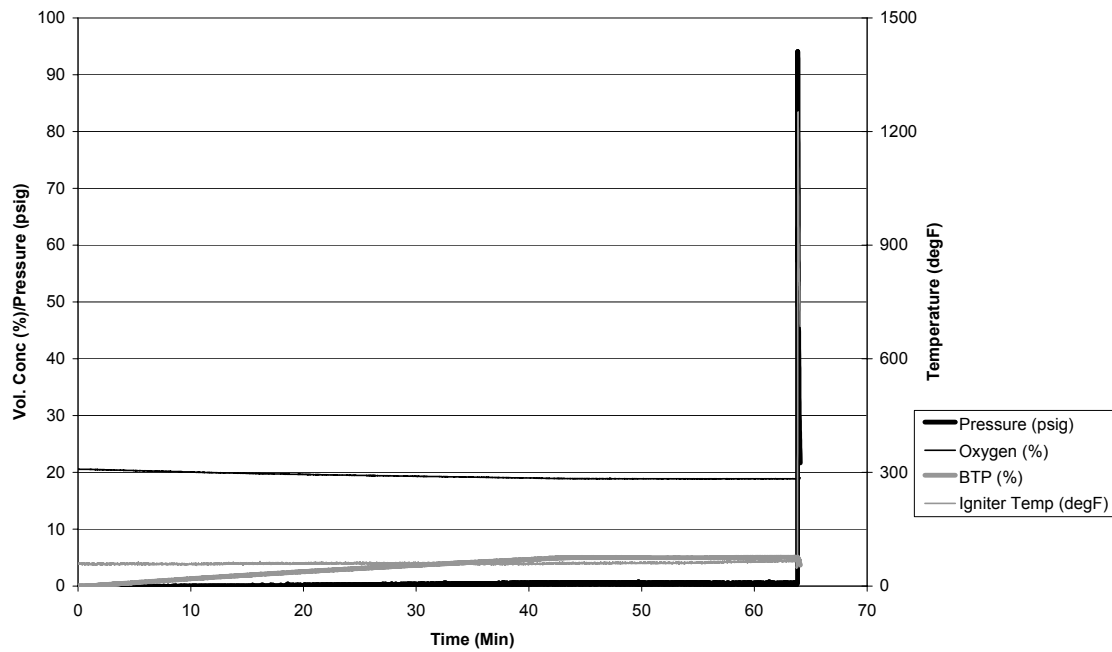


FIGURE 13. GAS AND TEMPERATURE TRACES FOR TEST 9

AEROSOL CAN SIMULATOR EXPLOSION TEST 120803T1
Concentration: 5% BTP

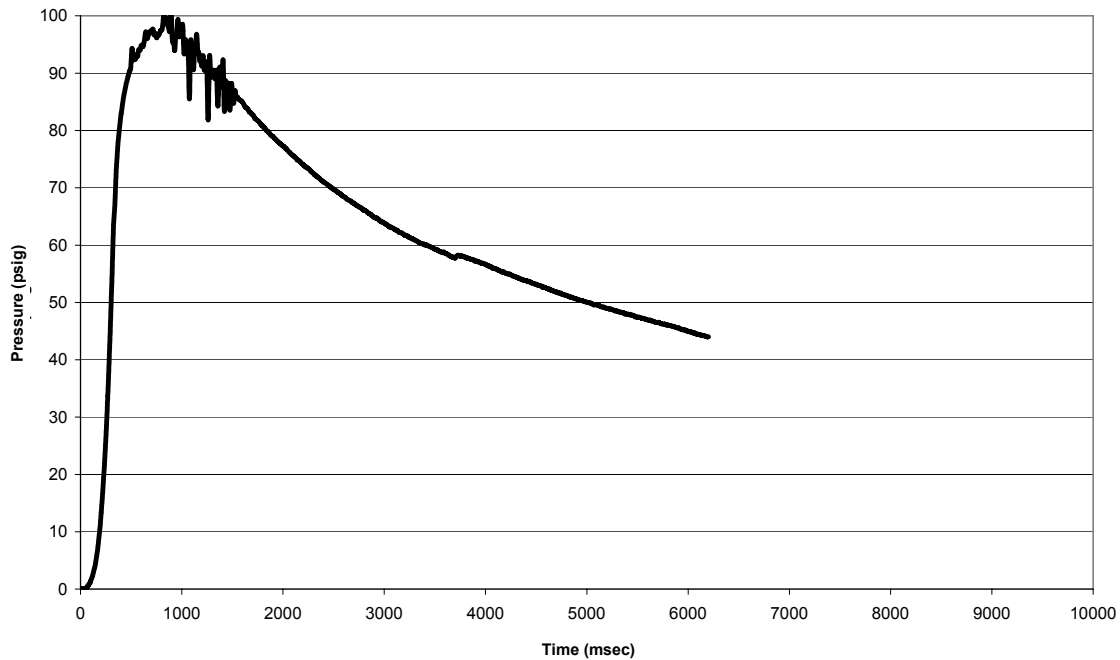


FIGURE 14. THE BTP PRESSURE PULSE AT 5.0% (TEST 9)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 121103T1
Concentration: 6% BTP

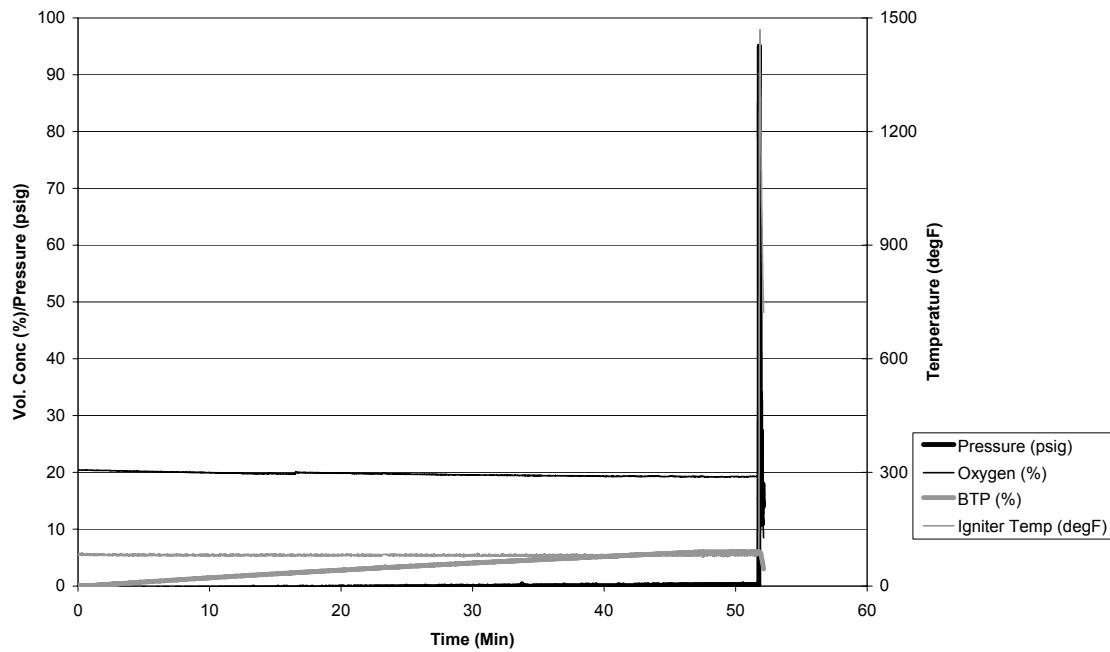


FIGURE 15. GAS AND TEMPERATURE TRACES FOR TEST 13

AEROSOL CAN SIMULATOR EXPLOSION TEST 121103T1
Concentration: 6% BTP

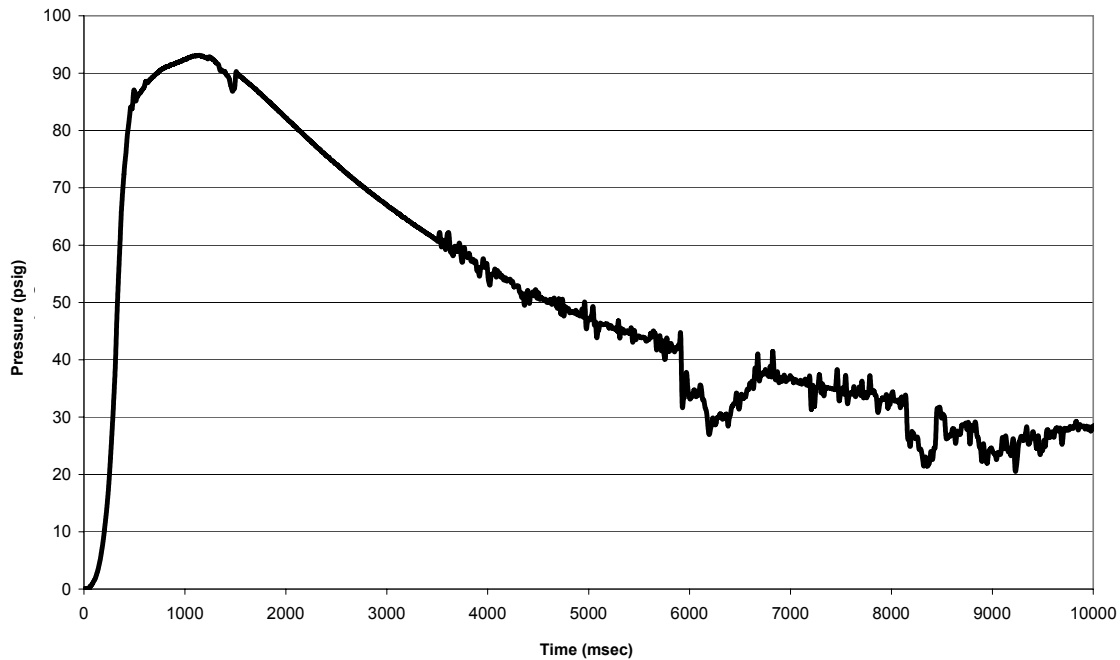


FIGURE 16. THE BTP PRESSURE PULSE AT 6.0% (TEST 13)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 121603T1
Concentration: 2.5% HALON 1301

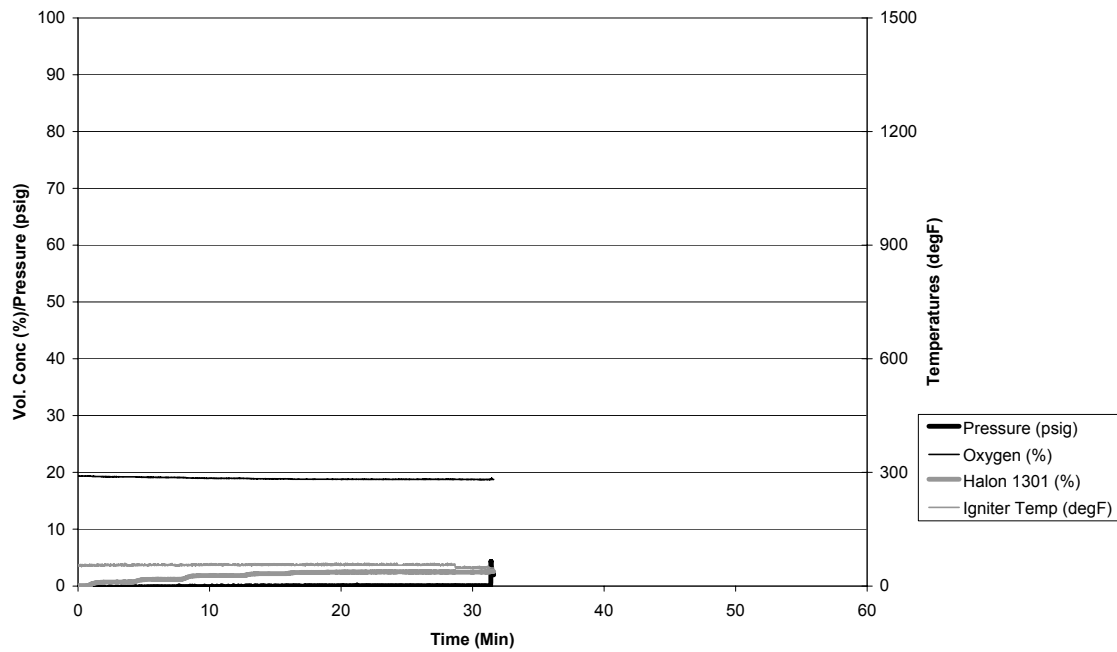


FIGURE 17. GAS AND TEMPERATURE TRACES FOR TEST 16

AEROSOL CAN SIMULATOR EXPLOSION TEST 121603T1
Concentration: 2.5% Halon 1301

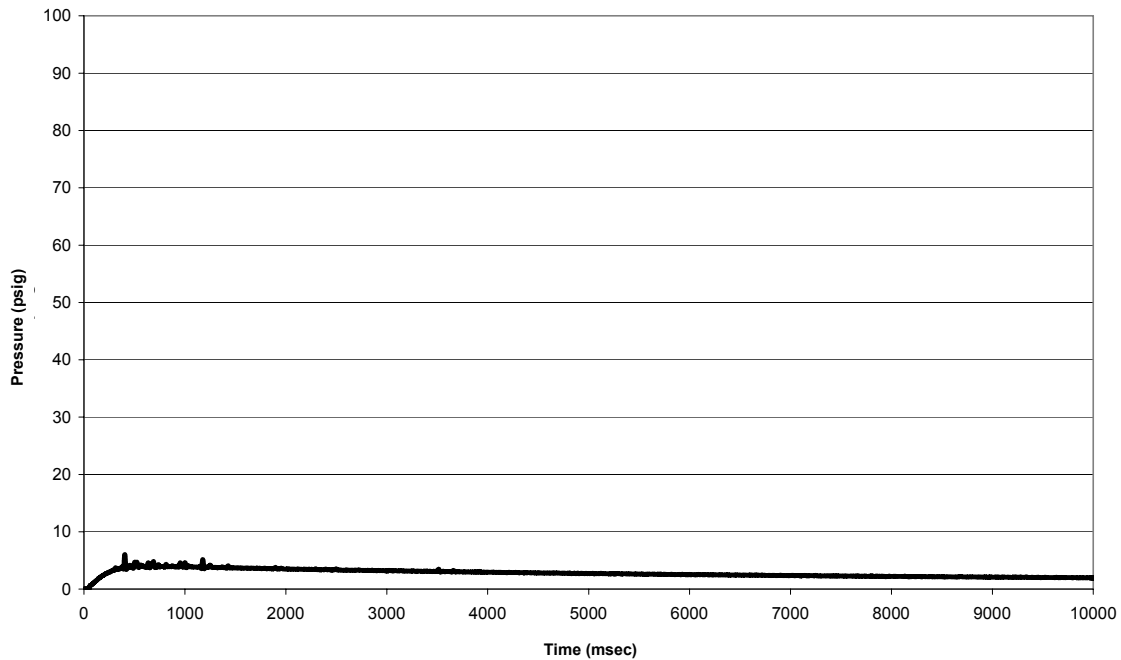


FIGURE 18. THE HALON 1301 PRESSURE PULSE AT 2.5% (TEST 16)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 010704T1
 Concentration: 8.9% HFC-125

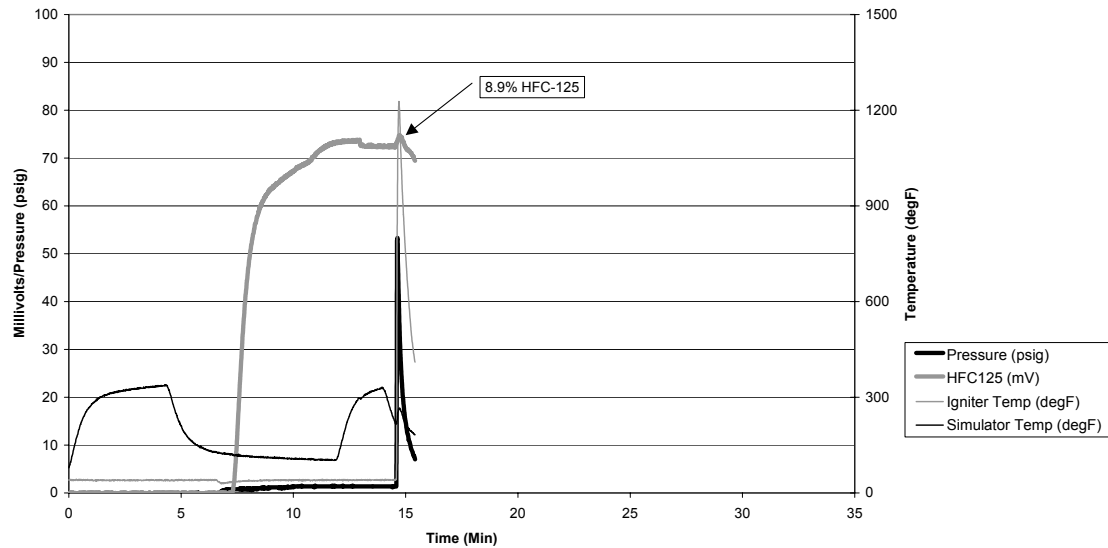


FIGURE 19. GAS AND TEMPERATURE TRACES FOR TEST 17

AEROSOL CAN SIMULATOR EXPLOSION TEST 010704T1
 Concentration: 8.9% HFC-125

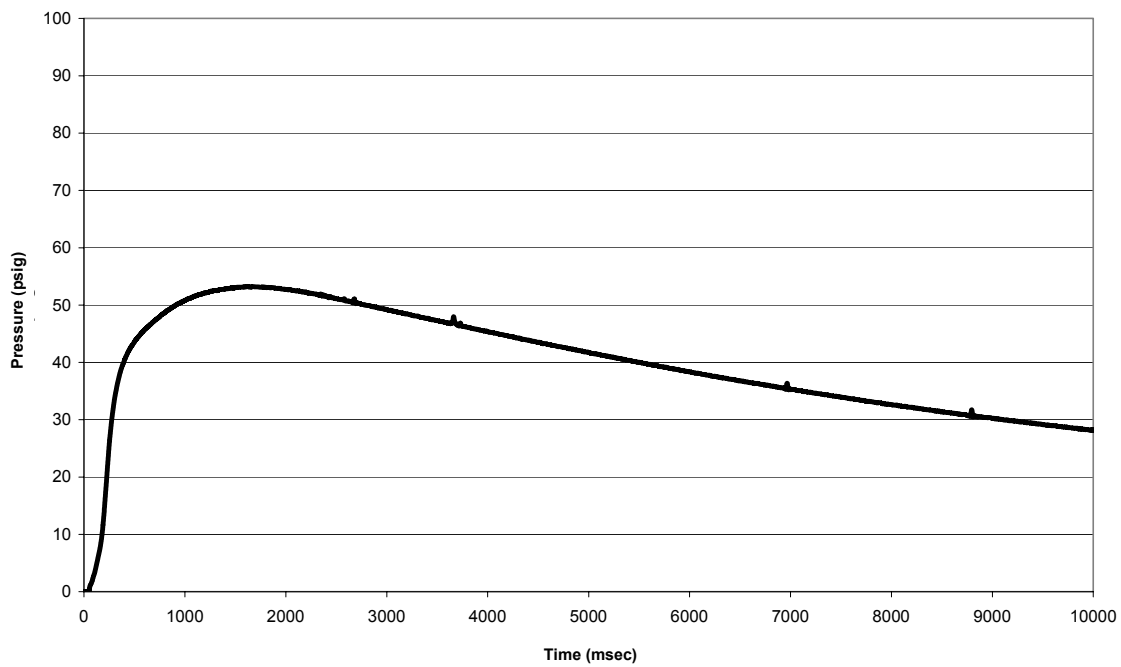


FIGURE 20. THE HFC-125 PRESSURE PULSE AT 8.9% (TEST 17)

AEROSOL CAN SIMULATOR EXPLOSION TESTS 010904T1
Concentration: 11.0% HFC-125

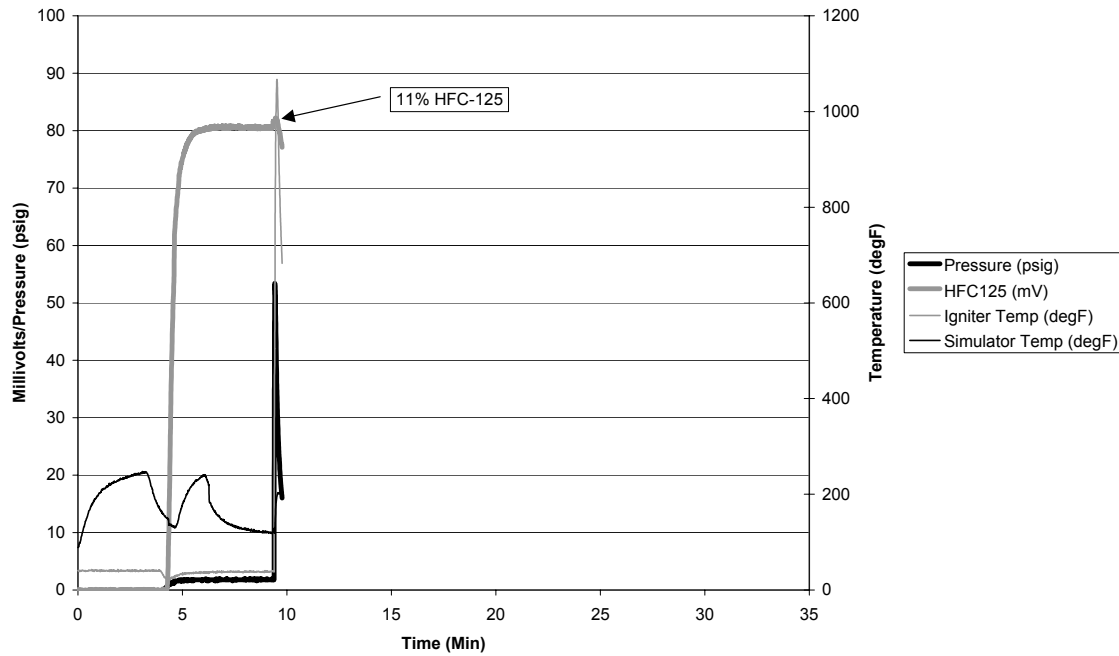


FIGURE 21. GAS AND TEMPERATURE TRACES FOR TEST 19

AEROSOL CAN SIMULATOR EXPLOSION TEST 010904T1
Concentration: 11% HFC-125

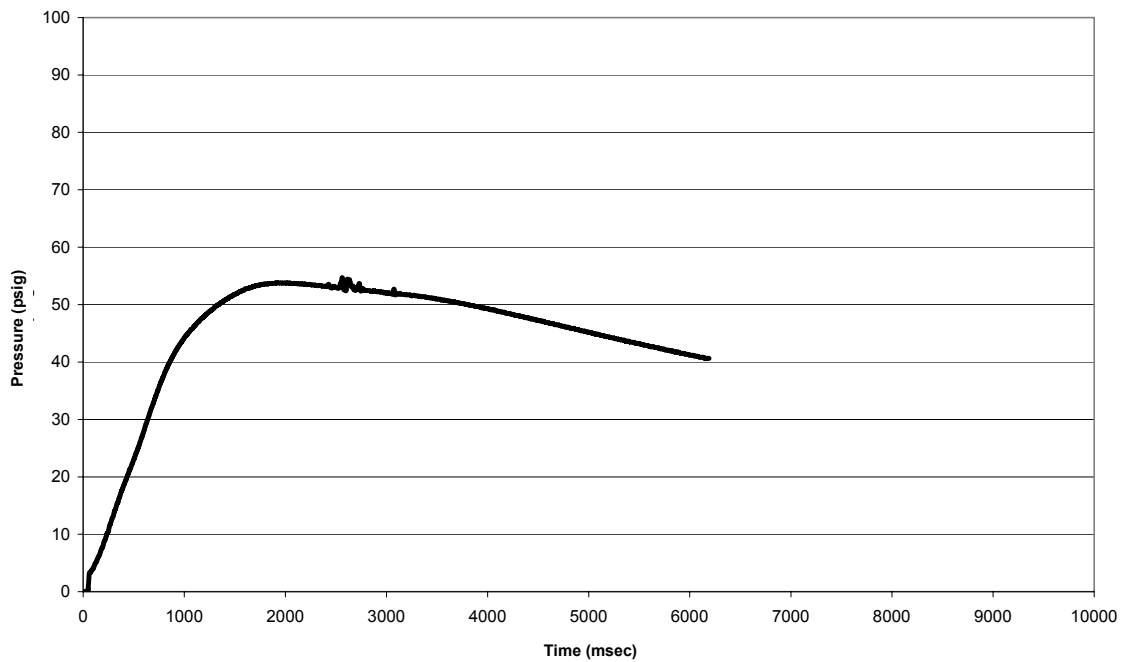


FIGURE 22. THE HFC-125 PRESSURE PULSE AT 11.0% (TEST 19)

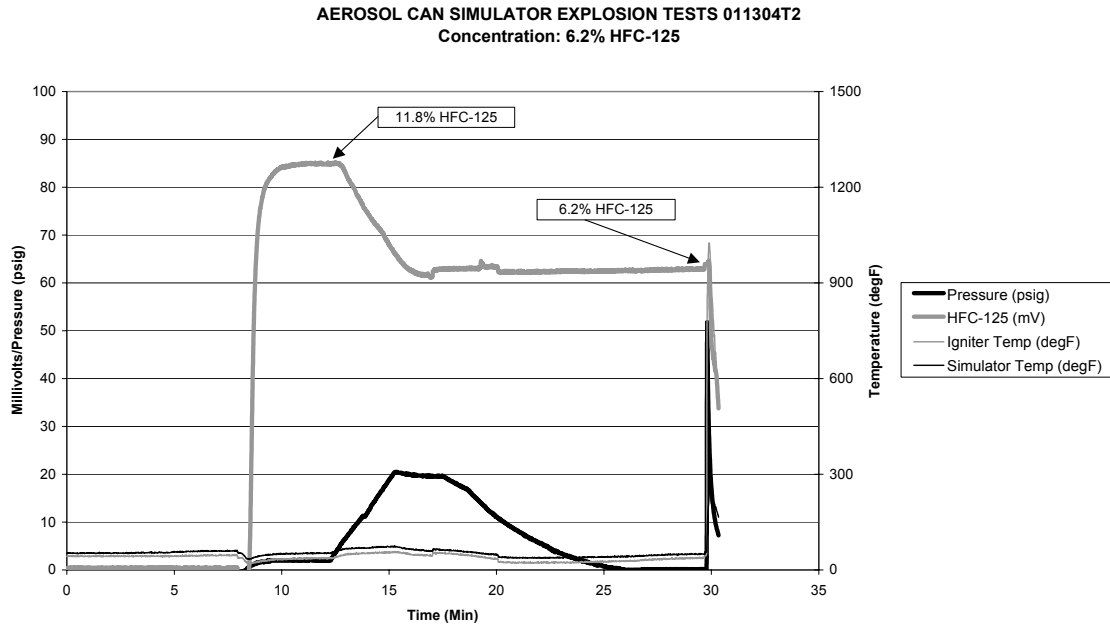


FIGURE 23. GAS AND TEMPERATURE TRACES FOR TEST 23

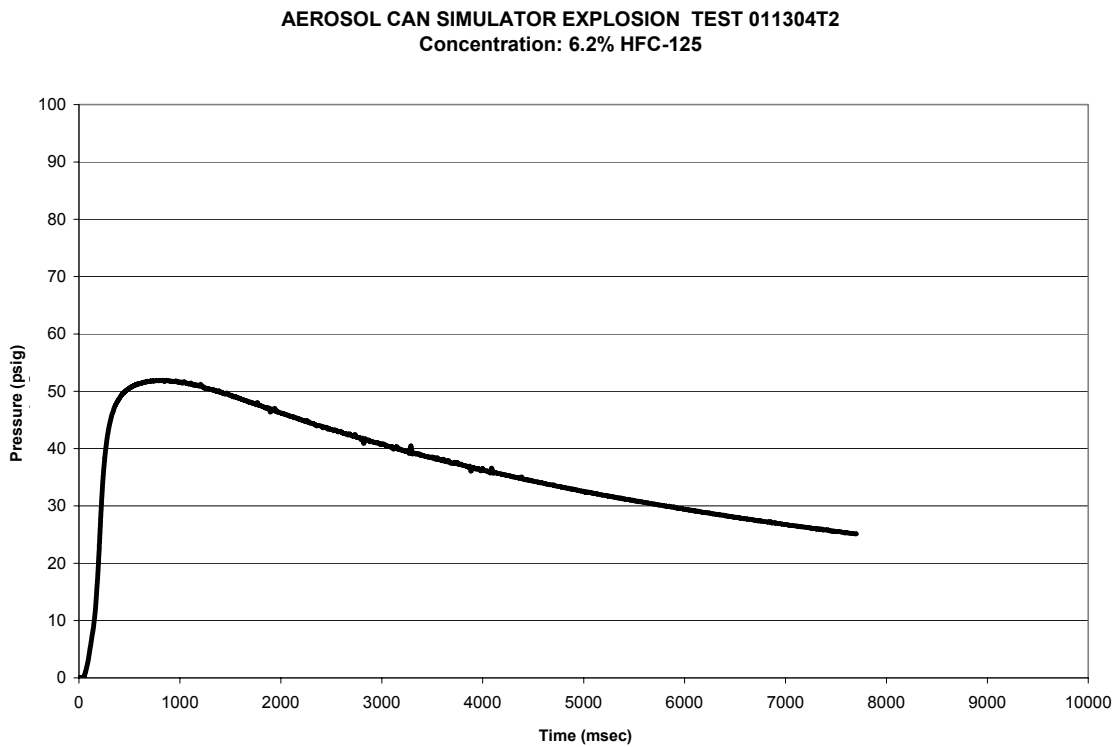


FIGURE 24. THE HFC-125 PRESSURE PULSE AT 6.2% (TEST 23)

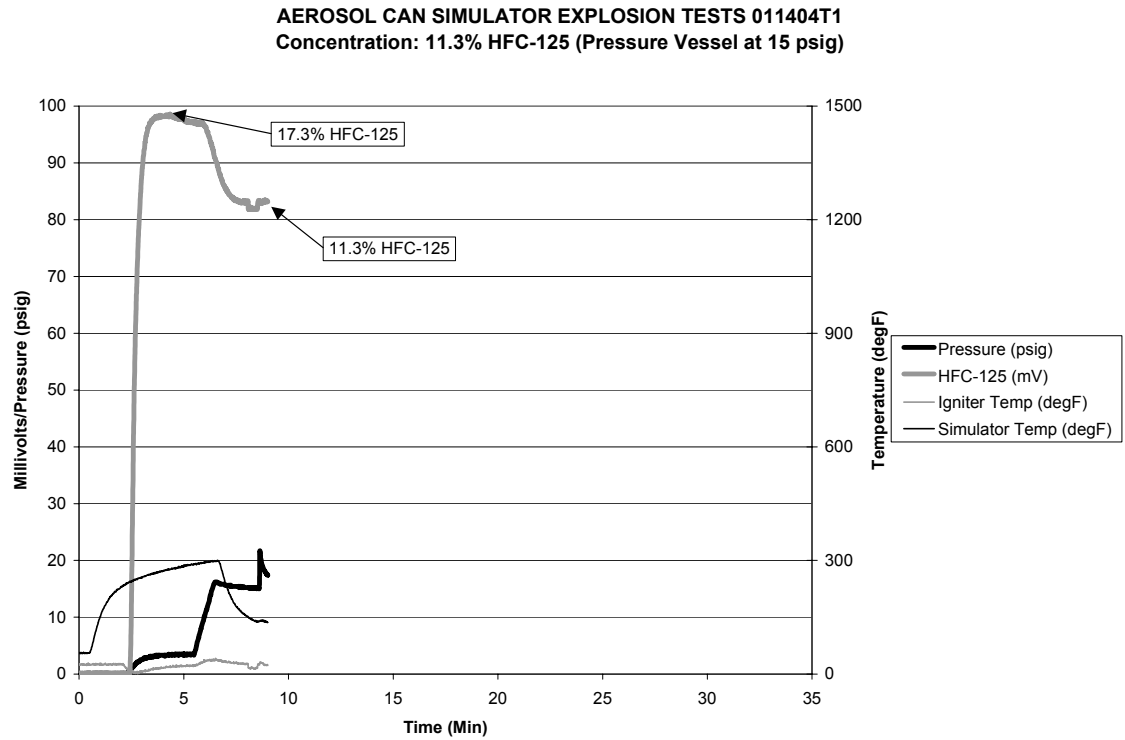


FIGURE 25. GAS AND TEMPERATURE TRACES FOR TEST 25

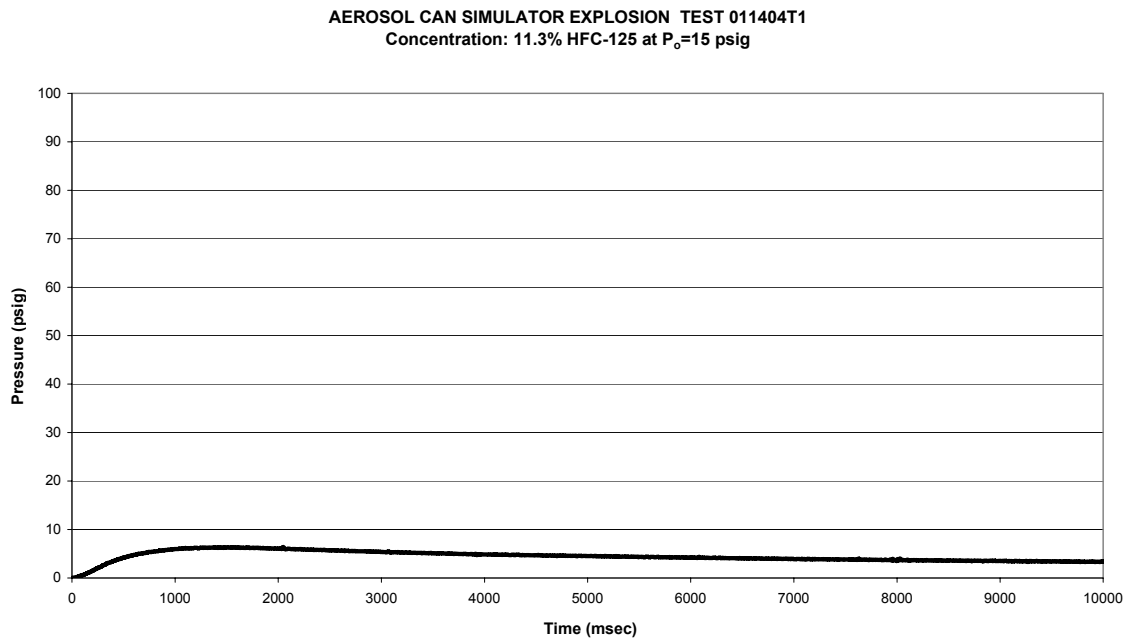


FIGURE 26. THE HFC-125 ($P_o=15$ psig) PRESSURE PULSE AT 11.3% (TEST 25)

TABLE 1. SUMMARY OF TEST RESULTS

Test Number	Test ID	Date	Agent	FIREX Type	Charge Weight (lbs)	Charge Pressure (psig)	Discharge Time (min)	Discharge Weight (lbs)	Agent Peak Concentration (%)	Air Temperature (Deg F)	Fire Event	Peak Temp (Deg F)	Peak Pressure (psig)	Comments
1	N/A	24-Nov-03	None	386 LRD	8.5	150	28.5	5*	2.5	72	N/A	N/A	N/A	FAA Analyzer to Statfam comparison
2	112503T1	25-Nov-03	BTP	386 LRD	10.6*	250	29.7	5*	2.5	67	Yes	368	64 psia	FAA computer data available
3	120203T1	2-Dec-03	BTP	386 LRD	N/A	N/A	N/A	N/A	N/A	65	Yes	387	25.4	Transducer saturated at 50 psia
4	120203T2	2-Dec-03	BTP	386 LRD	N/A	N/A	N/A	N/A	N/A	68	Yes	328	23.4	No BTP used in test - Baseline
5	120203T3	2-Dec-03	BTP	386 LRD	12.4*	262	27.1	5.5*	3	70	Yes	1056	63	No BTP used in test - Baseline
6	120303T1	3-Dec-03	BTP	386 LRD	11*	272	40.8	6.9*	4	65	Yes	1095	63	Location of igniter shield low, arc suppress by liquid
7	120403T1	4-Dec-03	BTP	386 LRD	12.5*	360	71	11.4*	6	59	No	N/A	N/A	High agent usage - test setup eval.
8	120403T2	4-Dec-03	BTP	386 LRD	10.5	360	40.4	10.5*	5	50	No	N/A	N/A	
Incorporated new scale system for weighing FIREX during test. Eliminated heat gun from the test setup.														
9	120803T1	8-Dec-03	BTP	386 LRD	12	360	43.3	9.75	5	86	Yes	1251	100	Calculated agent weight is 8.5 lbs. -1.25 lb discrepancy
10	120903T1	9-Dec-03	BTP	386 LRD	12.5	360	50.6	11.9	6	53	N/A	N/A	N/A	Questionable readout on simulator transducer. No test. Short on transducer signal.
11	121003T1	10-Dec-03	BTP	386 LRD	12.5	362	48.3	11.1	6	63	N/A	N/A	N/A	No test, igniter failed to work. Test aborted.
12	121003T1B	10-Dec-03	BTP	386 LRD	12.5	362	45.5	11.1	6	62	Partial	78	0	Small flame near ceiling area. Fan left on. Igniter 2 inches below ramp. Alcohol residue burning on igniters (small flames).
13	121103T1	11-Dec-03	BTP	386 LRD	12.5	362	48.5	11.1	6	63	Yes	1467	93	Heat gun test - no effect on the decomposition of BTP after 30 minutes activation
14	121503T1	15-Dec-03	BTP	386 LRD	13	360	55.5	11.1	6	62	N/A	N/A	N/A	Heat gun test - no effect on the decomposition of BTP after 10 minutes activation
15	121503T1	15-Dec-03	BTP	386 LRD	1.9	360	55.5	11.1	5	62	N/A	N/A	N/A	Halon 1301 used during this test
16	121603T1	16-Dec-03	Halon 1301	386 HRD	9	360	16 sec.	3.63	2.5	53.2	Yes	65	4	HFC125, igniter arc malfunctioned and suppressed by simulator liquid
17	010704T1	7-Jan-04	HFC-125	HRD	11.2	360	<1 min	Not Recorded	8.9		Yes	1227	53	HFC125
18	010804T1	8-Jan-04	HFC-125	HRD	17.5	360	<1 min	Not Recorded	11		N/A	N/A	N/A	HFC125
19	010904T1	9-Jan-04	HFC-125	HRD	17	360	<1 min	Not Recorded	11		Yes	1067	52	HFC125
20	011304T1a	13-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	13.5	49.6	No	N/A	N/A	HFC-125. Air added to drop concentration to required concentration, redundant igniter used
21	011304T1b	13-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	6.3	49.6	No	N/A	N/A	HFC-125. Pressure chamber pressurized to 20 psig and electrodes arcing. No simulator activation.
22	011304T2a	13-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	6.1	50	No	N/A	N/A	HFC-125. Pressure chamber pressurized to 20 psig and electrodes arcing. No simulator activation.
23	011304T2b	13-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	6.2	50	Yes	1026	52	HFC-125. Pressure vessel at ambient pressure
24	011404T1a	14-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	11.3	24	No	N/A	N/A	HFC-125. Pressure vessel pressurized to 15 psig. Igniter was activated, but no event (simulator not used).
25	011404T1b	14-Jan-04	HFC-125	HRD	30	360	<1 min	Not Recorded	11.3	24	Yes	32	6	HFC-125. Pressure vessel pressurized to 15 psig. Simulator activated.
* Estimated as a result of scale used during test.														
HRD= High Rate Discharge														
LRD= Low Rate Discharge														