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1. *Introduction and Summary.*—At speeds at which the compressibility of the air can be neglected it is known that the profile drag of an aerofoil section can be determined with sufficient accuracy from measurements of total head and static pressure across a section of the wake.¹ When compressibility is important measurement of a third quantity—e.g., air density—becomes theoretically necessary; but it appears that it is sufficiently accurate to assume that the total energy†, E , per unit mass of the air is constant across a section of the wake, and then measurements of total head and static pressure suffice. Assumptions analogous to those of R. & M. 1688 are that the total energy and the total head or the entropy are constant along a stream-tube in the wake between the measurement plane and a plane sufficiently far downstream for the static pressure to have become constant at its upstream value p_0 . On this basis a formula for determining the profile drag coefficient C_D is worked out below.

The constancy of E is equivalent to the constancy of the stagnation temperature‡ T_H , and experimental evidence of the constancy of T_H has been obtained. Experimental evidence concerning the accuracy of the pitot-traverse method, as described in this report, could also be deduced (i) from agreement between the values of the drag deduced from traverses at different distances behind the aerofoil, on which there is at present some limited data, and (ii) from a comparison of the values of the drag deduced from a wake exploration with the values measured on a balance, on which the evidence is incomplete because of the uncertain increase of drag on the end portions of the aerofoils in the tunnel boundary layer. Some of the available experimental evidence bearing on the accuracy of the method is set out below; it is clearly by no means complete, but in conjunction with theoretical considerations is thought to justify the use of the method, with a degree of accuracy sufficient for practical purposes, at any rate up to speeds of about 0.9 of the velocity of sound.‡

The presence of condensed moisture in the working section of a high speed tunnel will also vitiate the arguments of the present paper; this matter is discussed below in §13 and in Ref. 12.

* The experiments described in this report were made between 1936 and 1938: the report was revised for publication in 1945.

† For definitions of E and T_H see §2.

‡ The method should not be vitiated by the presence of limited shock waves.

2. *Definitions and some General Results for the Flow of a Compressible Fluid.*—For a perfect gas with constant specific heats

$$\frac{p}{\rho} = RT \quad \dots \dots \dots (1)$$

where p is the pressure, ρ the density, and T the absolute temperature. The specific heats at constant pressure and at constant volume, in work units, are denoted by C_p and C_v , and their ratio by γ ; the value of γ is taken as 1.4. The total energy, E , per unit mass is the sum of the kinetic energy, E_1 , per unit mass, the pressure energy, E_2 , per unit mass, and the intrinsic energy, E_3 , per unit mass, where

$$E_1 = \frac{1}{2}q^2, E_2 = p/\rho, E_3 = C_v T, \quad \dots \dots \dots (2)$$

and q is the resultant velocity. Since

$$C_p = C_v + R, \quad \dots \dots \dots (3)$$

$$E = \frac{p}{\rho} + C_v T + \frac{1}{2}q^2 = C_p T + \frac{1}{2}q^2 = \frac{\gamma}{(\gamma-1)} \frac{p}{\rho} + \frac{1}{2}q^2. \quad \dots \dots (4)$$

The entropy S of a perfect gas is given by

$$S = C_v \log \frac{p}{\rho^\gamma} = C_p \log \frac{RT}{p^\beta}, \quad \dots \dots \dots (5)$$

where

$$\beta = \frac{\gamma-1}{\gamma}. \quad \dots \dots \dots (6)$$

The total head H is defined as the pressure attained by a moving fluid element when brought to rest without change of entropy or total energy. It appears that H is sufficiently nearly equal to the pressure in an open-ended pitot-tube at velocities below the local velocity of sound, and this condition is satisfied in the wakes of aerofoils at subsonic speeds*.

The density and temperature corresponding to the pressure H are denoted by ρ_H and T_H and are referred to as the stagnation density and stagnation temperature. The velocity of sound, a , at pressure p and density ρ is given by

$$a^2 = \gamma p / \rho. \quad \dots \dots \dots (7)$$

The local Mach number is denoted by

$$M = q/a = (q\rho^{1/2})/(\gamma p)^{1/2}. \quad \dots \dots \dots (8)$$

It follows from the definitions and from equation (4) that the total energy per unit mass satisfies the relation

$$E = \frac{\gamma}{(\gamma-1)} \frac{H}{\rho_H} = C_p T_H, \quad \dots \dots \dots (9)$$

so that

$$\frac{1}{2}q^2 = C_p(T_H - T). \quad \dots \dots \dots (10)$$

* At velocities above the local velocity of sound H may be deduced from a pitot-tube reading by a formula due to Rayleigh, Scientific Papers, V, 608-610.

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The algebra is simplified by using T and T_H as variables whenever possible. It is necessary, however, to introduce the pressure since this alone is easily observable ;

$$C_p T = \frac{\gamma}{(\gamma - 1)} \frac{p}{\rho}, \quad C_p T_H = \frac{\gamma}{(\gamma - 1)} \frac{H}{\rho_H} \quad \dots \dots \dots (11)$$

as in (4). By definition the stagnation condition refers to fluid brought to rest adiabatically so that by (5)

$$\frac{p}{\rho^\gamma} = \frac{H}{\rho_H^\gamma}.$$

Hence eliminating density

$$\frac{T_H}{T} = \left(\frac{H}{p}\right)^\beta \quad \dots \dots \dots (12)$$

The final formula for drag coefficient is most conveniently expressed in terms of the auxiliary variable λ closely related to the Mach number M ,

$$\lambda = \frac{1}{2} \gamma M^2 = \frac{1}{2} \gamma (q/a)^2 = \frac{1}{2} \rho q^2 / p = \frac{1}{\beta} \cdot \frac{(T_H - T)}{T} = \frac{1}{\beta} \left\{ \left(\frac{H}{p}\right)^\beta - 1 \right\} \dots (13)$$

λ is tabulated as a function of $(H - p)/p$ in Table 1.* It is worth noting that as $(H - p)/H$ tends to zero

$$\lambda = \frac{\frac{1}{2} \rho q^2}{p} = \frac{H - p}{p} + 0 \left(\frac{H - p}{H} \right)^2 = \frac{H - p}{H} + 0 \left(\frac{H - p}{H} \right)^2 \quad \dots (14)$$

By means of this relation the final expression (35) for C_D' reduces at once to the standard low speed relation—R. & M. 1688¹, equation (2a).

3. *Some Remarks on the Total Energy.*—Consider steady flow through a wind tunnel containing an aerofoil, on the assumption that the walls of the tunnel and the surface of the aerofoil are perfectly non-conducting. The mass flux Q across any section of the tunnel is $\int dW$ across the section, where

$$dW = \rho q d\sigma, \quad \dots \dots \dots (15)$$

$d\sigma$ is an element of area of the section, and the direction of q is assumed to be normal to $d\sigma$. The mass flux is the same across any two sections. The difference between the fluxes of the sum of the kinetic and intrinsic energies across the two sections is equal to the difference of the rate at which work is being done by the pressures across the two sections. The rate at which the pressures do work across a section is

$$\int p q d\sigma = \int (p/\rho) dW = \int E_2 dW, \quad \dots \dots \dots (16)$$

and the rate of flux of kinetic plus intrinsic energy is

$$\int (E_1 + E_3) dW. \quad \dots \dots \dots (17)$$

Hence

$$(1/Q) \int (E_1 + E_2 + E_3) dW \quad \dots \dots \dots (18)$$

is the same across any section of the tunnel,—i.e., the average value of the total energy E is the same across any section of the tunnel.

* If a curve is preferred to a table, $x - \lambda(x)$ should be plotted.

These considerations apply to any real fluid. Moreover, outside the boundary layers and the wake, where the motion is practically irrotational and the effects of viscosity and conductivity negligible, it is known from the theory of the irrotational motion of an ideal fluid that E is practically constant. Thus E is constant across a section upstream of the aerofoil, and the mean value across any section downstream of the aerofoil is equal to the constant value upstream.

Let us now neglect the tunnel walls and consider in more detail the flow past the aerofoil, with particular reference to the determination of profile drag by means of a wake exploration across a section fairly near to the aerofoil. In Fig. 1 let AA be a section sufficiently far upstream for the velocity, pressure and density to be constant across it, these constant values being denoted by V , p_0 , ρ_0 respectively. Let BB be a section sufficiently far downstream for the static pressure to have become constant at its upstream value p_0 . Let T , T' be the boundaries of the wake at BB , and let $PQST$, $P'Q'S'T'$ be streamlines of the steady flow past the aerofoil. The wake widens downstream, and upstream of BB these streamlines lie entirely outside the wake and the boundary layer of the aerofoil; hence outside these streamlines the motion is practically irrotational, and the influence of viscosity and conductivity is negligible, so the total energy E and the entropy S are constant. (The entropy of a fluid element is affected only by dissipation and internal conduction, which are negligible; hence the entropy is constant along a streamline, and since it is constant at AA it has the same value on all streamlines outside $PQST$, $P'Q'S'T'$). Hence on BB , outside the wake, the density is ρ_0 and the velocity V . Denote the velocity and density at BB inside the wake by u and ρ respectively. Let CC be the section across which the wake is to be explored, cutting the streamlines $PQST$, $P'Q'S'T'$ at S and S' . Denote the velocity, pressure and density at CC , between S and S' , by u_1 , p_1 , ρ_1 respectively. Denote the total heads, stagnation densities and temperatures at AA , BB , CC by H_0 , H , H_1 , ρ_{H0} , ρ_H , ρ_{H1} , and T_0 , T , T_1 respectively, as shown in Fig. 1.

The flux of energy across $PQST$ and $P'Q'S'T'$ may be neglected, since viscosity and conduction are negligible there. The flux of energy across the boundary of the aerofoil is zero if its surface is non-conducting, and in any case may be neglected. The drag of the aerofoil does no work, since the motion is referred to axes fixed in the aerofoil. Hence by our previous arguments the average value of E on SS' or TT' is equal to its value E_0 on AA . (It may be noted that there is an increase in the average value of the entropy between PP' and SS' , due to the dissipation of kinetic energy into heat energy in the boundary layer of the aerofoil and immediately behind it, or in passage through a shock wave, this process being inevitably involved in the production of drag.)

If E is not constant and equal to E_0 on SS' and TT' then any excess at one place must be balanced by a defect at another place. We shall assume that in fact E is equal to E_0 on SS' and TT' . In §10 the results of an experimental research on the constancy of the stagnation temperature are set out; moreover E is the same on both sides of a shock wave.

4. *Determination of Drag from Wake Explorations.*—From considerations of momentum the drag D per unit length of the aerofoil is given* by

$$D = \int \rho u(V - u) dy \quad \dots \dots \dots (19)$$

where the integral is taken across the wake at the section BB .

* Previously published proofs of the formula use the total-head relation for an incompressible fluid. A proof valid for subsonic compressible flow, even with limited shock waves present is given in the Appendix.

Now let dy in equation (19) be the breadth of a stream-tube, and let its breadth at the section CC be dy_1 . If any inclination of the stream at the section CC' to the normal to the section is ignored, it follows from continuity that

$$\rho u dy = \rho_1 u_1 dy_1, \quad \dots \quad (20)$$

so
$$D = \int \rho_1 u_1 (V - u) dy_1 \quad \dots \quad (21)$$

and if c is the chord of the aerofoil it is convenient to write for the drag coefficient C_D

$$C_D (= D / \frac{1}{2} \rho_0 V^2 c) = \int C_D' dy_1 / c \quad \dots \quad (22)$$

where
$$C_D' = 2 \frac{\rho_1}{\rho_0} \cdot \frac{u_1}{V} \left(1 - \frac{u}{V} \right) \quad \dots \quad (23)$$

In the expressions (21) and (22) the integrals are taken across the wake at the section CC , and u is the velocity at the section BB on the streamline through the point at which the velocity is u_1 at the section CC .

It is required to express C_D' in terms of the observable quantities p_1 and H_1 . In addition to the assumption that on SS' and TT' the total energy E is constant and equal to E_0 , we now make the same assumption as that made by B. M. Jones in R. & M. 1688¹ for an incompressible fluid. We assume that for the purposes of calculation mean streamlines may be drawn in the wake such that between SS' and TT' the total head is constant along each stream-tube. This assumption, when E is assumed constant, is exactly equivalent to the assumption that the entropy is constant along each stream-tube.* For from equation (9) (applied to the three sections AA , BB and CC) and the constancy of E it follows that

$$H / \rho_H = H_1 / \rho_{H_1} = H_0 / \rho_{H_0} \quad \dots \quad (24)$$

hence if $H = H_1$ at points on the same streamline it follows that $\rho_H = \rho_{H_1}$, and

$$\frac{H}{\rho_H^\gamma} = \frac{H_1}{\rho_{H_1}^\gamma}, \quad \dots \quad (25)$$

i.e. the entropy is the same at points on the same stream-line. Conversely if (24) and (25) hold, then $H = H_1$ and $\rho_H = \rho_{H_1}$.

It follows from (10) and from the constancy of T_H that

$$\frac{1}{2} u^2 = C_p (T_{H_0} - T), \quad \dots \quad (26)$$

$$\frac{1}{2} V^2 = C_p (T_{H_0} - T_0), \quad \dots \quad (27)$$

$$\frac{1}{2} u_1^2 = C_p (T_{H_0} - T_1), \quad \dots \quad (28)$$

* The extension of Jones' method to compressible flow on the assumption of constant total energy everywhere and constant entropy and total head along each assumed stream-tube in the wake was considered by A. D. Young in Ref. 2, which includes the expansion of C_D' as far as the term in $(V/a_0)^2$ given in eqn. (53). In Ref. 3 Young gave an exact expression for C_D' . His arrangement of the expression and methods of computation are considered more troublesome for the same accuracy than the methods described here.

From equations (10) and (13) it follows that the conditions in the free stream at AA are determined by the value λ_0 of λ at that section according to the relation

$$\frac{1}{2}\rho_0 V_0^2 / p_0 = \frac{1}{2}\gamma M_0^2 = \lambda_0 \quad \dots \quad (29)$$

where
$$\lambda_0 = \lambda \left(\frac{H_0 - p_0}{p_0} \right)$$

is to be taken from Table 1. M_0 is tabulated as a function of $(H_0 - p_0)/p_0$ in Table 5.

In evaluating the expression for the drag it is convenient to make use of a fictitious temperature T_2 and value λ_2 of λ defined by

$$\begin{aligned} T_{H_0}/T_2 &= (H_0/H_1)^\beta, \\ \lambda_2 &= \lambda \left(\frac{H_0 - H_1}{H_1} \right) = \frac{1}{\beta} \cdot \frac{(T_{H_0} - T_2)}{T_2}. \quad \dots \quad (30) \end{aligned}$$

Then by (12)

$$\begin{aligned} \frac{T_{H_0}}{T_2} &= \left(\frac{H_0}{p_0} \right)^\beta \left(\frac{p_0}{H_1} \right)^\beta = \left(\frac{H_0}{p_0} \right)^\beta \left(\frac{p_0}{H} \right)^\beta \\ &= \frac{T_{H_0}}{T_0} \cdot \frac{T}{T_{H_0}} = \frac{T}{T_0}. \quad \dots \quad (31) \end{aligned}$$

Thus T_2 represents a proportional loss of stagnation temperature equal to the proportional gain of actual temperature in the wake. By (26), (27) and (31),

$$1 - \frac{u^2}{V^2} = \frac{T - T_0}{T_{H_0} - T_0} = \frac{T - T_0}{T_0} \cdot \frac{T_0}{T_{H_0} - T_0} = \frac{T_{H_0} - T_2}{T_2} \cdot \frac{T_0}{T_{H_0} - T_0} = \frac{\lambda_2}{\lambda_0}. \quad \dots \quad (32)$$

Again the term in u_1 in (23) involves the value λ_1 of λ at section CC. By (27), (28), (13) and (12)

$$\lambda_1 = \lambda \left(\frac{H_1 - p_1}{p_1} \right), \quad \dots \quad (33)$$

$$\frac{u_1^2}{V^2} = \frac{T_H - T_1}{T_H - T_0} = \frac{\lambda_1 T_1}{\lambda_0 T_0} = \frac{\lambda_1}{\lambda_0} \cdot \left(\frac{p_1}{H_1} \right)^\beta \left(\frac{H_0}{p_0} \right)^\beta \quad \dots \quad (34)$$

and by (11) and (12)

$$\frac{\rho_1}{\rho_0} = \frac{p_1}{p_0} \cdot \frac{T_0}{T_1} = \frac{p_1}{p_0} \cdot \left(\frac{p_0}{p_1} \right)^\beta \left(\frac{H_1}{H_0} \right)^\beta.$$

Finally substituting in (23)

$$C_D' = 2 \left(\frac{H_1}{H_0} \right)^{(\gamma-1)/2\gamma} \left(\frac{p_1}{p_0} \right)^{(\gamma+1)/2\gamma} \left(\frac{\lambda_1}{\lambda_0} \right)^{1/2} \left\{ 1 - \left(1 - \frac{\lambda_2}{\lambda_0} \right)^{1/2} \right\}. \quad \dots \quad (35)$$

The expression in $\{ \}$ is tabulated as a function of (λ_2/λ_0) in Table 4; for small values of $(H_0 - H_1)/H_0$ or λ_2/λ_0 it is equal to

$$\frac{1}{2}(\lambda_2/\lambda_0) + 0(\lambda_2/\lambda_0)^2.$$

Also $(\gamma - 1)/2\gamma = 1/7$ and $(\gamma + 1)/2\gamma = 6/7$; values of $(H_1/H_0)^{1/7}$ and $(p_1/p_0)^{6/7}$ are tabulated in Tables 2 and 3.

The expression (35) for the drag coefficient has the following advantages connected with the evaluation of the last factor in $\{ \}$. It evaluates λ_0 and λ_2 as functions of ratios of the observed pressures by means of the single entry Table 1 (or a single curve) and evaluates

the expression in { } as a function of the ratio λ_2/λ_0 by the single entry Table 2. Any other nominally exact method would involve a double entry table or family of curves, and would lose accuracy when H_1 is nearly equal to H_0 (as it always is near the edge of the wake) and when M_0 is small; in the former case the expression $1 - (\lambda_2/\lambda_0)$ is nearly unity and must therefore be worked out to considerable accuracy; in the latter case both λ_2 and λ_0 become small. Simpler approximate methods are in fact generally used in practice ^(9, 10, 11) but the present method is useful in extreme cases and as a standard of comparison of high nominal accuracy.

When V/a_0 is small, λ_0 , λ_1 and λ_2 are all small. In this case we show that (22) and (35) reduce to the formula given by B. M. Jones in R. & M. 1688,¹ and we find the first correction term. In conformity with the notation used in R. & M. 1688, write

$$g = \frac{H_1 - p_0}{H_0 - p_0}, \quad p = \frac{p_1 - p_0}{H_0 - p_0}, \quad \dots \dots \dots (36)$$

g and p then have the same meanings as in R. & M. 1688. Also write temporarily

$$\frac{H_0 - p_0}{p_0} = x. \quad \dots \dots \dots (37)$$

By the definition of λ , (13),

$$\begin{aligned} \lambda(x) &= \beta^{-1} \{ (x+1)^\beta - 1 \} \\ &= x - \frac{1}{2\gamma} x^2 + \frac{1}{3!} \cdot \frac{1}{\gamma} \left(1 + \frac{1}{\gamma}\right) x^3 - \frac{1}{4!} \cdot \frac{1}{\gamma} \left(1 + \frac{1}{\gamma}\right) \left(2 + \frac{1}{\gamma}\right) x^4 \dots \end{aligned} \quad (38)$$

so that from the definition of λ_0 , (29), (37) and (38)

$$\lambda_0 = x - \frac{1}{2\gamma} x^2 + \dots, \quad x = \lambda_0 + \frac{1}{2\gamma} \lambda_0^2 + \dots \dots \dots (39)$$

Then

$$\frac{p_0}{H_0} = \frac{1}{1+x}, \quad \dots \dots \dots (40)$$

$$\frac{H_1}{H_0} = \frac{1+gx}{1+x} = 1 - (1-g)x + \dots = 1 - (1-g)\lambda_0 + \dots, \dots (41)$$

$$\frac{p_1}{p_0} = 1 + px = 1 + p\lambda_0 + \dots, \quad \dots \dots \dots (42)$$

so $\left(\frac{H_1}{H_0}\right)^{(\gamma-1)/2\gamma} = 1 - \frac{\gamma-1}{2\gamma} (1-g)\lambda_0 + \dots, \quad \dots \dots \dots (43)$

$$\left(\frac{p_1}{p_0}\right)^{(\gamma+1)/2\gamma} = 1 + \frac{\gamma+1}{2\gamma} p\lambda_0 + \dots, \quad \dots \dots \dots (44)$$

Also

$$\begin{aligned} \frac{H_0 - H_1}{H_1} &= \frac{(1-g)x}{1+gx} = (1-g) \{ x - gx^2 + \dots \} \\ &= (1-g) \left\{ \lambda_0 + \left(\frac{1}{2\gamma} - g \right) \lambda_0^2 + \dots \right\}. \quad \dots \dots \dots (45) \end{aligned}$$

and hence, from (38) and (30),

$$\begin{aligned}\lambda_2 &= (1-g) \left\{ \lambda_0 + \left(\frac{1}{2\gamma} - g \right) \lambda_0^2 - \frac{1}{2\gamma} (1-g) \lambda_0^2 + \dots \right\} \\ &= (1-g) \left\{ \lambda_0 - \left(1 - \frac{1}{2\gamma} \right) g \lambda_0^2 + \dots \right\}, \quad \dots \quad \dots \quad (46)\end{aligned}$$

so

$$1 - \frac{\lambda_2}{\lambda_0} = g \left\{ 1 + \left(1 - \frac{1}{2\gamma} \right) (1-g) \lambda_0 + \dots \right\} \quad \dots \quad \dots \quad (47)$$

and

$$\begin{aligned}1 - \left(1 - \frac{\lambda_2}{\lambda_0} \right)^{1/2} &= 1 - g^{1/2} - \frac{1}{2} \left(1 - \frac{1}{2\gamma} \right) g^{1/2} (1-g) \lambda_0 + \dots \\ &= (1 - g^{1/2}) \left\{ 1 - \frac{1}{2} \left(1 - \frac{1}{2\gamma} \right) (g^{1/2} + g) \lambda_0 + \dots \right\}. \quad \dots \quad \dots \quad (48)\end{aligned}$$

Finally

$$\begin{aligned}\frac{H_1}{p_1} &= \frac{1+gx}{1+px}, \\ \frac{H_1 - p_1}{p_1} &= \frac{(g-p)x}{1+px} = (g-p) \{ x - px^2 + \dots \} \\ &= (g-p) \left\{ \lambda_0 + \left(\frac{1}{2\gamma} - p \right) \lambda_0^2 + \dots \right\}, \quad \dots \quad \dots \quad (49)\end{aligned}$$

and from (38) and (33)

$$\lambda_1 = (g-p) \left\{ \lambda_0 + \lambda_0^2 \left[\frac{1}{2\gamma} (1-g) - \left(1 - \frac{1}{2\gamma} \right) p \right] + \dots \right\}, \quad \dots \quad \dots \quad (50)$$

so

$$\left(\frac{\lambda_1}{\lambda_0} \right)^{1/2} = (g-p)^{1/2} \left\{ 1 + \frac{1}{2} \lambda_0 \left[\frac{1}{2\gamma} (1-g) - \left(1 - \frac{1}{2\gamma} \right) p \right] + \dots \right\}. \quad \dots \quad \dots \quad (51)$$

From (35), (43), (44), (48) and (51) it now follows that, correct to the first power of λ_0

$$C_D' = 2(g-p)^{1/2} (1 - g^{1/2}) \left\{ 1 + \frac{\lambda_0}{4\gamma} [3 - 2\gamma + 3p - 2g - (2\gamma - 1)g^{1/2}] \right\} \dots \quad \dots \quad (52)$$

i.e., from (29)*

$$C_D' = 2(g-p)^{1/2} (1 - g^{1/2}) \left\{ \left[1 + \frac{1}{8} (M_0)^2 [3 - 2\gamma + 3p - 2g - (2\gamma - 1)g^{1/2}] \right] \right\} \dots \quad \dots \quad (53)$$

Thus λ_0 , λ_1 , λ_2 are calculated from (29), (33) and (30) with the help of Table 1; C_D' is calculated from (35) with the help of Tables 2, 3 and 4; for small values of M_0 , C_D' is calculated from (53), where g and p are defined in (36).

5. *Apparatus.*—(a) *High-Speed Wind Tunnel and Model Aerofoils.*—The working section of the High-Speed Wind Tunnel (Fig. 2) included† about 17 in. of steel tube of 1 ft. diameter. The tunnel was vertical and the air flowed upwards. The working section may be considered to extend from the end of the intake flare to the injector slot.

A model aerofoil of standard size has a chord of 2 in. The aerofoils crossed the working section horizontally 8 in. above the end of the intake flare.

* Formula (53) was given by A. D. Young in Reference 2.

† The tunnel has been modified and the length of the working section increased since the completion of the experiments described in this report.

(b) *Pitot Tubes*.—In most of the earlier pitot traverse experiments a single pitot tube was used. It was mounted on a streamline bar (Figs. 3 and 4) which crossed the jet horizontally and at right angles to the span of the aerofoil, the centre line of the bar being 4.1 in. above the centre line of the aerofoil. The pitot tube was traversed across the wake by a micrometer screw.

The standard length of the pitot tube was 1.0 in.; the mouth of the tube was 1.7 in. behind the trailing edge of the aerofoil. A few observations were taken with a pitot tube 2.3 in. long (Fig. 5) with its orifice 0.4 in. behind the trailing edge.

(c) *Static-Pressure Tubes*.—The static-pressure tubes used are shown in Figs. 4 and 5. The distances of the static holes from the trailing edge of an aerofoil were considered to be sufficiently nearly equal to the distances of the mouths of the corresponding pitot tubes. In the longer pitot tube the static holes were, in fact, 0.4 in. behind the trailing edge, and since the length of the tube beyond the static holes was 0.2 in., the point of the tube was only 0.2 in. behind the trailing edge. A closer approach was considered inadvisable. (The diameter of the working portion of the longer static tube was 0.035 in., so the length beyond the static holes was about $5\frac{1}{2}$ diameters.)

(d) *Comb of Pitot Tubes*.—Some additional observations were made with the comb of pitot tubes shown in Fig. 4. The tubes were flattened at the ends* so that the effective internal width was reduced to 0.005 in., the external width being 0.02 in. (A rather larger width is considered advisable because of the sluggishness of the readings.) The five inner tubes had spacings between 0.07 in. and 0.09 in. across the wake, but were staggered so that the total separation was not less than 0.1 in.; the outer tubes were more widely spaced in order to cover the wake of a shock wave at high speeds, the outermost tube on one side being 2 in. from the centre. The central tubes were not close enough together to give sufficient detail at low speeds, so the comb was traversed by the micrometer screw to a series of positions (usually three positions at intervals of 0.025 in.). The length of the tubes in the comb was 0.95 in.

(e) *Manometers*.—The pressure in the single pitot tube was read against the pressure of the atmosphere (which was equal to the total head in the tunnel outside the wake) on a 3-ft. vertical water manometer, except in the case of the readings near the centre of the wake at the highest tunnel speeds, for which a mercury manometer was used. The tubes in the comb of pitot tubes were connected to a vertical multiple water manometer reading up to 5 ft. of water, the range again being sufficient except at the highest speed. The static-pressure tubes were read on a water manometer against a standard pressure hole in the tunnel wall, 5.4 in. upstream of the centre line of the model aerofoil. (This pressure hole is used, apart from a correction for tunnel wall interference (see §7), to determine the air speed in the tunnel.)

6. *Correction for Finite Diameter of Pitot Tube*.—When there is a transverse gradient of total head across the mouth of a pitot tube the effective centre of the tube is displaced from the geometrical centre towards the region of higher velocity, so that the area under the total pressure curve is less than it should be, and for the tubes described in §5 it is sufficiently accurate, at low speeds, to take this displacement as 0.18 times the external diameter of the tube⁴. This correction was applied both at low and at high speeds; there is no direct experimental evidence of its validity at high speeds, but the relative importance of the correction diminishes rapidly with increase of speed above the shock stall because of the increase in the drag coefficient C_D .

C_D is the area under the curve of C_D' against y , where y is distance across the wake in chords (see equation (22)); the correction amounts to increasing the arithmetical value of the abscissa at every point by 0.18 times the diameter of the tube divided by the chord of the aerofoil, and this is true for the parts of the curve on both sides of the maximum ordinate. Hence to apply the correction it is necessary only to increase C_D by 0.36 times the maximum ordinate of the C_D' curve times the diameter of the tube divided by the chord.

* The ends of the single pitot tubes were not flattened since they had to be screwed into the traversing bar when it was in position in the tunnel.

7. *Correction for Tunnel Interference.*—The correction for tunnel wall interference with a 2-in. chord aerofoil in a 1-ft. tunnel is small at low speeds, even for fairly high lift coefficients, but above the compressibility stall, with shock waves present, the correction is much greater.

Information on the magnitude of the correction was obtained from drag determinations by the pitot traverse method on two models, of 2-in. chord and 1.2-in. chord respectively, of the aerofoil N.A.C.A.0020 at zero incidence. The results are shown in Fig. 6. The fairly good agreement for values of M_0 between about 0.4 and 0.65 shows that for these speeds the correction is small. (The discrepancy at lower speeds is presumably due to variation of C_D with Reynolds number.) The difference in the uncorrected values of C_D for the two models becomes large at larger values of M_0 , but since C_D is increasing rapidly the difference in the values of M_0 for a given C_D is still small.

In order to deduce from the results a method of working out the correction for other aerofoils, pressure readings were taken not only at the standard pressure hole A in the wall, 5.4 in. upstream of the centre line of the model aerofoil, but also at a hole B exactly opposite the centre line; and values of M_0 were deduced from these pressures by formula (29). Denote these values by M_{AL} and M_{BL} for the 2-in. chord aerofoil, and by M_{AS} , M_{BS} for the 1.2-in. chord aerofoil. Let M_0 denote the equivalent value in an unbounded stream. Then if we write

$$\frac{M_{BL} - M_0}{M_0 - M_{AL}} = \frac{M_{BS} - M_0}{M_0 - M_{AS}} = \mu, \quad \dots \quad (54)$$

the theoretical value of μ is 2 for two-dimensional flow (an aerofoil spanning a rectangular tunnel) at low speeds.⁵ We assume that for an aerofoil spanning a circular tunnel μ is a constant, even when shock waves are present, and deduce its value experimentally. We define equivalent speeds for the two models as speeds at which the drag divided by the chord is the same; elimination of M_0 from equations (54) yields the equation

$$\mu = \frac{M_{BL} - M_{BS}}{M_{AS} - M_{AL}}, \quad \dots \quad (55)$$

and the sixth column of the table below gives values of μ for four values of the ratio drag/(chord $\times$ atmospheric pressure $\times$ tunnel diameter), corresponding to values of the drag coefficient from 2 to 6 times the low-speed value. The values of M_0 corresponding to these values of μ , deduced from the equation

$$M_0 = \frac{\mu}{1 + \mu} M_{AL} + \frac{1}{1 + \mu} M_{BL}, \quad \dots \quad (56)$$

are shown in the seventh column; values of M_0 with $\mu = 1.5$ throughout, so that

$$M_0 = 0.6 M_{AL} + 0.4 M_{BL}, \quad \dots \quad (57)$$

are shown in the eighth column, and the differences from the values in the seventh column are negligible. Hence equation (57) may be used to correct for tunnel interference.

Drag $\div$ (Chord $\times$ atmospheric pressure $\times$ tunnel diameter)	M_{AL}	M_{BL}	M_{AS}	M_{BS}	μ	M_0	M_0 ($\lambda = 1.5$)
0.0373	0.767	0.875	0.800	0.825	1.515	0.810	0.810
0.0280	0.758	0.838	0.785	0.801	1.370	0.792	0.790
0.0187	0.746	0.806	0.767	0.777	1.381	0.772	0.770
0.0093	0.726	0.770	0.739	0.743	2.077	0.740	0.744

A curve of C_D against M_0 , corrected by equation (57), is also shown in Fig. 6. The above correction applies to the circular high-speed tunnel both before and after modification.*

* See footnote on page 8.

It may be remarked that a static-pressure drop along the tunnel would have no effect on the determination of drag by the pitot-traverse method. Since equation (57) was derived from such determinations, it should be independent of static-pressure drop. It should be applicable to other pitot-traverse drag determinations in the tunnel, whatever the static-pressure drop may be.

8. *Pitot-Traverse Curves above and below the Shock Stall.*—Curves of total head drop, $H_0 - H_1$, in inches of water, against distance from the centre of the wake in chords are shown in Fig. 7a for a traverse at 0.2 chord behind the trailing edge of a model of the symmetrical aerofoil N.A.C.A. 0012 (12 per cent. thick). The traverses were taken at zero incidence, and are shown at two speeds, one below and the other above, the shock stall. Similar curves are shown in Fig. 7b for the 20 per cent. thick aerofoil N.A.C.A. 0020.

At speeds below the shock stall the shapes of the curves are the same as at low speeds, the effects of changes of Reynolds number being small. Above the shock stall the curves have widened (and the drag coefficient has correspondingly increased rapidly), and the outer parts of the curves have a marked sideways extension with a fairly low pressure difference. Thus in Fig. 7a the wake may be considered to be about 0.08 chords wide below the shock stall; above the shock stall it is wider than 0.8 chords.

The sideways extension of the curves represents the wake of a limited shock wave attached to the aerofoil; but a marked thickening or a breakaway of the boundary layer may also be present, being associated with the presence of the shock wave. It is not possible to distinguish with any certainty where the wake due to thickening or breakaway of the boundary layer merges into the wake of the shock wave, but the fact that for the thicker section the bends between the central and outer parts of the curves are less abrupt than for the thinner section indicates that boundary layer effects are more important with thick than with thin sections.

9. *Thermocouples for the Measurement of Stagnation Temperature.*—Since the total energy E is the product of the specific heat at constant pressure C_p and the stagnation temperature T_H (§2, equation (9)), considerable interest attaches to measurements of T_H .

After several unsuccessful attempts to design an instrument to measure T_H , a satisfactory instrument (Fig. 8) was developed with the help of suggestions from Mr. G. E. Kerr and Professor G. I. Taylor. The instrument consists of an ebonite pitot tube 1.2 in. long with an outside diameter 0.15 in., mounted at right angles to a streamline bar similar to that used for total-head and static-pressure explorations, so that it can be traversed across a wake over the same path as the pitot and static-pressure tubes. A single thermojunction of 30 S.W.G. iron-eureka wire was situated 0.25 in. from the mouth of the tube, and the wires were carried through the tube and the traversing bar to the outside of the tunnel. The tube was pierced with holes 0.5 in. from its mouth so that air could flow past the thermojunction; the velocity of the flow past the thermojunction must not be large enough to cause the recorded temperature to depart appreciably from the stagnation temperature, but subject to this condition a large flow of air is favourable in order to ensure complete control of the temperature of the thermojunction by the air flowing through the tube; a velocity of the order of 100 ft. per second appears reasonable. The rate of flow was not measured; it was considered sufficient to ensure that the reading of the instrument when calibrated in the empty tunnel should be independent of tunnel speed.

Two pitot thermocouples A and B were mounted on the traversing bar 1.5 in. apart, and (except at the highest speeds) B was outside the wake when A was traversed across it. A and B were each read against a thermojunction situated in a low velocity region in the intake. The voltage was read on a vernier potentiometer, sensitive to one microvolt, i.e., to $1/(52.6)$ of a degree centigrade.

The thermocouples were calibrated in the empty tunnel with several sizes of leak, and calibration curves for three different leaks are shown at the top of Fig. 9. As a result of these calibrations the leak finally adopted was a single hole with a diameter of 0.03 in.; this leak

appears to give less variation with tunnel speed than a larger or a smaller leak. For the thermocouple finally adopted there was an unexplained difference of temperature of nearly 1°C. in the empty tunnel between the readings of the pitot thermocouple and the intake thermocouple at speeds above $M_0 = 0.3$; at lower speeds consistent readings could not be obtained.

It may be of interest to mention that in earlier types of thermocouple there was no flow through the tube, and the thermojunction was situated at the mouth of the tube. The readings in the empty tunnel were rather erratic, and the calibration curves had an appreciable slope. A calibration for a thermojunction at the upstream end of a pointed projection is shown in Fig. 9⁶.

For comparison with the temperature differences shown in the calibration curves in Fig. 9, it may be mentioned that when the absolute temperature in the intake is T_0 , the drop in the actual temperature of the air from the intake to the working section is $M_0^2 T_0 / (5 + M_0^2)$. Thus for $M_0 = 0.7$ and an intake temperature of 16°C. , the drop is 26°C.

After calibration the thermocouples *A* and *B*, each of the design finally adopted (Fig. 8), were traversed across the wake behind the aerofoil N.A.C.A. 0020 at zero incidence at values of M_0 ranging from 0.458 to 0.756. The main difficulty in the experiments was caused by irregular fluctuations of temperature in the tunnel intake; these fluctuations were sometimes much greater than the small temperature differences to be measured, so in order to obtain satisfactory results advantage had to be taken of favourable weather and temperature conditions. In addition, in order to reduce as far as possible the effects of fluctuations and of instrumental errors, simultaneous readings, a_1 and b_1 were taken with the thermocouples *A* and *B* respectively, with the aerofoil in place, *A* being inside and *B* outside the wake. Readings a_0 and b_0 were then taken with *A* and *B* with the aerofoil removed, and the final reading was taken to be $(a_1 - a_0) - (b_1 - b_0)$. Ideally the stagnation temperature should be the same as in the intake both outside the wake and in the empty tunnel, i.e., b_1, a_0, b_0 should all be zero, so if there were no fluctuations or instrumental errors $a_1 - a_0 - b_1 + b_0$ should give the correct readings. The most likely sources of error are (i) calibration differences between the two instruments *A* and *B*; (ii) fluctuations with time; (iii) a difference in the readings of the intake and pitot thermocouples, such as is shown in the calibration curves in Fig. 9. Of these sources of error (i) would affect $a_1 - b_1$ and $a_0 - b_0$ separately, but should not affect the double difference; (ii) would affect $a_1 - a_0$ and $b_1 - b_0$ (since the readings a_1, b_1 and a_0, b_0 were not taken simultaneously) but the effect should at any rate be much lessened by taking the double difference; the effect of (iii) should also be eliminated by taking the double difference. Hence the effects of all three sources of error may be best eliminated by using the double difference $a_1 - a_0 - b_1 + b_0$ for the final reading.

10. Stagnation Temperature Measurements in a Wake.—Results of measurements of stagnation temperature at five values of M_0 across a section of the wake behind a brass model of the aerofoil N.A.C.A. 0020 at zero incidence are shown in Fig. 10. The aerofoil had a 2-in. chord, and the end of the thermojunction was 1.75 in. from the trailing edge. The readings a_1 of the thermojunction *A* traversed through the wake, the corresponding readings a_0 in the empty tunnel, and the doubly corrected readings $a_1 - a_0 - b_1 + b_0$ are shown separately.

The curves show that the stagnation temperature, referred to the value* outside the wake as datum, is negative in the centre of the wake and positive at the sides. For values of M_0 up to about 0.63 the maximum difference from zero is of the order of $\frac{1}{2}^{\circ}\text{C.}$, while the mean value across the wake is practically zero; at $M_0 = 0.756$ the maximum value is 1°C. and the mean value is less than $\frac{1}{2}^{\circ}\text{C.}$ Variations of the stagnation temperature of these magnitudes will not cause appreciable errors in the values of the drag coefficient deduced by the method described in §4 on the assumption of constant total energy.

The doubly corrected results of the measurements of stagnation temperature at $M_0 = 0.458, 0.576, 0.756$ are drawn again in Fig. 11, where curves of C_D' (§4, equation (36)) over a section 1.7 in. behind the trailing edge of the same aerofoil are shown for comparison. (The horizontal

* The mean value of the stagnation temperature across a section of the wake (strictly speaking weighted with the product of the velocity and the density) is theoretically equal to the value outside the wake (cf. §3).

scales are the same for the two sets of curves, but the zeros were not determined, and the peaks of corresponding curves have been placed over one another). For the two lower values of M_0 the widths over which the stagnation temperature and C_D' (and therefore the total-head loss in the wake) differ from zero are in good agreement. A curve of C_D' at $M_0 = 0.756$ was not available; curves are shown for $M_0 = 0.717$ and $M_0 = 0.762$. There is some evidence that the width of the "total-head wake" at $M_0 = 0.762$ was considerably greater than the width of the "stagnation temperature" wake at $M_0 = 0.756$; the values of M_0 are not very different, and it is significant that the sideways extension of the "total-head wake" is attributable to shock waves and that theoretically the stagnation temperature does not change across a shock wave.

Some measurements taken with an earlier (and unsatisfactory) type of thermocouple are of interest, since they showed no difference between traverses of stagnation temperature across the wake behind the metal aerofoil and behind one made of tufnol, which is a good thermal insulator. These measurements therefore showed that even for a metal aerofoil the effect on the total energy of conduction across the aerofoil surface is negligible.

11. *The Results of Traverses at Different Distances behind an Aerofoil.*—Values of the drag coefficient C_D deduced from traverses 0.85 chord and 0.2 chord, respectively, behind the trailing edge of a 2-in. model of the aerofoil N.A.C.A. 0020 at zero incidence are shown in Fig. 12. The agreement is fairly satisfactory.

12. *Comparison with Drag Measured on a Balance.*—When the drag of an aerofoil is measured on the electric balance in use with the working section of the circular High-Speed Tunnel, there is an uncertain increase of drag on the end portions of the aerofoil in the tunnel boundary layer. For this reason a tapered aerofoil was selected for a comparison of the drag coefficients measured on the balance and deduced from wake explorations. The aerofoil had a chord of 2.1 in. and a thickness-chord ratio 0.37 in the middle, and a chord of 1.42 in. and a thickness-chord ratio 0.14 near the ends.* The effect of the tunnel boundary layer on the drag of this aerofoil is therefore likely to be a smaller fraction of its total drag than for an aerofoil of uniform chord and thickness.

The comparison is shown in Fig. 13. For values of M_0 between 0.3 and 0.65 the drag as measured on the balance is from 5 to 12 per cent. higher than the drag deduced from wake explorations; at $M_0 = 0.7$ the difference is almost 25 per cent. At $M_0 = 0.39, 0.55$ and 0.675 the wake explorations included traverses at a distance of only $\frac{1}{4}$ in. from the tunnel wall; these traverses suggested an upper limit to the end effects of about 25 per cent. at these speeds, and the pitot-traverse results with the maximum possible allowance for end effects are shown by crosses in Fig. 13. At higher speeds no observations were made close to the ends. The results show that, at any rate in the lower range of speeds, the discrepancy is amply accounted for by end effects.

13. *Effect of Condensed Moisture.*—Most of the experiments described in the present paper were made in the original circular High-Speed Tunnel, which drew its air supply from the interior of the compressed-air tunnel building. Effects of condensation of moisture are much more pronounced in the present circular tunnel, as a result of the fact that its air supply is drawn more nearly directly from outside the building, and also on account of its greater length of working section. It takes an appreciable fraction of a second for supersaturated air to condense into moisture.

The effect of condensation has been considered in an unpublished paper, 7482¹². It is hoped in the near future to reduce the condensation considerably by fitting return ducts to the

* Further details will be found in Reference 8.

High-Speed Tunnels, and using the relatively dry compressed-air supply. The rest of the present paper has therefore been left as originally written with the understanding that the arguments apply strictly in the absence of condensation only.

14. *Conclusion.*—Measurements of the stagnation temperature in the wake behind an aerofoil, together with theoretical arguments, suggest that it is sufficiently accurate to calculate the profile drag of an aerofoil from the results of wake measurements of total head and static pressure on the assumption that the total energy is constant. It is further assumed that for the purposes of calculation mean streamlines may be drawn in the wake along each of which the total head (or the entropy) is constant, and formulae are developed for deducing the profile drag coefficient from total-head and static-pressure traverses. Traverses at 0.85 chord and 0.20 chord behind the trailing edge of an aerofoil produced results in fairly satisfactory agreement. Discrepancies between values of the drag deduced from wake explorations and measured on a balance are satisfactorily accounted for by end effects on the portions of the aerofoil in the tunnel boundary layer.

15. *Acknowledgment.*—The authors are indebted to Miss G. Hyde for assistance in the experimental work and the reduction of the observations.

APPENDIX.

Drag in Subsonic Compressible Flow.

In two-dimensional flow past a fixed cylindrical body the drag D per unit length on the body is given by the formula

$$D = \int (p_0 - p) dy + \int \rho u(U - u) dy, \quad \dots \dots \dots (1)$$

where p and ρ are the static pressure and density of the fluid at any point, p_0 and U are the undisturbed static pressure and velocity upstream, u is the component of fluid velocity at any point parallel to the undisturbed flow, and the integrals are taken along straight lines across the wake and at right angles to the undisturbed flow.

Previously published proofs of this formula refer only to an incompressible fluid of constant density, and use the total head relation. (See, for example, reference 7.)

The following proof is simple, and is valid for subsonic compressible flow, with limited shock waves present.

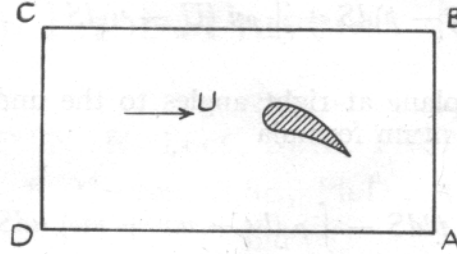
Take the axis of x in the direction of the undisturbed flow. Denote by u and v the components of fluid velocity and let

$$u = U + u'.$$

By the momentum theorem

$$\begin{aligned} D &= - \int p l ds - \int \rho(lu + mv)u ds \\ &= - \int p dy - \int \rho u^2 dy + \int \rho uvdx \quad \dots \dots \dots (2) \end{aligned}$$

round any circuit enclosing the body. (l, m denote the direction cosines of the outward-drawn normal to the circuit, and $lds = dy, mds = -dx$).



Take the integrals round a rectangle $ABCD$, where BC and AD are parallel to the axis of x , and AB cuts the wake.

By continuity

$$\int \rho (lu + mv) ds = \int \rho u dy - \int \rho v dx = 0,$$

i.e., $\int_D^A \rho v dx - \int_C^B \rho v dx = \int_A^B \rho u dy - \int_D^C \rho u dy. \quad \dots \dots \dots (3)$

From equation (2)

$$D = \int_D^C p dy - \int_A^B p dy + \int_D^C \rho u^2 dy - \int_A^B \rho u^2 dy + \int_D^A \rho u v dx - \int_C^B \rho u v dx. \quad \dots (4)$$

Also

$$\begin{aligned} \int_D^A \rho u v dx - \int_C^B \rho u v dx &= U \left[\int_D^A \rho v dx - \int_C^B \rho v dx \right] + \int_D^A \rho u' v dx - \int_C^B \rho u' v dx \\ &= U \left[\int_A^B \rho u dy - \int_D^C \rho u dy \right] + \int_D^A \rho u' v dx - \int_C^B \rho u' v dx \text{ (from (3)).} \quad \dots (5) \end{aligned}$$

Substitute from (5) into (4), and let CD tend to infinity upstream.

Then

$$\int_D^C p dy - \int_A^B p dy \rightarrow \int_A^B (p_0 - p) dy, \quad \dots \dots \dots (6)$$

and

$$\int_D^C \rho u (U - u) dy \rightarrow 0, \quad \dots \dots \dots (7)$$

since in the limit $p = p_0, u = U$ on CD . Hence

$$D = \int_A^B (p_0 - p) dy + \int_A^B \rho u (U - u) dy + \int_D^A \rho u' v dx - \int_C^B \rho u' v dx. \quad \dots (8)$$

Now let BC, AD tend to an infinite distance from the body. Then on BC and AD, u' and v are at most of order r^{-1} , where r denotes distance from a fixed point of the body. Hence

$$\int_C^B \rho u' v dx \rightarrow 0, \quad \int_D^A \rho u' v dx \rightarrow 0,$$

and

$$D = \int_A^B (p_0 - p) dy + \int_A^B \rho u (U - u) dy. \quad \dots \dots \dots (9)$$

A similar proof shows that the drag D of any solid body in three-dimensional flow is given by the formula

$$D = \int (p_0 - p) dS + \int \rho u (U - u) dS \quad \dots \quad \dots \quad \dots \quad (10)$$

where the integrals are over a plane at right angles to the undisturbed flow and cutting the wake. We start from the momentum formula

$$D = - \int p l dS - \int \rho (lu + mv + nw) u dS$$

where the integrals are over any surface S enclosing the body. For S we take a right cylinder, with its flat ends at right angles to the undisturbed flow and upstream and downstream of the body respectively. If we denote the upstream and downstream ends by 1 and 2 respectively, and the curved surface by S' , then on 1 we have $l = -1$, $m = n = 0$, on 2 we have $l = 1$, $m = n = 0$, and on S' , $l = 0$. Also by the equation of continuity

$$\int \rho (lu + mv + nw) dS = \int_2 \rho u dS - \int_1 \rho u dS + \int_{S'} \rho (mv + nw) dS = 0. \quad \dots \quad \dots \quad \dots \quad (11)$$

Hence

$$\begin{aligned} D &= \int_1 (p + \rho u^2) dS - \int_2 (p + \rho u^2) dS - \int_{S'} \rho u (mv + nw) dS \\ &= \int_1 (p + \rho u^2) dS - \int_2 (p + \rho u^2) dS - U \left[\int_1 \rho u dS - \int_2 \rho u dS \right] \\ &\quad - \int_{S'} \rho u' (mv + nw) dS. \quad \dots \quad \dots \quad \dots \quad \dots \quad \dots \quad \dots \quad (12) \end{aligned}$$

Now let the upstream end of the cylinder tend to infinity. Then

$$D = \int_2 (p_0 - p) dS + \int_2 \rho u (U - u) dS - \int_{S'} \rho u' (mv + nw) dS \quad \dots \quad (13)$$

Finally let the curved surface tend to infinity. On the curved surface u', v, w are at most of order r^{-2} , and

$$\int_{S'} \rho u' (mv + nw) dS = 0.$$

Hence

$$D = \int_2 (p_0 - p) dS + \int_2 \rho u (U - u) dS. \quad \dots \quad \dots \quad \dots \quad \dots \quad (14)$$

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TABLE 1

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
0.001	100	0.030	98	0.059	96	0.088	95	0.117	92
0.002	100	0.031	98	0.060	96	0.089	94	0.118	93
0.003	100	0.032	98	0.061	96	0.090	94	0.119	92
0.004	99	0.033	98	0.062	95	0.091	94	0.120	92
0.005	100	0.034	98	0.063	96	0.092	94	0.121	92
0.006	100	0.035	97	0.064	95	0.093	94	0.122	93
0.007	99	0.036	98	0.065	96	0.094	93	0.123	92
0.008	100	0.037	97	0.066	96	0.095	94	0.124	92
0.009	99	0.038	98	0.067	96	0.096	94	0.125	92
0.010	99	0.039	97	0.068	95	0.097	93	0.126	92
0.011	100	0.040	97	0.069	95	0.098	94	0.127	91
0.012	99	0.041	97	0.070	96	0.099	94	0.128	92
0.013	99	0.042	97	0.071	95	0.100	93	0.129	92
0.014	99	0.043	98	0.072	95	0.101	93	0.130	92
0.015	99	0.044	97	0.073	95	0.102	94	0.131	91
0.016	99	0.045	96	0.074	95	0.103	93	0.132	92
0.017	99	0.046	97	0.075	95	0.104	93	0.133	91
0.018	98	0.047	97	0.076	95	0.105	93	0.134	92
0.019	99	0.048	97	0.077	95	0.106	93	0.135	91
0.020	98	0.049	96	0.078	95	0.107	93	0.136	92
0.021	99	0.050	97	0.079	94	0.108	93	0.137	91
0.022	98	0.051	96	0.080	95	0.109	93	0.138	91
0.023	99	0.052	97	0.081	95	0.110	93	0.139	91
0.024	98	0.053	96	0.082	94	0.111	93	0.140	91
0.025	98	0.054	96	0.083	94	0.112	92	0.141	91
0.026	98	0.055	96	0.084	95	0.113	93	0.142	91
0.027	98	0.056	97	0.085	94	0.114	92	0.143	91
0.028	98	0.057	96	0.086	94	0.115	93	0.144	91
0.029		0.058		0.087		0.116		0.145	

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 TABLE 1—contd.

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
0.146	0.13897 ⁹¹	0.175	0.16504 ⁸⁹	0.204	0.19066 ⁸⁸	0.233	0.21585 ⁸⁷	0.262	0.24061 ⁸⁵
0.147	0.13987 ⁹⁰	0.176	0.16593 ⁸⁹	0.205	0.19154 ⁸⁸	0.234	0.21671 ⁸⁶	0.263	0.24145 ⁸⁴
0.148	0.14078 ⁹¹	0.177	0.16682 ⁸⁹	0.206	0.19241 ⁸⁷	0.235	0.21757 ⁸⁶	0.264	0.24230 ⁸⁵
0.149	0.14168 ⁹⁰	0.178	0.16771 ⁸⁹	0.207	0.19329 ⁸⁸	0.236	0.21842 ⁸⁵	0.265	0.24315 ⁸⁵
0.150	0.14259 ⁹¹	0.179	0.16860 ⁸⁹	0.208	0.19416 ⁸⁷	0.237	0.21928 ⁸⁶	0.266	0.24399 ⁸⁴
0.151	0.14349 ⁹⁰	0.180	0.16949 ⁸⁹	0.209	0.19503 ⁸⁷	0.238	0.22014 ⁸⁶	0.267	0.24484 ⁸⁵
0.152	0.14440 ⁹¹	0.181	0.17038 ⁸⁹	0.210	0.19591 ⁸⁸	0.239	0.22100 ⁸⁶	0.268	0.24568 ⁸⁴
0.153	0.14530 ⁹⁰	0.182	0.17127 ⁸⁹	0.211	0.19678 ⁸⁷	0.240	0.22186 ⁸⁶	0.269	0.24652 ⁸⁴
0.154	0.14621 ⁹¹	0.183	0.17215 ⁸⁸	0.212	0.19765 ⁸⁷	0.241	0.22272 ⁸⁶	0.270	0.24737 ⁸⁵
0.155	0.14711 ⁹⁰	0.184	0.17304 ⁸⁹	0.213	0.19852 ⁸⁷	0.242	0.22357 ⁸⁵	0.271	0.24821 ⁸⁴
0.156	0.14801 ⁹⁰	0.185	0.17393 ⁸⁹	0.214	0.19939 ⁸⁷	0.243	0.22443 ⁸⁶	0.272	0.24905 ⁸⁴
0.157	0.14891 ⁹⁰	0.186	0.17481 ⁸⁸	0.215	0.20026 ⁸⁷	0.244	0.22528 ⁸⁵	0.273	0.24989 ⁸⁴
0.158	0.14981 ⁹⁰	0.187	0.17570 ⁸⁹	0.216	0.20113 ⁸⁷	0.245	0.22614 ⁸⁶	0.274	0.25073 ⁸⁴
0.159	0.15071 ⁹⁰	0.188	0.17658 ⁸⁸	0.217	0.20200 ⁸⁷	0.246	0.22700 ⁸⁶	0.275	0.25157 ⁸⁵
0.160	0.15161 ⁹⁰	0.189	0.17747 ⁸⁹	0.218	0.20287 ⁸⁷	0.247	0.22785 ⁸⁵	0.276	0.25242 ⁸⁴
0.161	0.15251 ⁹⁰	0.190	0.17835 ⁸⁸	0.219	0.20374 ⁸⁷	0.248	0.22870 ⁸⁶	0.277	0.25326 ⁸⁴
0.162	0.15341 ⁹⁰	0.191	0.17923 ⁸⁸	0.220	0.20461 ⁸⁷	0.249	0.22956 ⁸⁵	0.278	0.25410 ⁸³
0.163	0.15431 ⁹⁰	0.192	0.18011 ⁸⁹	0.221	0.20548 ⁸⁶	0.250	0.23041 ⁸⁵	0.279	0.25493 ⁸⁴
0.164	0.15521 ⁸⁹	0.192	0.18100 ⁸⁸	0.222	0.20634 ⁸⁷	0.251	0.23126 ⁸⁶	0.280	0.25577 ⁸⁴
0.165	0.15610 ⁹⁰	0.194	0.18188 ⁸⁸	0.223	0.20721 ⁸⁶	0.252	0.23212 ⁸⁵	0.281	0.25661 ⁸⁴
0.166	0.15700 ⁸⁹	0.195	0.18276 ⁸⁸	0.224	0.20807 ⁸⁷	0.253	0.23297 ⁸⁵	0.282	0.25745 ⁸⁴
0.167	0.15789 ⁹⁰	0.196	0.18364 ⁸⁸	0.225	0.20894 ⁸⁶	0.254	0.23382 ⁸⁵	0.283	0.25829 ⁸³
0.168	0.15879 ⁸⁹	0.197	0.18452 ⁸⁸	0.226	0.20980 ⁸⁷	0.255	0.23467 ⁸⁵	0.284	0.25912 ⁸⁴
0.169	0.15968 ⁹⁰	0.198	0.18540 ⁸⁸	0.227	0.21067 ⁸⁶	0.256	0.23552 ⁸⁵	0.285	0.25996 ⁸⁴
0.170	0.16058 ⁸⁹	0.199	0.18628 ⁸⁷	0.228	0.21153 ⁸⁷	0.257	0.23637 ⁸⁵	0.286	0.26080 ⁸³
0.171	0.16147 ⁹⁰	0.200	0.18715 ⁸⁸	0.229	0.21240 ⁸⁶	0.258	0.23722 ⁸⁴	0.287	0.26163 ⁸⁴
0.172	0.16237 ⁸⁹	0.201	0.18803 ⁸⁸	0.230	0.21326 ⁸⁶	0.259	0.23806 ⁸⁵	0.288	0.26247 ⁸³
0.173	0.16326 ⁸⁹	0.202	0.18891 ⁸⁷	0.231	0.21412 ⁸⁶	0.260	0.23891 ⁸⁵	0.289	0.26330 ⁸³
0.174	0.16415	0.203	0.18978	0.232	0.21498	0.261	0.23976	0.290	0.26413

TABLE 1—*contd.*

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
0.291	0.26497 ⁸⁴	0.320	0.28894 ⁸²	0.349	0.31254 ⁸¹	0.378	0.33578 ⁸⁰	0.407	0.35867 ⁷⁸
0.292	0.26580 ⁸³	0.321	0.28976 ⁸²	0.350	0.31335 ⁸¹	0.379	0.33657 ⁷⁹	0.408	0.35946 ⁷⁹
0.293	0.26663 ⁸³	0.322	0.29058 ⁸²	0.351	0.31415 ⁸⁰	0.380	0.33737 ⁸⁰	0.409	0.36024 ⁷⁸
0.294	0.26747 ⁸⁴	0.323	0.29140 ⁸²	0.352	0.31496 ⁸¹	0.381	0.33816 ⁷⁹	0.410	0.36102 ⁷⁸
0.295	0.26830 ⁸³	0.324	0.29222 ⁸²	0.353	0.31577 ⁸¹	0.382	0.33896 ⁸⁰	0.411	0.36180 ⁷⁸
0.296	0.26913 ⁸³	0.325	0.29303 ⁸¹	0.354	0.31657 ⁸⁰	0.383	0.33975 ⁷⁹	0.412	0.36259 ⁷⁹
0.297	0.26996 ⁸³	0.326	0.29385 ⁸²	0.355	0.31738 ⁸¹	0.384	0.34054 ⁷⁹	0.413	0.36337 ⁷⁸
0.298	0.27079 ⁸³	0.327	0.29467 ⁸²	0.356	0.31818 ⁸⁰	0.385	0.34134 ⁸⁰	0.414	0.36415 ⁷⁸
0.299	0.27162 ⁸³	0.328	0.29549 ⁸²	0.357	0.31898 ⁸⁰	0.386	0.34213 ⁷⁹	0.415	0.36493 ⁷⁸
0.300	0.27245 ⁸³	0.329	0.29630 ⁸¹	0.358	0.31979 ⁸¹	0.387	0.34292 ⁷⁹	0.416	0.36571 ⁷⁸
0.301	0.27328 ⁸³	0.330	0.29712 ⁸²	0.359	0.32059 ⁸⁰	0.388	0.34371 ⁷⁹	0.417	0.36649 ⁷⁸
0.302	0.27411 ⁸³	0.331	0.29793 ⁸¹	0.360	0.32139 ⁸⁰	0.389	0.34450 ⁷⁹	0.418	0.36727 ⁷⁸
0.303	0.27493 ⁸²	0.332	0.29875 ⁸²	0.361	0.32220 ⁸¹	0.390	0.34529 ⁷⁹	0.419	0.36804 ⁷⁷
0.304	0.27576 ⁸³	0.333	0.29957 ⁸²	0.362	0.32300 ⁸⁰	0.391	0.34608 ⁷⁹	0.420	0.36882 ⁷⁸
0.305	0.27659 ⁸³	0.334	0.30038 ⁸¹	0.363	0.32380 ⁸⁰	0.392	0.34687 ⁷⁹	0.421	0.36960 ⁷⁸
0.306	0.27741 ⁸²	0.335	0.30119 ⁸¹	0.364	0.32460 ⁸⁰	0.393	0.34766 ⁷⁹	0.422	0.37038 ⁷⁸
0.307	0.27824 ⁸³	0.336	0.30201 ⁸²	0.365	0.32540 ⁸⁰	0.394	0.34845 ⁷⁹	0.423	0.37116 ⁷⁸
0.308	0.27907 ⁸³	0.337	0.30282 ⁸¹	0.366	0.32620 ⁸⁰	0.395	0.34924 ⁷⁹	0.424	0.37193 ⁷⁷
0.309	0.27989 ⁸²	0.338	0.30363 ⁸¹	0.367	0.32700 ⁸⁰	0.396	0.35003 ⁷⁹	0.425	0.37271 ⁷⁸
0.310	0.28072 ⁸³	0.339	0.30444 ⁸¹	0.368	0.32780 ⁸⁰	0.397	0.35082 ⁷⁹	0.426	0.37349 ⁷⁸
0.311	0.28154 ⁸²	0.340	0.30526 ⁸²	0.369	0.32860 ⁸⁰	0.398	0.35160 ⁷⁸	0.427	0.37426 ⁷⁷
0.312	0.28237 ⁸³	0.341	0.30607 ⁸¹	0.370	0.32940 ⁸⁰	0.399	0.35239 ⁷⁹	0.428	0.37504 ⁷⁸
0.313	0.28319 ⁸²	0.342	0.30688 ⁸¹	0.371	0.33020 ⁸⁰	0.400	0.35318 ⁷⁹	0.429	0.37581 ⁷⁷
0.314	0.28401 ⁸²	0.343	0.30769 ⁸¹	0.372	0.33100 ⁸⁰	0.401	0.35396 ⁷⁸	0.430	0.37659 ⁷⁸
0.315	0.28483 ⁸³	0.344	0.30850 ⁸¹	0.373	0.33180 ⁸⁰	0.402	0.35475 ⁷⁹	0.431	0.37736 ⁷⁷
0.316	0.28566 ⁸³	0.345	0.30931 ⁸¹	0.374	0.33259 ⁷⁹	0.403	0.35554 ⁷⁹	0.432	0.37814 ⁷⁸
0.317	0.28648 ⁸²	0.346	0.31012 ⁸¹	0.375	0.33339 ⁸⁰	0.404	0.35632 ⁷⁸	0.433	0.37891 ⁷⁷
0.318	0.28730 ⁸²	0.347	0.31093 ⁸¹	0.376	0.33419 ⁸⁰	0.405	0.35711 ⁷⁹	0.434	0.37968 ⁷⁷
0.319	0.28812 ⁸²	0.348	0.31173 ⁸⁰	0.377	0.33498 ⁷⁹	0.406	0.35789 ⁷⁸	0.435	0.38046 ⁷⁸

TABLE 1—*contd.*

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
	77		76		75		74		73
0.436	0.38123	0.465	0.40346	0.494	0.42539	0.523	0.44701	0.552	0.46834
	77		77		75		74		73
0.437	0.38200	0.466	0.40423	0.495	0.42614	0.524	0.44775	0.553	0.46907
	77		76		75		74		73
0.438	0.38277	0.467	0.40499	0.496	0.42689	0.525	0.44849	0.554	0.46980
	77		76		75		74		73
0.439	0.38354	0.468	0.40575	0.497	0.42764	0.526	0.44923	0.555	0.47053
	77		76		75		74		73
0.440	0.38431	0.469	0.40651	0.498	0.42839	0.527	0.44997	0.556	0.47126
	77		76		75		74		73
0.441	0.38508	0.470	0.40727	0.499	0.42914	0.528	0.45071	0.557	0.47199
	77		76		74		73		72
0.442	0.38585	0.471	0.40803	0.500	0.42988	0.529	0.45144	0.558	0.47271
	77		76		75		74		73
0.443	0.38662	0.472	0.40879	0.501	0.43063	0.530	0.45218	0.559	0.47344
	77		75		75		74		73
0.444	0.38739	0.473	0.40954	0.502	0.43138	0.531	0.45292	0.560	0.47417
	77		76		75		74		73
0.445	0.38816	0.474	0.41030	0.503	0.43213	0.532	0.45366	0.561	0.47490
	77		76		75		74		73
0.446	0.38893	0.475	0.41106	0.504	0.43288	0.533	0.45440	0.562	0.47563
	77		76		74		73		72
0.447	0.38970	0.476	0.41182	0.505	0.43362	0.534	0.45513	0.563	0.47635
	77		75		75		74		73
0.448	0.39047	0.477	0.41257	0.506	0.43437	0.535	0.45587	0.564	0.47708
	77		76		75		74		72
0.449	0.39124	0.478	0.41333	0.507	0.43512	0.536	0.45661	0.565	0.47780
	76		76		74		73		73
0.450	0.39200	0.479	0.41409	0.508	0.43586	0.537	0.45734	0.566	0.47853
	77		75		75		74		73
0.451	0.39277	0.480	0.41484	0.509	0.43661	0.538	0.45808	0.567	0.47926
	77		75		74		73		72
0.452	0.39354	0.481	0.41559	0.510	0.43735	0.539	0.45881	0.568	0.47998
	76		76		75		74		73
0.453	0.39430	0.482	0.41635	0.511	0.43810	0.540	0.45955	0.569	0.48071
	77		76		74		73		72
0.454	0.39507	0.483	0.41711	0.512	0.43884	0.541	0.46028	0.570	0.48143
	76		75		74		74		73
0.455	0.39583	0.484	0.41786	0.513	0.43958	0.542	0.46102	0.571	0.48216
	77		76		75		73		72
0.456	0.39660	0.485	0.41862	0.514	0.44033	0.543	0.46175	0.572	0.48288
	76		75		74		73		73
0.457	0.39736	0.486	0.41937	0.515	0.44107	0.544	0.46248	0.573	0.48361
	77		75		75		74		72
0.458	0.39813	0.487	0.42012	0.516	0.44182	0.545	0.46322	0.574	0.48433
	76		76		74		73		72
0.459	0.39889	0.488	0.42088	0.517	0.44256	0.546	0.46395	0.575	0.48505
	76		75		74		73		73
0.460	0.39965	0.489	0.42163	0.518	0.44330	0.547	0.46468	0.576	0.48578
	77		75		74		73		72
0.461	0.40042	0.490	0.42238	0.519	0.44404	0.548	0.46541	0.577	0.48650
	76		75		74		73		72
0.462	0.40118	0.491	0.42313	0.520	0.44478	0.549	0.46614	0.578	0.48722
	76		76		75		74		72
0.463	0.40194	0.492	0.42389	0.521	0.44553	0.550	0.46688	0.579	0.48794
	76		75		74		73		72
0.464	0.40270	0.493	0.42464	0.522	0.44627	0.551	0.46761	0.580	0.48866

TABLE 1—contd.

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
0.581	0.48938 ⁷²	0.610	0.51016 ⁷²	0.639	0.53066 ⁷⁰	0.668	0.55091 ⁶⁹	0.697	0.57091 ⁶⁹
0.582	0.49011 ⁷³	0.611	0.51087 ⁷¹	0.640	0.53136 ⁷⁰	0.669	0.55160 ⁶⁹	0.698	0.57159 ⁶⁸
0.583	0.49083 ⁷²	0.612	0.51158 ⁷¹	0.641	0.53207 ⁷¹	0.670	0.55230 ⁷⁰	0.699	0.57228 ⁶⁹
0.584	0.49155 ⁷²	0.613	0.51229 ⁷¹	0.642	0.53277 ⁷⁰	0.671	0.55299 ⁶⁹	0.700	0.57296 ⁶⁸
0.585	0.49227 ⁷²	0.614	0.51300 ⁷¹	0.643	0.53347 ⁷⁰	0.672	0.55368 ⁶⁹	0.701	0.57365 ⁶⁹
0.586	0.49299 ⁷¹	0.615	0.51371 ⁷¹	0.644	0.53417 ⁷⁰	0.673	0.55438 ⁷⁰	0.702	0.57433 ⁶⁸
0.587	0.49370 ⁷²	0.616	0.51442 ⁷¹	0.645	0.53487 ⁷⁰	0.674	0.55507 ⁶⁹	0.703	0.57502 ⁶⁹
0.588	0.49442 ⁷²	0.617	0.51513 ⁷¹	0.646	0.53557 ⁷⁰	0.675	0.55576 ⁶⁹	0.704	0.57570 ⁶⁸
0.589	0.49514 ⁷²	0.618	0.51584 ⁷¹	0.647	0.53627 ⁷⁰	0.676	0.55645 ⁶⁹	0.705	0.57638 ⁶⁹
0.590	0.49586 ⁷²	0.619	0.51655 ⁷¹	0.648	0.53697 ⁷⁰	0.677	0.55714 ⁶⁹	0.706	0.57707 ⁶⁸
0.591	0.49658 ⁷¹	0.620	0.51726 ⁷⁰	0.649	0.53767 ⁷⁰	0.678	0.55783 ⁶⁹	0.707	0.57775 ⁶⁸
0.592	0.49729 ⁷²	0.621	0.51796 ⁷¹	0.650	0.53837 ⁷⁰	0.679	0.55852 ⁷⁰	0.708	0.57843 ⁶⁸
0.592	0.49801 ⁷²	0.622	0.51867 ⁷¹	0.651	0.53907 ⁷⁰	0.680	0.55922 ⁶⁹	0.709	0.57911 ⁶⁹
0.594	0.49873 ⁷¹	0.623	0.51938 ⁷¹	0.652	0.53977 ⁷⁰	0.681	0.55991 ⁶⁹	0.710	0.57980 ⁶⁸
0.595	0.49944 ⁷²	0.624	0.52009 ⁷⁰	0.653	0.54047 ⁷⁰	0.682	0.56060 ⁶⁹	0.711	0.58048 ⁶⁸
0.596	0.50016 ⁷²	0.625	0.52079 ⁷¹	0.654	0.54117 ⁷⁰	0.683	0.56129 ⁶⁸	0.712	0.58116 ⁶⁸
0.597	0.50088 ⁷¹	0.626	0.52150 ⁷¹	0.655	0.54186 ⁷⁰	0.684	0.56197 ⁶⁹	0.713	0.58184 ⁶⁸
0.598	0.50159 ⁷²	0.627	0.52221 ⁷⁰	0.656	0.54256 ⁷⁰	0.685	0.56266 ⁶⁹	0.714	0.58252 ⁶⁸
0.599	0.50231 ⁷¹	0.628	0.52291 ⁷¹	0.657	0.54326 ⁶⁹	0.686	0.56335 ⁶⁹	0.715	0.58320 ⁶⁸
0.600	0.50302 ⁷²	0.629	0.52362 ⁷¹	0.658	0.54395 ⁷⁰	0.687	0.56404 ⁶⁹	0.716	0.58388 ⁶⁸
0.601	0.50374 ⁷¹	0.630	0.52433 ⁷⁰	0.659	0.54465 ⁷⁰	0.688	0.56473 ⁶⁹	0.717	0.58456 ⁶⁸
0.602	0.50445 ⁷²	0.631	0.52503 ⁷¹	0.660	0.54535 ⁷⁰	0.689	0.56542 ⁶⁸	0.718	0.58524 ⁶⁸
0.603	0.50517 ⁷¹	0.632	0.52574 ⁷⁰	0.661	0.54605 ⁶⁹	0.690	0.56610 ⁶⁹	0.719	0.58592 ⁶⁸
0.604	0.50588 ⁷¹	0.633	0.52644 ⁷⁰	0.662	0.54674 ⁷⁰	0.691	0.56679 ⁶⁹	0.720	0.58660 ³³⁹
0.605	0.50659 ⁷²	0.634	0.52714 ⁷¹	0.663	0.54744 ⁶⁹	0.692	0.56748 ⁶⁸	0.725	0.58999 ³³⁸
0.606	0.50731 ⁷¹	0.635	0.52785 ⁷⁰	0.664	0.54813 ⁷⁰	0.693	0.56816 ⁶⁹	0.730	0.59337 ³³⁸
0.607	0.50802 ⁷¹	0.636	0.52855 ⁷¹	0.665	0.54883 ⁶⁹	0.694	0.56885 ⁶⁹	0.735	0.59675 ³³⁷
0.608	0.50873 ⁷¹	0.637	0.52926 ⁷⁰	0.666	0.54952 ⁷⁰	0.695	0.56954 ⁶⁸	0.740	0.60012 ³³⁶
0.609	0.50944	0.638	0.52996	0.667	0.55022	0.696	0.57022	0.745	0.60348

TABLE 1—*contd.*

x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$	x	$\lambda(x)$
0.750	0.60684 ³³⁶	0.785	0.63014 ³³¹	0.820	0.65311 ³²⁶	0.855	0.67578 ³²²	0.890	0.69814 ³¹⁸
0.755	0.61019 ³³⁵	0.790	0.63344 ³³⁰	0.825	0.65637 ³²⁶	0.860	0.67899 ³²¹	0.895	0.70131 ³¹⁷
0.760	0.61353 ³³⁴	0.795	0.63673 ³²⁹	0.830	0.65962 ³²⁵	0.865	0.68220 ³²¹	0.900	0.70448 ³¹⁷
0.765	0.61686 ³³³	0.800	0.64002 ³²⁹	0.835	0.66287 ³²⁵	0.870	0.68540 ³²⁰		
0.770	0.62019 ³³³	0.805	0.64331 ³²⁹	0.840	0.66610 ³²³	0.875	0.68859 ³¹⁹		
0.775	0.62352 ³³³	0.810	0.64658 ³²⁷	0.845	0.66934 ³²⁴	0.880	0.69178 ³¹⁹		
0.780	0.62683 ³³¹	0.815	0.64985 ³²⁷	0.850	0.67256 ³²²	0.885	0.69496 ³¹⁸		

TABLE 1a

Table of Proportional Parts for use with Tables 1 and 3.

	$\times 0.1$	$\times 0.2$	$\times 0.3$	$\times 0.4$	$\times 0.5$	$\times 0.6$	$\times 0.7$	$\times 0.8$	$\times 0.9$
68	7	14	20	27	34	41	48	54	61
69	7	14	21	28	34 ₅	41	48	55	62
70	7	14	21	28	35	42	49	56	63
71	7	14	21	28	35 ₅	43	50	57	64
72	7	14	22	29	36	43	50	58	65
73	7	15	22	29	36 ₅	44	51	58	66
74	7	15	22	30	37	44	52	59	67
75	7 ₅	15	22 ₅	30	37 ₅	45	52 ₅	60	67 ₅
76	8	15	23	30	38	46	53	61	68
77	8	15	23	31	38 ₅	46	54	62	69
78	8	16	23	31	39	47	55	62	70
79	8	16	24	32	39 ₅	47	55	63	71
80	8	16	24	32	40	48	56	64	72
81	8	16	24	32	40 ₅	49	57	65	73
82	8	16	25	33	41	49	57	66	74
83	8	17	25	33	41 ₅	50	58	66	75
84	8	17	25	34	42	50	59	67	76
85	8 ₅	17	25 ₅	34	42 ₅	51	59 ₅	68	76 ₅
86	9	17	26	34	43	52	60	69	77
87	9	17	26	35	43 ₅	52	61	70	78
88	9	18	26	35	44	53	62	70	79
89	9	18	27	36	44 ₅	53	62	71	80
90	9	18	27	36	45	54	63	72	81
91	9	18	27	36	45 ₅	55	64	73	82
92	9	18	28	37	46	55	64	74	83
93	9	19	28	37	46 ₅	56	65	74	84
94	9	19	28	38	47	56	66	75	85
95	9 ₅	19	28 ₅	38	47 ₅	57	66 ₅	76	85 ₅
96	10	19	29	38	48	58	67	77	86
97	10	19	29	39	48 ₅	58	68	78	87
98	10	20	29	39	49	59	69	78	88
99	10	20	30	40	49 ₅	59	69	79	89
100	10	20	30	40	50	60	70	80	90

TABLE 2

H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$
0.800	0.96863 ¹⁷	0.829	0.97357 ¹⁷	0.858	0.97836 ¹⁷	0.887	0.98302 ¹⁶	0.916	0.98754 ¹⁵
0.801	0.96880 ¹⁷	0.830	0.97373 ¹⁶	0.859	0.97852 ¹⁶	0.888	0.98317 ¹⁵	0.917	0.98770 ¹⁶
0.802	0.96897 ¹⁷	0.831	0.97390 ¹⁷	0.860	0.97868 ¹⁶	0.889	0.98333 ¹⁶	0.918	0.98785 ¹⁵
0.803	0.96914 ¹⁷	0.832	0.97407 ¹⁷	0.861	0.97885 ¹⁷	0.890	0.98349 ¹⁶	0.919	0.98801 ¹⁶
0.804	0.96932 ¹⁸	0.833	0.97423 ¹⁶	0.862	0.97901 ¹⁶	0.891	0.98365 ¹⁶	0.920	0.98816 ¹⁵
0.805	0.96949 ¹⁷	0.834	0.97440 ¹⁷	0.863	0.97917 ¹⁶	0.892	0.98381 ¹⁶	0.921	0.98831 ¹⁵
0.806	0.96966 ¹⁷	0.835	0.97457 ¹⁷	0.864	0.97933 ¹⁶	0.893	0.98396 ¹⁵	0.922	0.98847 ¹⁶
0.807	0.96983 ¹⁷	0.836	0.97474 ¹⁷	0.865	0.97950 ¹⁷	0.894	0.98412 ¹⁶	0.923	0.98862 ¹⁵
0.808	0.97000 ¹⁷	0.837	0.97490 ¹⁶	0.866	0.97966 ¹⁶	0.895	0.98428 ¹⁶	0.924	0.98877 ¹⁵
0.809	0.97017 ¹⁷	0.838	0.97507 ¹⁷	0.867	0.97982 ¹⁶	0.896	0.98443 ¹⁵	0.925	0.98892 ¹⁵
0.810	0.97035 ¹⁸	0.839	0.97523 ¹⁶	0.868	0.97998 ¹⁶	0.897	0.98459 ¹⁶	0.926	0.98908 ¹⁶
0.811	0.97052 ¹⁷	0.840	0.97540 ¹⁷	0.869	0.98014 ¹⁶	0.898	0.98475 ¹⁶	0.927	0.98923 ¹⁵
0.812	0.97069 ¹⁷	0.841	0.97557 ¹⁷	0.870	0.98030 ¹⁶	0.899	0.98490 ¹⁵	0.928	0.98938 ¹⁵
0.813	0.97086 ¹⁷	0.842	0.97573 ¹⁶	0.871	0.98046 ¹⁶	0.900	0.98506 ¹⁶	0.929	0.98953 ¹⁵
0.814	0.97103 ¹⁷	0.843	0.97590 ¹⁷	0.872	0.98062 ¹⁶	0.901	0.98522 ¹⁶	0.930	0.98969 ¹⁶
0.815	0.97120 ¹⁷	0.844	0.97606 ¹⁶	0.873	0.98078 ¹⁶	0.902	0.98537 ¹⁵	0.931	0.98984 ¹⁵
0.816	0.97137 ¹⁷	0.845	0.97623 ¹⁷	0.874	0.98094 ¹⁶	0.903	0.98553 ¹⁶	0.932	0.98999 ¹⁵
0.817	0.97154 ¹⁷	0.846	0.97639 ¹⁶	0.875	0.98110 ¹⁶	0.904	0.98569 ¹⁶	0.933	0.99014 ¹⁵
0.818	0.97171 ¹⁷	0.847	0.97656 ¹⁷	0.876	0.98127 ¹⁷	0.905	0.98584 ¹⁵	0.934	0.99029 ¹⁵
0.819	0.97188 ¹⁷	0.848	0.97672 ¹⁶	0.877	0.98143 ¹⁶	0.906	0.98600 ¹⁶	0.935	0.99045 ¹⁶
0.820	0.97205 ¹⁷	0.849	0.97689 ¹⁷	0.878	0.98158 ¹⁵	0.907	0.98615 ¹⁵	0.936	0.99060 ¹⁵
0.821	0.97222 ¹⁷	0.850	0.97705 ¹⁶	0.879	0.98174 ¹⁶	0.908	0.98631 ¹⁶	0.937	0.99075 ¹⁵
0.822	0.97239 ¹⁷	0.851	0.97721 ¹⁶	0.880	0.98190 ¹⁶	0.909	0.98646 ¹⁵	0.938	0.99090 ¹⁵
0.823	0.97256 ¹⁷	0.852	0.97738 ¹⁷	0.881	0.98206 ¹⁶	0.910	0.98662 ¹⁶	0.939	0.99105 ¹⁵
0.824	0.97272 ¹⁶	0.853	0.97754 ¹⁶	0.882	0.98222 ¹⁶	0.911	0.98677 ¹⁵	0.940	0.99120 ¹⁵
0.825	0.97289 ¹⁷	0.854	0.97771 ¹⁷	0.883	0.98238 ¹⁶	0.912	0.98693 ¹⁶	0.941	0.99135 ¹⁵
0.826	0.97306 ¹⁷	0.855	0.97787 ¹⁶	0.884	0.98254 ¹⁶	0.913	0.98708 ¹⁵	0.942	0.99150 ¹⁵
0.827	0.97323 ¹⁷	0.856	0.97803 ¹⁶	0.885	0.98270 ¹⁶	0.914	0.98724 ¹⁶	0.943	0.99165 ¹⁵
0.828	0.97340 ¹⁷	0.857	0.97819 ¹⁶	0.886	0.98286 ¹⁶	0.915	0.98739 ¹⁵	0.944	0.99180 ¹⁵

TABLE 2—*contd.*

H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$	H_1/H_0	$(H_1/H_0)^{1/7}$
0.945	0.99195 ¹⁵	0.957	0.99374 ¹⁵	0.969	0.99551 ¹⁵	0.981	0.99726 ¹⁴	0.993	0.99900 ¹⁵
0.946	0.99210 ¹⁵	0.958	0.99389 ¹⁵	0.970	0.99566 ¹⁵	0.982	0.99741 ¹⁵	0.994	0.99914 ¹⁴
0.947	0.99225 ¹⁵	0.959	0.99404 ¹⁵	0.971	0.99580 ¹⁴	0.983	0.99755 ¹⁴	0.995	0.99928 ¹⁴
0.948	0.99240 ¹⁵	0.960	0.99419 ¹⁵	0.972	0.99595 ¹⁵	0.984	0.99770 ¹⁵	0.996	0.99943 ¹⁵
0.949	0.99255 ¹⁵	0.961	0.99433 ¹⁴	0.973	0.99610 ¹⁵	0.985	0.99784 ¹⁴	0.997	0.99957 ¹⁴
0.950	0.99270 ¹⁵	0.962	0.99448 ¹⁵	0.974	0.99624 ¹⁴	0.986	0.99799 ¹⁵	0.998	0.99971 ¹⁴
0.951	0.99285 ¹⁵	0.963	0.99463 ¹⁵	0.975	0.99639 ¹⁵	0.987	0.99813 ¹⁴	0.999	0.99986 ¹⁵
0.952	0.99300 ¹⁵	0.964	0.99478 ¹⁵	0.976	0.99654 ¹⁵	0.988	0.99828 ¹⁵	1.000	1.00000 ¹⁴
0.953	0.99315 ¹⁵	0.965	0.99492 ¹⁴	0.977	0.99668 ¹⁴	0.989	0.99842 ¹⁴		
0.954	0.99329 ¹⁴	0.966	0.99507 ¹⁵	0.978	0.99683 ¹⁵	0.990	0.99857 ¹⁵		
0.955	0.99344 ¹⁵	0.967	0.99522 ¹⁵	0.979	0.99697 ¹⁴	0.991	0.99871 ¹⁴		
0.956	0.99359 ¹⁵	0.968	0.99536 ¹⁴	0.980	0.99712 ¹⁵	0.992	0.99885 ¹⁴		

TABLE 2a

Table of Proportional Parts for Use with Table 2

	$\times 0.1$	$\times 0.2$	$\times 0.3$	$\times 0.4$	$\times 0.5$	$\times 0.6$	$\times 0.7$	$\times 0.8$	$\times 0.9$
14	1	3	4	6	7	8	10	11	13
15	1 ₅	3	4 ₅	6	7 ₅	9	10 ₅	12	13 ₅
16	2	3	5	6	8	10	11	13	14
17	2	3	5	7	8 ₅	10	12	14	15

TABLE 3

P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$
0.800	0.82591 ⁸⁹	0.829	0.85151 ⁸⁸	0.858	0.87698 ⁸⁸	0.887	0.90233 ⁸⁸	0.916	0.92755 ⁸⁶
0.801	0.82680 ⁸⁸	0.830	0.85239 ⁸⁸	0.859	0.87786 ⁸⁸	0.888	0.90320 ⁸⁷	0.917	0.92842 ⁸⁷
0.802	0.82768 ⁸⁹	0.831	0.85327 ⁸⁸	0.860	0.87873 ⁸⁷	0.889	0.90407 ⁸⁷	0.918	0.92929 ⁸⁷
0.803	0.82857 ⁸⁸	0.832	0.85415 ⁸⁸	0.861	0.87961 ⁸⁸	0.890	0.90494 ⁸⁷	0.919	0.93016 ⁸⁷
0.804	0.82945 ⁸⁹	0.833	0.85503 ⁸⁸	0.862	0.88048 ⁸⁸	0.891	0.90581 ⁸⁷	0.920	0.93102 ⁸⁶
0.805	0.83034 ⁸⁸	0.834	0.85591 ⁸⁸	0.863	0.88136 ⁸⁷	0.892	0.90668 ⁸⁷	0.921	0.93189 ⁸⁷
0.806	0.83122 ⁸⁸	0.835	0.85679 ⁸⁸	0.864	0.88223 ⁸⁸	0.893	0.90755 ⁸⁸	0.922	0.93276 ⁸⁷
0.807	0.83210 ⁸⁹	0.836	0.85767 ⁸⁸	0.865	0.88311 ⁸⁷	0.894	0.90843 ⁸⁷	0.923	0.93363 ⁸⁶
0.808	0.83299 ⁸⁸	0.837	0.85855 ⁸⁸	0.866	0.88398 ⁸⁸	0.895	0.90930 ⁸⁷	0.924	0.93449 ⁸⁷
0.809	0.83387 ⁸⁸	0.838	0.85943 ⁸⁸	0.867	0.88486 ⁸⁷	0.896	0.91017 ⁸⁷	0.925	0.93536 ⁸⁶
0.810	0.83475 ⁸⁹	0.839	0.86031 ⁸⁸	0.868	0.88573 ⁸⁸	0.897	0.91104 ⁸⁷	0.926	0.93622 ⁸⁷
0.811	0.83564 ⁸⁸	0.840	0.86119 ⁸⁷	0.869	0.88661 ⁸⁷	0.898	0.91191 ⁸⁷	0.927	0.93709 ⁸⁷
0.812	0.83652 ⁸⁸	0.841	0.86206 ⁸⁸	0.870	0.88748 ⁸⁸	0.899	0.91278 ⁸⁷	0.928	0.93796 ⁸⁶
0.813	0.83740 ⁸⁹	0.842	0.86294 ⁸⁸	0.871	0.88836 ⁸⁷	0.900	0.91365 ⁸⁷	0.929	0.93882 ⁸⁷
0.814	0.83829 ⁸⁸	0.843	0.86382 ⁸⁸	0.872	0.88923 ⁸⁷	0.901	0.91452 ⁸⁷	0.930	0.93969 ⁸⁷
0.815	0.83917 ⁸⁸	0.844	0.86470 ⁸⁸	0.873	0.89010 ⁸⁸	0.902	0.91539 ⁸⁷	0.931	0.94056 ⁸⁶
0.816	0.84005 ⁸⁸	0.845	0.86558 ⁸⁸	0.874	0.89098 ⁸⁷	0.903	0.91626 ⁸⁷	0.932	0.94142 ⁸⁷
0.817	0.84093 ⁸⁹	0.846	0.86646 ⁸⁷	0.875	0.89185 ⁸⁸	0.904	0.91713 ⁸⁷	0.933	0.94229 ⁸⁶
0.818	0.84182 ⁸⁸	0.847	0.86733 ⁸⁸	0.876	0.89273 ⁸⁷	0.905	0.91800 ⁸⁷	0.934	0.94315 ⁸⁷
0.819	0.84270 ⁸⁸	0.848	0.86821 ⁸⁸	0.877	0.89360 ⁸⁷	0.906	0.91887 ⁸⁷	0.935	0.94402 ⁸⁶
0.820	0.84358 ⁸⁸	0.849	0.86909 ⁸⁸	0.878	0.89447 ⁸⁸	0.907	0.91974 ⁸⁷	0.936	0.94488 ⁸⁷
0.821	0.84446 ⁸⁸	0.850	0.86997 ⁸⁷	0.879	0.89535 ⁸⁷	0.908	0.92061 ⁸⁷	0.937	0.94575 ⁸⁷
0.822	0.84534 ⁸⁸	0.851	0.87084 ⁸⁸	0.880	0.89622 ⁸⁷	0.909	0.92148 ⁸⁶	0.938	0.94662 ⁸⁶
0.823	0.84622 ⁸⁹	0.852	0.87172 ⁸⁸	0.881	0.89709 ⁸⁷	0.910	0.92234 ⁸⁷	0.939	0.94748 ⁸⁷
0.824	0.84711 ⁸⁸	0.853	0.87260 ⁸⁷	0.882	0.89796 ⁸⁸	0.911	0.92321 ⁸⁷	0.940	0.94835 ⁸⁶
0.825	0.84799 ⁸⁸	0.854	0.87347 ⁸⁸	0.883	0.89884 ⁸⁷	0.912	0.92408 ⁸⁷	0.941	0.94921 ⁸⁶
0.826	0.84887 ⁸⁸	0.855	0.87435 ⁸⁸	0.884	0.89971 ⁸⁷	0.913	0.92495 ⁸⁷	0.942	0.95007 ⁸⁷
0.827	0.84975 ⁸⁸	0.856	0.87523 ⁸⁷	0.885	0.90058 ⁸⁷	0.914	0.92582 ⁸⁷	0.943	0.95094 ⁸⁶
0.828	0.85063	0.857	0.87610	0.886	0.90145	0.915	0.92669	0.944	0.95180

TABLE 3—contd.

P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$
0.945	0.95267 ⁸⁷	0.974	0.97767 ⁸⁶	1.003	1.00257 ⁸⁶	1.032	1.02737 ⁸⁶	1.061	1.05206 ⁸⁵
0.946	0.95353 ⁸⁶	0.975	0.97853 ⁸⁶	1.004	1.00343 ⁸⁶	1.033	1.02822 ⁸⁵	1.062	1.05291 ⁸⁵
0.947	0.95439 ⁸⁶	0.976	0.97939 ⁸⁶	1.005	1.00428 ⁸⁵	1.034	1.02907 ⁸⁵	1.063	1.05376 ⁸⁵
0.948	0.95526 ⁸⁷	0.977	0.98025 ⁸⁶	1.006	1.00514 ⁸⁶	1.035	1.02992 ⁸⁵	1.064	1.05461 ⁸⁵
0.949	0.95612 ⁸⁶	0.978	0.98111 ⁸⁶	1.007	1.00600 ⁸⁶	1.036	1.03078 ⁸⁶	1.065	1.05546 ⁸⁵
0.950	0.95699 ⁸⁷	0.979	0.98197 ⁸⁶	1.008	1.00685 ⁸⁵	1.037	1.03163 ⁸⁵	1.066	1.05631 ⁸⁵
0.951	0.95785 ⁸⁶	0.980	0.98283 ⁸⁶	1.009	1.00771 ⁸⁶	1.038	1.03248 ⁸⁵	1.067	1.05716 ⁸⁵
0.952	0.95871 ⁸⁶	0.981	0.98369 ⁸⁶	1.010	1.00857 ⁸⁶	1.039	1.03334 ⁸⁶	1.068	1.05801 ⁸⁵
0.953	0.95958 ⁸⁷	0.982	0.98455 ⁸⁶	1.011	1.00942 ⁸⁵	1.040	1.03419 ⁸⁵	1.069	1.05886 ⁸⁵
0.954	0.96044 ⁸⁶	0.983	0.98541 ⁸⁶	1.012	1.01028 ⁸⁶	1.041	1.03504 ⁸⁵	1.070	1.05971 ⁸⁵
0.955	0.96130 ⁸⁶	0.984	0.98627 ⁸⁶	1.013	1.01113 ⁸⁵	1.042	1.03589 ⁸⁵	1.071	1.06056 ⁸⁵
0.956	0.96217 ⁸⁷	0.985	0.98713 ⁸⁶	1.014	1.01199 ⁸⁶	1.043	1.03675 ⁸⁶	1.072	1.06141 ⁸⁵
0.957	0.96303 ⁸⁶	0.986	0.98799 ⁸⁶	1.015	1.01284 ⁸⁵	1.044	1.03760 ⁸⁵	1.073	1.06225 ⁸⁴
0.958	0.96389 ⁸⁶	0.987	0.98885 ⁸⁶	1.016	1.01370 ⁸⁶	1.045	1.03845 ⁸⁵	1.074	1.06310 ⁸⁵
0.959	0.96475 ⁸⁶	0.988	0.98971 ⁸⁶	1.017	1.01455 ⁸⁵	1.046	1.03930 ⁸⁵	1.075	1.06395 ⁸⁵
0.960	0.96562 ⁸⁷	0.989	0.99057 ⁸⁶	1.018	1.01541 ⁸⁶	1.047	1.04015 ⁸⁵	1.076	1.06480 ⁸⁵
0.961	0.96648 ⁸⁶	0.990	0.99142 ⁸⁵	1.019	1.01626 ⁸⁵	1.048	1.04100 ⁸⁵	1.077	1.06565 ⁸⁵
0.962	0.96734 ⁸⁶	0.991	0.99228 ⁸⁶	1.020	1.01712 ⁸⁶	1.049	1.04186 ⁸⁶	1.078	1.06650 ⁸⁵
0.963	0.96820 ⁸⁶	0.992	0.99314 ⁸⁶	1.021	1.01797 ⁸⁵	1.050	1.04271 ⁸⁵	1.079	1.06734 ⁸⁴
0.964	0.96906 ⁸⁶	0.993	0.99400 ⁸⁶	1.022	1.01883 ⁸⁶	1.051	1.04356 ⁸⁵	1.080	1.06819 ⁸⁵
0.965	0.96992 ⁸⁶	0.994	0.99486 ⁸⁶	1.023	1.01968 ⁸⁵	1.052	1.04441 ⁸⁵	1.081	1.06904 ⁸⁵
0.966	0.97079 ⁸⁷	0.995	0.99571 ⁸⁵	1.024	1.02054 ⁸⁶	1.053	1.04526 ⁸⁵	1.082	1.06989 ⁸⁵
0.967	0.97165 ⁸⁶	0.996	0.99657 ⁸⁶	1.025	1.02139 ⁸⁵	1.054	1.04611 ⁸⁵	1.083	1.07073 ⁸⁴
0.968	0.97251 ⁸⁶	0.997	0.99743 ⁸⁶	1.026	1.02224 ⁸⁵	1.055	1.04696 ⁸⁵	1.084	1.07158 ⁸⁵
0.969	0.97337 ⁸⁶	0.998	0.99829 ⁸⁶	1.027	1.02310 ⁸⁶	1.056	1.04781 ⁸⁵	1.085	1.07243 ⁸⁵
0.970	0.97423 ⁸⁶	0.999	0.99914 ⁸⁵	1.028	1.02395 ⁸⁵	1.057	1.04866 ⁸⁵	1.086	1.07328 ⁸⁵
0.971	0.97509 ⁸⁶	1.000	1.00000 ⁸⁶	1.029	1.02481 ⁸⁶	1.058	1.04951 ⁸⁵	1.087	1.07412 ⁸⁴
0.972	0.97595 ⁸⁶	1.001	1.00086 ⁸⁶	1.030	1.02566 ⁸⁵	1.059	1.05036 ⁸⁵	1.088	1.07497 ⁸⁵
0.973	0.97681 ⁸⁶	1.002	1.00171 ⁸⁵	1.031	1.02651 ⁸⁵	1.060	1.05121 ⁸⁵	1.089	1.07582 ⁸⁵

TABLE 3—contd.

P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$	P_1/P_0	$(P_1/P_0)^{6/7}$
1.090	84	1.113	85	1.136	85	1.159	83	1.182	84
1.091	85	1.114	84	1.137	84	1.160	84	1.183	84
1.092	85	1.115	84	1.138	84	1.161	84	1.184	83
1.093	84	1.116	85	1.139	84	1.162	84	1.185	84
1.094	85	1.117	84	1.140	84	1.163	84	1.186	84
1.095	84	1.118	85	1.141	84	1.164	84	1.187	83
1.096	85	1.119	84	1.142	84	1.165	84	1.188	84
1.097	84	1.120	85	1.143	84	1.166	84	1.189	83
1.098	85	1.121	84	1.144	84	1.167	83	1.190	84
1.099	84	1.122	85	1.145	85	1.168	84	1.191	83
1.100	85	1.123	84	1.146	84	1.169	84	1.192	84
1.101	84	1.124	85	1.147	84	1.170	84	1.193	84
1.102	85	1.125	84	1.148	84	1.171	84	1.194	83
1.103	84	1.126	85	1.149	84	1.172	83	1.195	84
1.104	85	1.127	84	1.150	84	1.173	84	1.196	83
1.105	84	1.128	85	1.151	84	1.174	84	1.197	84
1.106	85	1.129	84	1.152	84	1.175	84	1.198	83
1.107	84	1.130	85	1.153	84	1.176	83	1.199	84
1.108	85	1.131	84	1.154	84	1.177	84	1.200	84
1.109	84	1.132	85	1.155	84	1.178	84		
1.110	85	1.133	84	1.156	84	1.179	84		
1.111	84	1.134	85	1.157	84	1.180	83		
1.112	85	1.135	84	1.158	84	1.181	83		

TABLE 4

$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$
0	0								
			51		51		52		53
		0.029	0.01461	0.058	0.02943	0.087	0.04449	0.116	0.05979
	50		50		52		52		53
0.001	0.00050	0.030	0.01511	0.059	0.02995	0.088	0.04501	0.117	0.06032
	50		51		51		53		53
0.002	0.00100	0.031	0.01562	0.060	0.03046	0.089	0.04554	0.118	0.06085
	50		51		52		52		53
0.003	0.00150	0.032	0.01613	0.061	0.03098	0.090	0.04606	0.119	0.06138
	50		51		52		53		54
0.004	0.00200	0.033	0.01664	0.062	0.03150	0.091	0.04659	0.120	0.06192
	50		51		51		52		53
0.005	0.00250	0.034	0.01715	0.063	0.03201	0.092	0.04711	0.121	0.06245
	50		51		52		52		53
0.006	0.00300	0.035	0.01766	0.064	0.03253	0.093	0.04763	0.122	0.06298
	51		50		52		53		54
0.007	0.00351	0.036	0.01816	0.065	0.03305	0.094	0.04816	0.123	0.06352
	50		51		51		53		53
0.008	0.00401	0.037	0.01867	0.066	0.03356	0.095	0.04869	0.124	0.06405
	50		51		52		52		54
0.009	0.00451	0.038	0.01918	0.067	0.03408	0.096	0.04921	0.125	0.06459
	50		51		52		53		53
0.010	0.00501	0.039	0.01969	0.068	0.03460	0.097	0.04974	0.126	0.06512
	51		51		52		52		54
0.011	0.00552	0.040	0.02020	0.069	0.03512	0.098	0.05026	0.127	0.06566
	50		51		51		53		53
0.012	0.00602	0.041	0.02071	0.070	0.03563	0.099	0.05079	0.128	0.06619
	50		52		52		53		54
0.013	0.00652	0.042	0.02123	0.071	0.03615	0.100	0.05132	0.129	0.06673
	50		51		52		52		53
0.014	0.00702	0.043	0.02174	0.072	0.03667	0.101	0.05184	0.130	0.06726
	51		51		52		53		54
0.015	0.00753	0.044	0.02225	0.073	0.03719	0.102	0.05237	0.131	0.06780
	50		51		52		53		53
0.016	0.00803	0.045	0.02276	0.074	0.03771	0.103	0.05290	0.132	0.06833
	51		51		52		53		54
0.017	0.00854	0.046	0.02327	0.075	0.03823	0.104	0.05343	0.133	0.06887
	50		51		52		53		54
0.018	0.00904	0.047	0.02378	0.076	0.03875	0.105	0.05396	0.134	0.06941
	51		52		52		52		54
0.019	0.00955	0.048	0.02430	0.077	0.03927	0.106	0.05448	0.135	0.06995
	50		51		52		53		53
0.020	0.01005	0.049	0.02481	0.078	0.03979	0.107	0.05501	0.136	0.07048
	51		51		52		53		54
0.021	0.01056	0.050	0.02532	0.079	0.04031	0.108	0.05554	0.137	0.07102
	50		51		52		53		54
0.022	0.01106	0.051	0.02583	0.080	0.04083	0.109	0.05607	0.138	0.07156
	51		52		53		53		54
0.023	0.01157	0.052	0.02635	0.081	0.04136	0.110	0.05660	0.139	0.07210
	50		51		52		53		54
0.024	0.01207	0.053	0.02686	0.082	0.04188	0.111	0.05713	0.140	0.07264
	51		51		52		53		54
0.025	0.01258	0.054	0.02737	0.083	0.04240	0.112	0.05766	0.141	0.07318
	51		52		52		53		54
0.026	0.01309	0.055	0.02789	0.084	0.04292	0.113	0.05819	0.142	0.07372
	50		51		52		53		54
0.027	0.01359	0.056	0.02840	0.085	0.04344	0.114	0.05872	0.143	0.07426
	51		52		53		54		54
0.028	0.01410	0.057	0.02892	0.086	0.04397	0.115	0.05926	0.144	0.07480

TABLE 4—*contd.*

$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$
	54		55		56		57		58
0.145	0.07534	0.174	0.09115	0.203	0.10725	0.232	0.12364	0.261	0.14035
	54		55		56		57		58
0.146	0.07588	0.175	0.09170	0.204	0.10781	0.233	0.12421	0.262	0.14093
	54		56		56		58		58
0.147	0.07642	0.176	0.09226	0.205	0.10837	0.234	0.12479	0.263	0.14151
	54		55		56		57		59
0.148	0.07696	0.177	0.09281	0.206	0.10893	0.235	0.12556	0.264	0.14210
	54		55		56		57		58
0.149	0.07750	0.178	0.09336	0.207	0.10949	0.236	0.12593	0.265	0.14268
	55		55		57		57		58
0.150	0.07805	0.179	0.09391	0.208	0.11006	0.237	0.12650	0.266	0.14326
	54		55		56		57		59
0.151	0.07859	0.180	0.09446	0.209	0.11062	0.238	0.12707	0.267	0.14385
	54		55		56		58		58
0.152	0.07913	0.181	0.09501	0.210	0.11118	0.239	0.12765	0.268	0.14443
	54		56		56		57		58
0.153	0.07967	0.182	0.09557	0.211	0.11174	0.240	0.12822	0.269	0.14501
	55		55		57		57		59
0.154	0.08022	0.183	0.09612	0.212	0.11231	0.241	0.12879	0.270	0.14560
	54		55		56		58		59
0.155	0.08076	0.184	0.09667	0.213	0.11287	0.242	0.12937	0.271	0.14619
	55		56		56		57		58
0.156	0.08131	0.185	0.09723	0.214	0.11343	0.243	0.12994	0.272	0.14677
	54		55		57		58		59
0.157	0.08185	0.186	0.09778	0.215	0.11400	0.244	0.13052	0.273	0.14736
	54		55		56		57		58
0.158	0.08239	0.187	0.09833	0.216	0.11456	0.245	0.13109	0.274	0.14794
	55		56		57		58		59
0.159	0.08294	0.188	0.09889	0.217	0.11513	0.246	0.13167	0.275	0.14853
	54		55		56		57		59
0.160	0.08348	0.189	0.09944	0.218	0.11569	0.247	0.13224	0.276	0.14912
	55		56		57		58		59
0.161	0.08403	0.190	0.10000	0.219	0.11626	0.248	0.13282	0.277	0.14971
	55		56		56		58		58
0.162	0.08458	0.191	0.10056	0.220	0.11682	0.249	0.13340	0.278	0.15029
	54		55		57		57		59
0.163	0.08512	0.192	0.10111	0.221	0.11739	0.250	0.13397	0.279	0.15088
	55		56		57		58		59
0.164	0.08567	0.193	0.10167	0.222	0.11796	0.251	0.13455	0.280	0.15147
	55		55		56		58		59
0.165	0.08622	0.194	0.10222	0.223	0.11852	0.252	0.13513	0.281	0.15206
	54		56		57		58		59
0.166	0.08676	0.195	0.10278	0.224	0.11909	0.253	0.13571	0.282	0.15265
	55		56		57		58		59
0.167	0.08731	0.196	0.10334	0.225	0.11966	0.254	0.13629	0.283	0.15324
	55		56		57		58		59
0.168	0.08786	0.197	0.10390	0.226	0.12023	0.255	0.13687	0.284	0.15383
	55		56		57		58		59
0.169	0.08841	0.198	0.10446	0.227	0.12080	0.256	0.13745	0.285	0.15442
	55		55		56		58		59
0.170	0.08896	0.199	0.10501	0.228	0.12136	0.257	0.13803	0.286	0.15501
	55		56		57		58		60
0.171	0.08951	0.200	0.10557	0.229	0.12193	0.258	0.13861	0.287	0.15561
	54		56		57		58		59
0.172	0.09005	0.201	0.10613	0.230	0.12250	0.259	0.13919	0.288	0.15620
	55		56		57		58		59
0.173	0.09060	0.202	0.10669	0.231	0.12307	0.260	0.13977	0.289	0.15679

TABLE 4—*contd.*

$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$
0.290	0.15739 ⁶⁰	0.319	0.17477 ⁶⁰	0.348	0.19253 ⁶¹	0.377	0.21070 ⁶⁴	0.406	0.22929 ⁶⁵
0.291	0.15788 ⁵⁹	0.320	0.17538 ⁶¹	0.349	0.19315 ⁶²	0.378	0.21133 ⁶³	0.407	0.22994 ⁶⁵
0.292	0.15857 ⁵⁹	0.321	0.17599 ⁶¹	0.350	0.19377 ⁶²	0.379	0.21196 ⁶³	0.408	0.23058 ⁶⁴
0.293	0.15917 ⁶⁰	0.322	0.17659 ⁶⁰	0.351	0.19439 ⁶²	0.380	0.21260 ⁶⁴	0.409	0.23123 ⁶⁵
0.294	0.15976 ⁵⁹	0.323	0.17720 ⁶¹	0.352	0.19502 ⁶³	0.381	0.21323 ⁶³	0.410	0.23189 ⁶⁶
0.295	0.16036 ⁶⁰	0.324	0.17781 ⁶¹	0.353	0.19564 ⁶²	0.382	0.21387 ⁶⁴	0.411	0.23254 ⁶⁵
0.296	0.16095 ⁵⁹	0.325	0.17842 ⁶¹	0.354	0.19626 ⁶²	0.383	0.21451 ⁶⁴	0.412	0.23319 ⁶⁵
0.297	0.16155 ⁶⁰	0.326	0.17902 ⁶⁰	0.355	0.19688 ⁶²	0.384	0.21514 ⁶³	0.413	0.23384 ⁶⁵
0.298	0.16215 ⁶⁰	0.327	0.17963 ⁶¹	0.356	0.19750 ⁶²	0.385	0.21578 ⁶⁴	0.414	0.23449 ⁶⁵
0.299	0.16274 ⁵⁹	0.328	0.18024 ⁶¹	0.357	0.19813 ⁶³	0.386	0.21642 ⁶⁴	0.415	0.23515 ⁶⁶
0.300	0.16334 ⁶⁰	0.329	0.18085 ⁶¹	0.358	0.19875 ⁶²	0.387	0.21706 ⁶⁴	0.416	0.23580 ⁶⁵
0.301	0.16394 ⁶⁰	0.330	0.18146 ⁶¹	0.359	0.19938 ⁶³	0.388	0.21770 ⁶⁴	0.417	0.23646 ⁶⁶
0.302	0.16454 ⁶⁰	0.331	0.18208 ⁶²	0.360	0.20000 ⁶²	0.389	0.21834 ⁶⁴	0.418	0.23711 ⁶⁵
0.303	0.16513 ⁵⁹	0.332	0.18269 ⁶¹	0.361	0.20063 ⁶³	0.390	0.21898 ⁶⁴	0.419	0.23777 ⁶⁶
0.304	0.16573 ⁶⁰	0.333	0.18330 ⁶¹	0.362	0.20125 ⁶²	0.391	0.21962 ⁶⁴	0.420	0.23842 ⁶⁵
0.305	0.16633 ⁶⁰	0.334	0.18391 ⁶¹	0.363	0.20188 ⁶³	0.392	0.22026 ⁶⁴	0.421	0.23908 ⁶⁶
0.306	0.16693 ⁶⁰	0.335	0.18452 ⁶¹	0.364	0.20250 ⁶²	0.393	0.22090 ⁶⁴	0.422	0.23974 ⁶⁵
0.307	0.16753 ⁶⁰	0.336	0.18514 ⁶²	0.365	0.20313 ⁶³	0.394	0.22154 ⁶⁴	0.423	0.24039 ⁶⁵
0.308	0.16813 ⁶⁰	0.337	0.18575 ⁶¹	0.366	0.20376 ⁶³	0.395	0.22218 ⁶⁴	0.424	0.24105 ⁶⁶
0.309	0.16874 ⁶¹	0.338	0.18637 ⁶²	0.367	0.20439 ⁶³	0.396	0.22283 ⁶⁵	0.425	0.24171 ⁶⁶
0.310	0.16934 ⁶⁰	0.339	0.18698 ⁶¹	0.368	0.20502 ⁶³	0.397	0.22347 ⁶⁴	0.426	0.24237 ⁶⁶
0.311	0.16994 ⁶⁰	0.340	0.18760 ⁶²	0.369	0.20564 ⁶²	0.398	0.22411 ⁶⁴	0.427	0.24303 ⁶⁶
0.312	0.17054 ⁶⁰	0.341	0.18821 ⁶¹	0.370	0.20627 ⁶³	0.399	0.22476 ⁶⁵	0.428	0.24369 ⁶⁶
0.313	0.17115 ⁶¹	0.342	0.18883 ⁶²	0.371	0.20690 ⁶³	0.400	0.22540 ⁶⁴	0.429	0.24435 ⁶⁶
0.314	0.17175 ⁶⁰	0.343	0.18944 ⁶¹	0.372	0.20754 ⁶⁴	0.401	0.22605 ⁶⁵	0.430	0.24502 ⁶⁷
0.315	0.17235 ⁶⁰	0.344	0.19006 ⁶²	0.373	0.20817 ⁶³	0.402	0.22670 ⁶⁵	0.431	0.24568 ⁶⁶
0.316	0.17296 ⁶¹	0.345	0.19068 ⁶²	0.374	0.20880 ⁶³	0.403	0.22734 ⁶⁴	0.432	0.24634 ⁶⁶
0.317	0.17356 ⁶⁰	0.346	0.19130 ⁶²	0.375	0.20943 ⁶³	0.404	0.22799 ⁶⁵	0.433	0.24701 ⁶⁷
0.318	0.17417 ⁶¹	0.347	0.19192 ⁶²	0.376	0.21006 ⁶³	0.405	0.22864 ⁶⁵	0.434	0.24767 ⁶⁶

TABLE 4—*contd.*

$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$	$x,$	$1-(1-x)^{1/2}$
0.435	0.24834 ⁶⁷	0.449	0.25771 ⁶⁸	0.463	0.26720 ⁶⁸	0.477	0.27681 ⁶⁹	0.491	0.28656 ⁷⁰
0.436	0.24900 ⁶⁶	0.450	0.25838 ⁶⁷	0.464	0.26788 ⁶⁸	0.478	0.27750 ⁶⁹	0.492	0.28726 ⁷⁰
0.437	0.24967 ⁶⁷	0.451	0.25905 ⁶⁷	0.465	0.26856 ⁶⁸	0.479	0.27820 ⁷⁰	0.493	0.28796 ⁷⁰
0.438	0.25033 ⁶⁶	0.452	0.25973 ⁶⁸	0.466	0.26925 ⁶⁹	0.480	0.27889 ⁶⁹	0.494	0.28866 ⁷⁰
0.439	0.25100 ⁶⁷	0.453	0.26041 ⁶⁸	0.467	0.26993 ⁶⁸	0.481	0.27958 ⁶⁹	0.495	0.28937 ⁷¹
0.440	0.25167 ⁶⁷	0.454	0.26108 ⁶⁷	0.468	0.27062 ⁶⁹	0.482	0.28028 ⁷⁰	0.496	0.29007 ⁷⁰
0.441	0.25234 ⁶⁷	0.455	0.26176 ⁶⁸	0.469	0.27130 ⁶⁸	0.483	0.28097 ⁶⁹	0.497	0.29078 ⁷¹
0.442	0.25301 ⁶⁷	0.456	0.26244 ⁶⁸	0.470	0.27199 ⁶⁹	0.484	0.28167 ⁷⁰	0.498	0.29148 ⁷⁰
0.443	0.25368 ⁶⁷	0.457	0.26311 ⁶⁷	0.471	0.27268 ⁶⁹	0.485	0.28236 ⁶⁹	0.499	0.29219 ⁷¹
0.444	0.25435 ⁶⁷	0.458	0.26379 ⁶⁸	0.472	0.27336 ⁶⁸	0.486	0.28306 ⁷⁰	0.500	0.29289 ⁷⁰
0.445	0.25502 ⁶⁷	0.459	0.26447 ⁶⁸	0.473	0.27405 ⁶⁹	0.487	0.28376 ⁷⁰		
0.446	0.25569 ⁶⁷	0.460	0.26515 ⁶⁸	0.744	0.27474 ⁶⁹	0.488	0.28446 ⁷⁰		
0.447	0.25636 ⁶⁷	0.461	0.26583 ⁶⁹	0.475	0.27543 ⁶⁹	0.489	0.28516 ⁷⁰		
0.448	0.25703	0.462	0.26652	0.476	0.27612	0.490	0.28586		

TABLE 4a

Table of Proportional Parts for Use with Table 4

	$\times 0.1$	$\times 0.2$	$\times 0.3$	$\times 0.4$	$\times 0.5$	$\times 0.6$	$\times 0.7$	$\times 0.8$	$\times 0.9$
50	-5	10	15	20	25	30	35	40	45
51	5	10	15	20	25 ₅	31	36	41	46
52	5	10	16	21	26	31	36	42	47
53	5	11	16	21	26 ₅	32	37	42	48
54	5	11	16	22	27	32	38	43	49
55	5 ₅	11	16 ₅	22	27 ₅	33	38 ₅	44	49 ₅
56	6	11	17	22	28	34	39	45	50
57	6	11	17	23	28 ₅	34	40	46	51
58	6	12	17	23	29	35	41	46	52
59	6	12	18	24	29 ₅	35	41	47	53
60	6	12	18	24	30	36	42	48	54
61	6	12	18	24	30 ₅	37	43	49	55
62	6	12	19	25	31	37	43	50	56
63	6	13	19	25	31 ₅	38	44	51	57
64	6	13	19	26	32	38	45	52	58
65	6 ₅	13	19 ₅	26	32 ₅	39	45 ₅	53	58 ₅
66	7	13	20	26	33	40	46	54	59
67	7	13	20	27	33 ₅	40	47	54	60
68	7	14	20	27	34	41	48	54	61
69	7	14	21	28	34 ₅	41	48	55	62
70	7	14	21	28	35	42	49	56	63
71	7	14	21	28	35 ₅	43	50	57	64

TABLE 5

$\frac{H_0 - p_0}{p_0}$	M_0	$\frac{H_0 - p_0}{p_0}$	M_0	$\frac{H_0 - p_0}{p_0}$	M_0	$\frac{H_0 - p_0}{p_0}$	M_0	$\frac{H_0 - p_0}{p_0}$	M_0	$\frac{H_0 - p_0}{p_0}$	M_0
0	0	0.055	0.278	0.110	0.389	0.218	0.538	0.365	0.682	0.640	0.871
0.001	0.038	0.056	0.280			0.220	0.541	0.370	0.686	0.645	0.874
0.002	0.053	0.057	0.282 ₅	0.112	0.392	0.222	0.543	0.375	0.690	0.650	0.877
0.003	0.065	0.058	0.285	0.114	0.396	0.224	0.545	0.380	0.694	0.655	0.880
0.004	0.075	0.059	0.287	0.116	0.399	0.226	0.547 ₅	0.385	0.698	0.660	0.883
0.005	0.084	0.060	0.290	0.118	0.402	0.228	0.550	0.390	0.702	0.665	0.885
0.006	0.092	0.061	0.292	0.120	0.406	0.230	0.552	0.395	0.706	0.670	0.888
0.007	0.100	0.062	0.294	0.122	0.409	0.232	0.554	0.400	0.710	0.675	0.891
0.008	0.107	0.063	0.297	0.124	0.412	0.234	0.556	0.405	0.714	0.680	0.894
0.009	0.113	0.064	0.299	0.126	0.415	0.236	0.559	0.410	0.718	0.685	0.897
0.010	0.119	0.065	0.301	0.128	0.418	0.238	0.561	0.415	0.722	0.690	0.899
0.011	0.125	0.066	0.304	0.130	0.421 ₅	0.240	0.563	0.420	0.726	0.695	0.902
0.012	0.131	0.067	0.306	0.132	0.425	0.242	0.565	0.425	0.730	0.700	0.905
0.013	0.136	0.068	0.308	0.134	0.428	0.244	0.567	0.430	0.733 ₅	0.705	0.907
0.014	0.141	0.069	0.310	0.136	0.431	0.246	0.569 ₅	0.435	0.737	0.710	0.910
0.015	0.146	0.070	0.312	0.138	0.434	0.248	0.572	0.440	0.741	0.715	0.913
0.016	0.151	0.071	0.315	0.140	0.437	0.250	0.574	0.445	0.745	0.720	0.915
0.017	0.155	0.072	0.317	0.142	0.440	0.252	0.576	0.450	0.748	0.725	0.918
0.018	0.160	0.073	0.319	0.144	0.443	0.254	0.578	0.455	0.752	0.730	0.921
0.019	0.164	0.074	0.321	0.146	0.446	0.256	0.580	0.460	0.756	0.735	0.923
0.020	0.168	0.075	0.323	0.148	0.448 ₅	0.258	0.582	0.465	0.759	0.740	0.926
0.021	0.173	0.076	0.325	0.150	0.451	0.260	0.584	0.470	0.763	0.745	0.928
0.022	0.177	0.077	0.327	0.152	0.454	0.262	0.586	0.475	0.766	0.750	0.931
0.023	0.181	0.078	0.329	0.154	0.457	0.264	0.588	0.480	0.770	0.755	0.934
0.024	0.184	0.079	0.331	0.156	0.460	0.266	0.590	0.485	0.773	0.760	0.936
0.025	0.188	0.080	0.333	0.158	0.463	0.268	0.592	0.490	0.777	0.765	0.939
0.026	0.192	0.081	0.335	0.160	0.465	0.270	0.594	0.495	0.780	0.770	0.941
0.027	0.195	0.082	0.337	0.162	0.468	0.272	0.596 ₅	0.500	0.784	0.775	0.944
0.028	0.199	0.083	0.339	0.164	0.471	0.274	0.598 ₅	0.505	0.787	0.780	0.946
0.029	0.202	0.084	0.341	0.166	0.474	0.276	0.600 ₅	0.510	0.790	0.785	0.949
0.030	0.206	0.085	0.343	0.168	0.476	0.278	0.602 ₅	0.515	0.794	0.790	0.951
0.031	0.209	0.086	0.345	0.170	0.479	0.280	0.604 ₅	0.520	0.797	0.795	0.954
0.032	0.213	0.087	0.347	0.172	0.482	0.282	0.606 ₅	0.525	0.800 ₅	0.800	0.956
0.033	0.216	0.088	0.349	0.174	0.484	0.284	0.608 ₅	0.530	0.804	0.805	0.959
0.034	0.219	0.089	0.351	0.176	0.487	0.286	0.610	0.535	0.807	0.810	0.961
0.035	0.222	0.090	0.353	0.178	0.489 ₅	0.288	0.612	0.540	0.810	0.815	0.964
0.036	0.225	0.091	0.355	0.180	0.492	0.290	0.614	0.545	0.813	0.820	0.966
0.037	0.228	0.092	0.357	0.182	0.495	0.292	0.616	0.550	0.817	0.825	0.968
0.038	0.231	0.093	0.359	0.184	0.497	0.294	0.618	0.555	0.820	0.830	0.971
0.039	0.234	0.094	0.361	0.186	0.500	0.296	0.620	0.560	0.823	0.835	0.973
0.040	0.237	0.095	0.362	0.188	0.502	0.298	0.622	0.565	0.826	0.840	0.975
0.041	0.240	0.096	0.364	0.190	0.505	0.300	0.624	0.570	0.829	0.845	0.978
0.042	0.243	0.097	0.366	0.192	0.507			0.575	0.832	0.850	0.980
0.043	0.246	0.098	0.368	0.194	0.510	0.305	0.629	0.580	0.836	0.855	0.983
0.044	0.249	0.099	0.370	0.196	0.512	0.310	0.633	0.585	0.839	0.860	0.985
0.045	0.252	0.100	0.371 ₅	0.198	0.515	0.315	0.638	0.590	0.842	0.865	0.987
0.046	0.254	0.101	0.373 ₅	0.200	0.517	0.320	0.642 ₅	0.595	0.845	0.870	0.990
0.047	0.257	0.102	0.375	0.202	0.519 ₅	0.325	0.647	0.600	0.848	0.875	0.992
0.048	0.260	0.103	0.377	0.204	0.522	0.330	0.651 ₅	0.605	0.851	0.880	0.994
0.049	0.262	0.104	0.379	0.206	0.525	0.335	0.656	0.610	0.854	0.885	0.996
0.050	0.265	0.105	0.380	0.203	0.527	0.340	0.660	0.615	0.857	0.890	0.999
0.051	0.267 ₅	0.106	0.382	0.210	0.529	0.345	0.665	0.620	0.860	0.895	1.001
0.052	0.270	0.107	0.384	0.212	0.531	0.350	0.669	0.625	0.863		
0.053	0.273	0.108	0.386	0.214	0.534	0.355	0.673	0.630	0.865 ₅		
0.054	0.275	0.109	0.387	0.216	0.536	0.360	0.678	0.635	0.868		

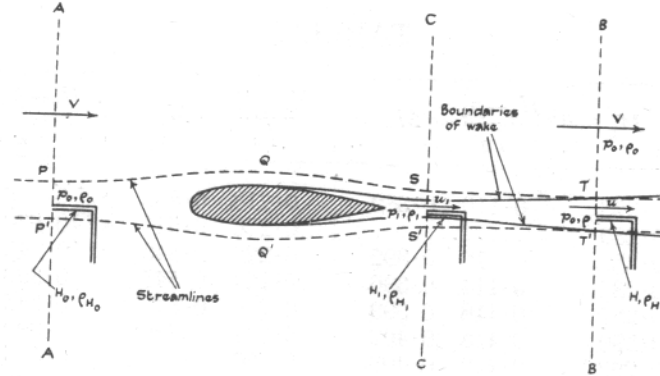


FIG. 1.—Steady Flow of a Compressible Fluid past an Aerofoil.

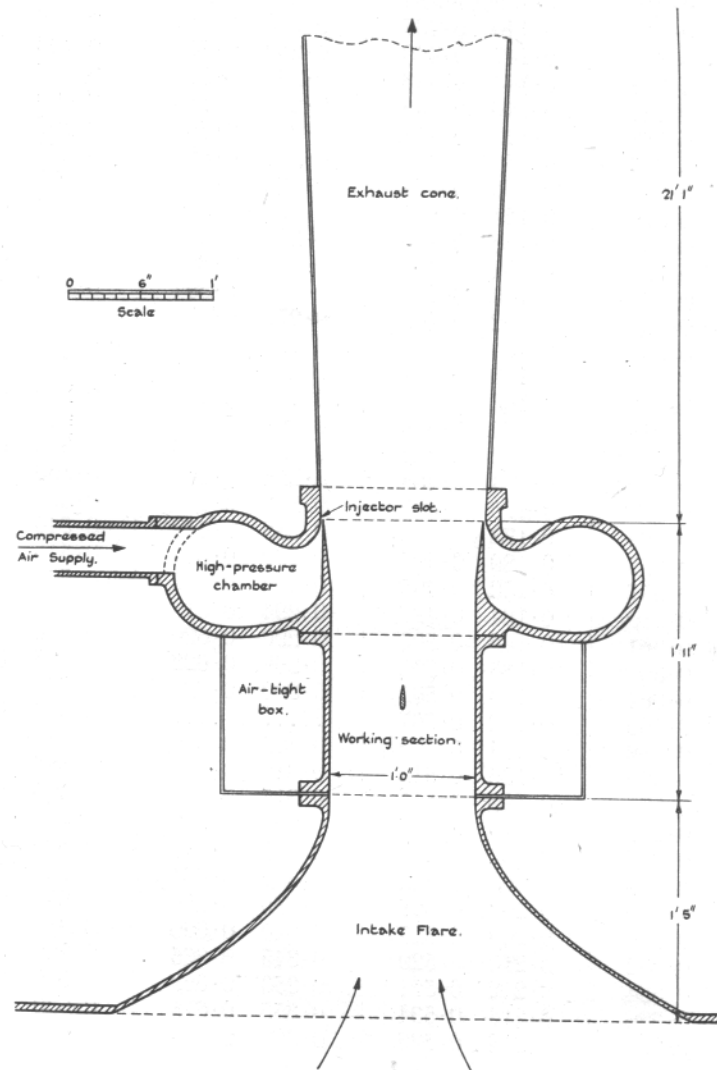


FIG. 2.—High-Speed Wind Tunnel.

35

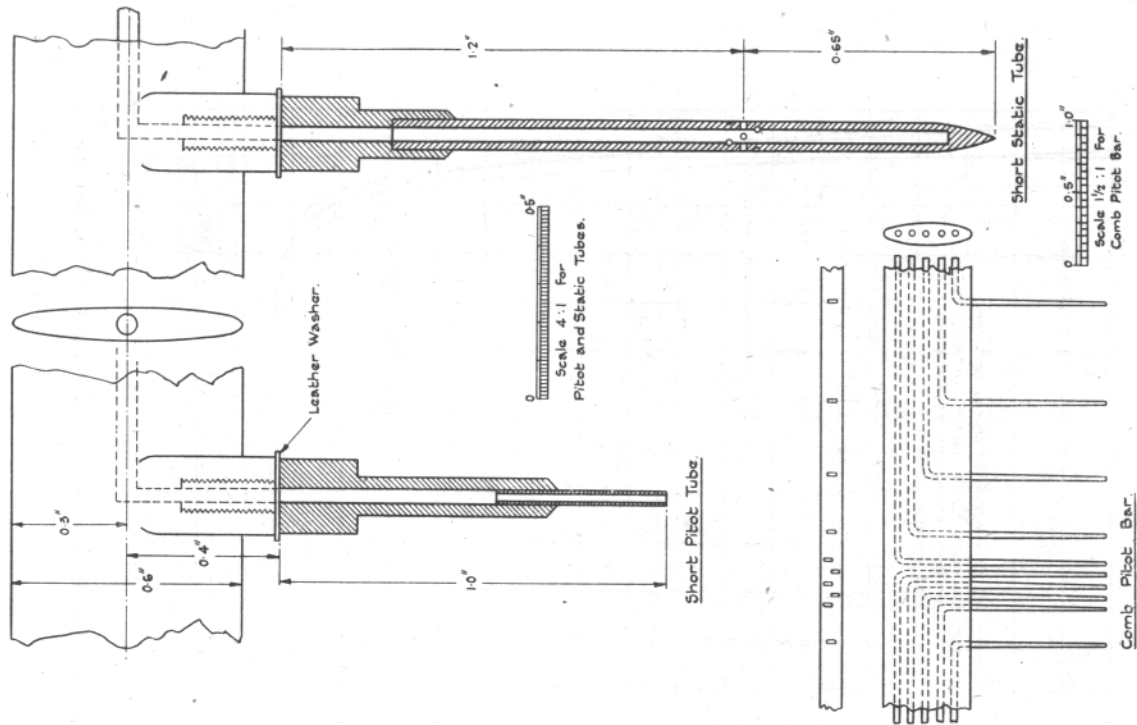


FIG. 4.

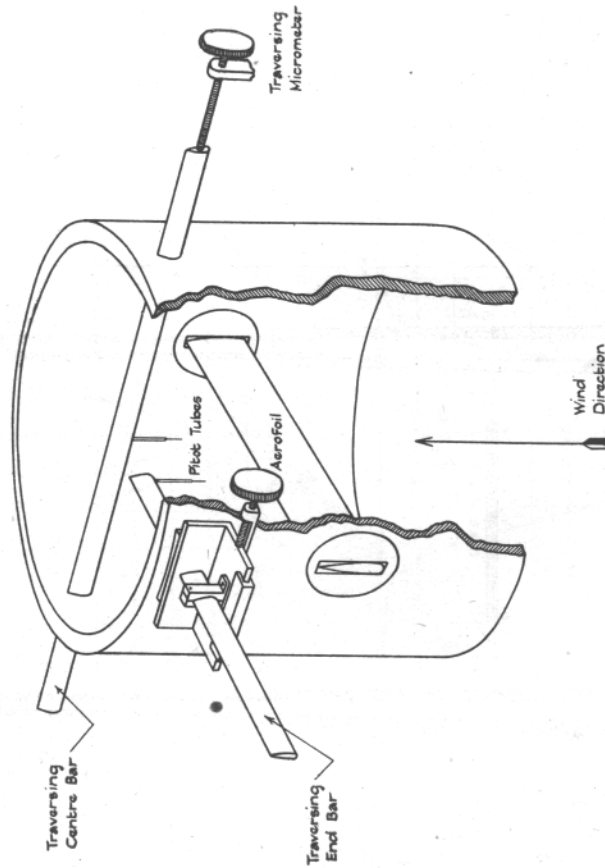


FIG. 3.—Diagrammatic Arrangement of Traversing Bars in the High-Speed Tunnel.

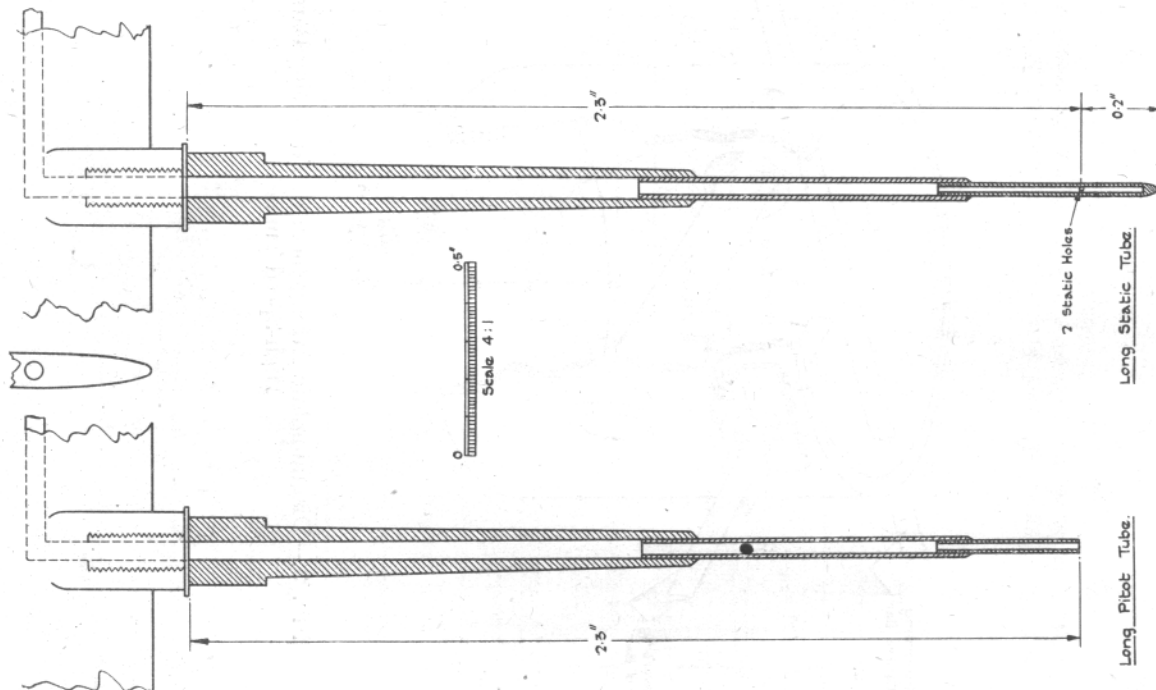


FIG. 5.

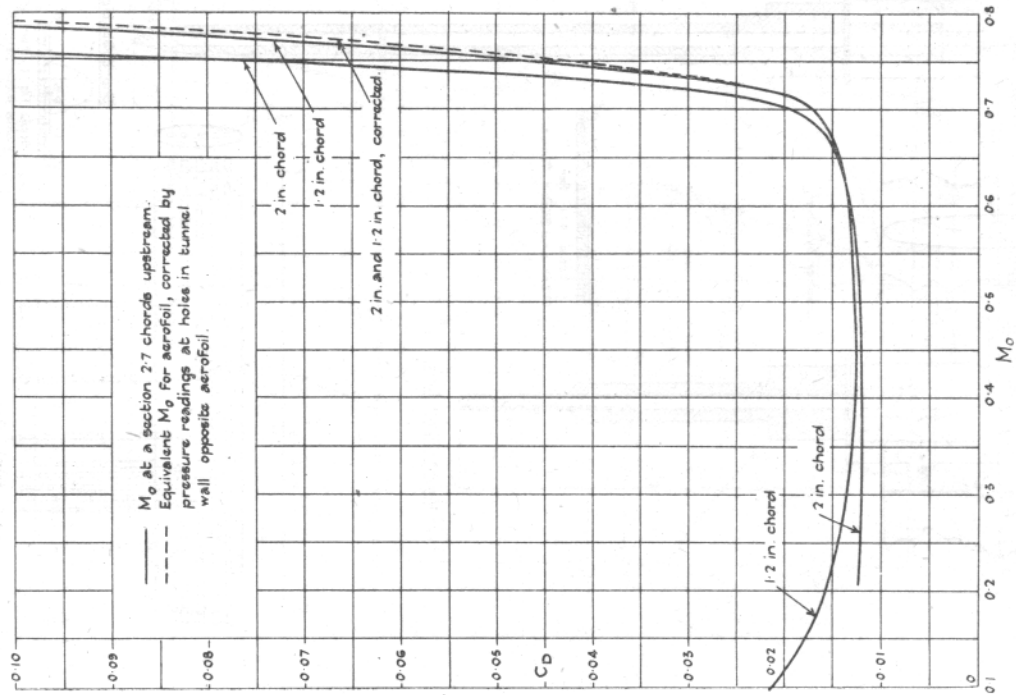


FIG. 6.—Correction to Speed for Tunnel Interference.

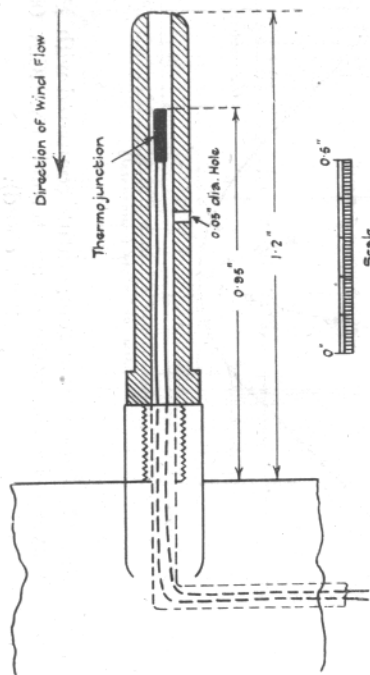


FIG. 8.—Pitot Thermocouple.

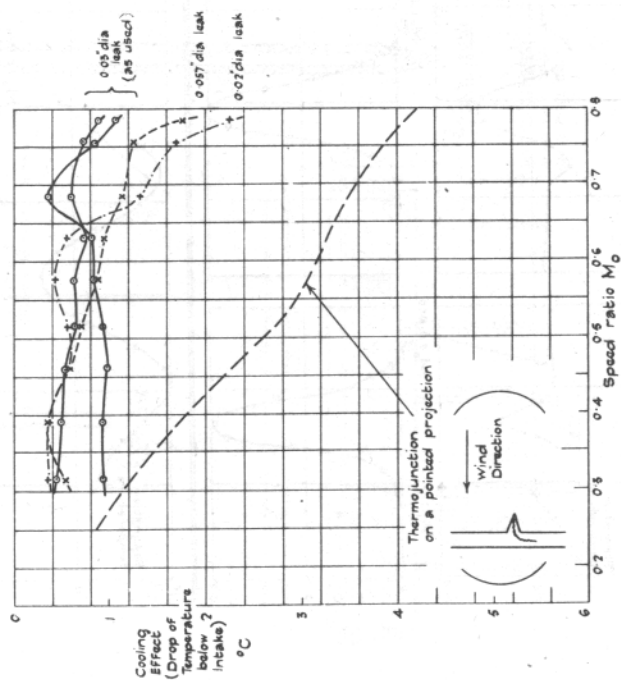


FIG. 9.—Empty Tunnel Calibration of Thermocouples.

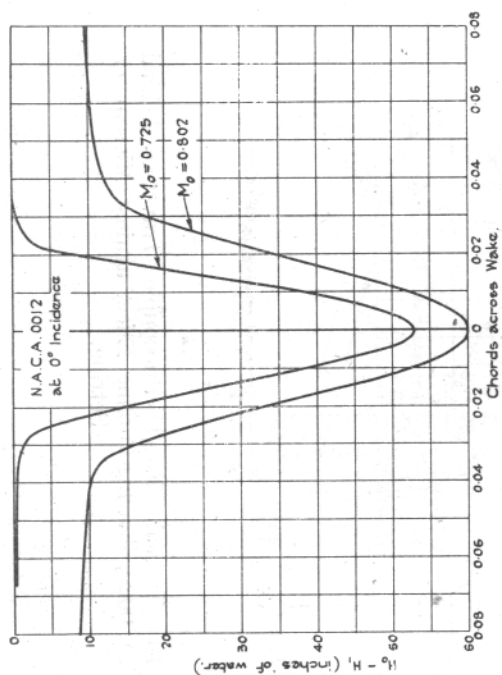


FIG. 7a.

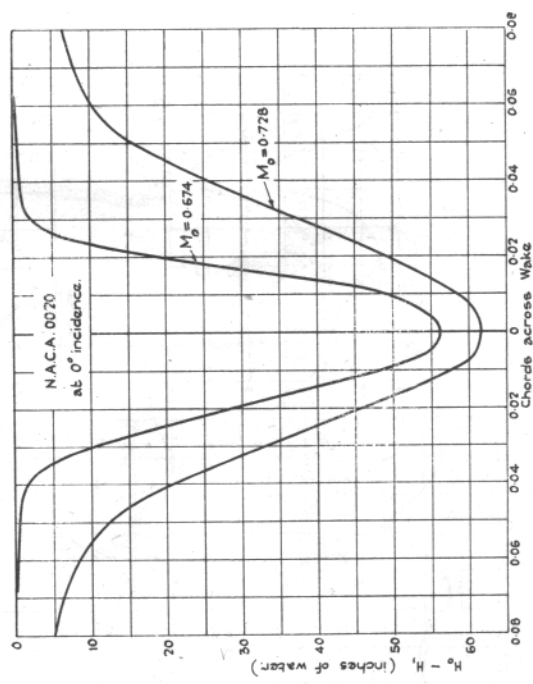


FIG. 7b.—Traverses above and below the Shock Stalling Speed.
 (0.2 chords behind the trailing edge.)

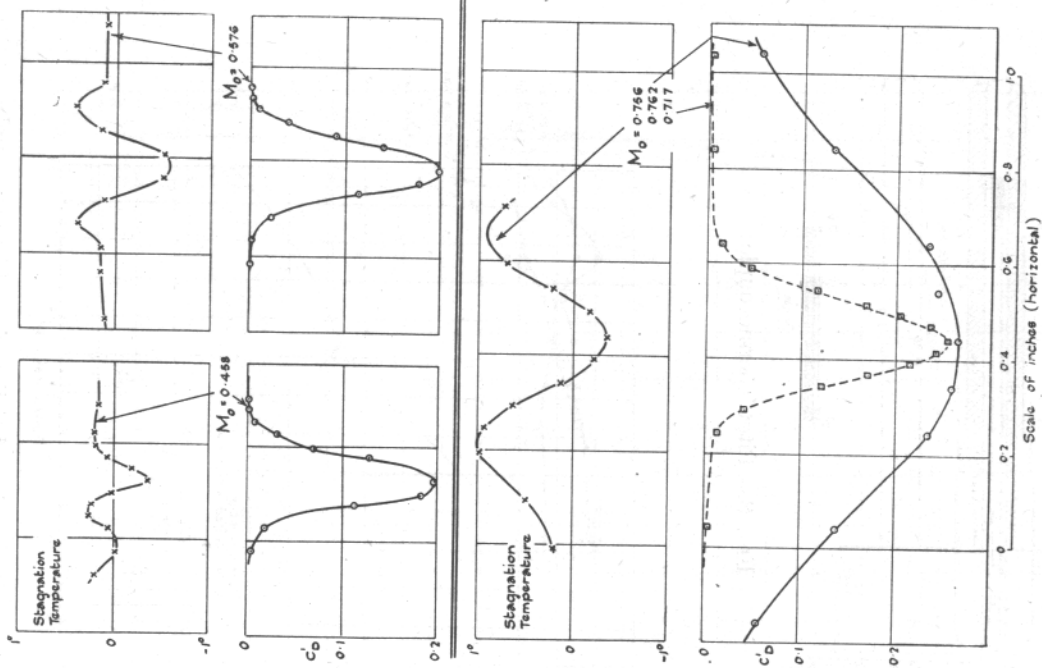


FIG. 11.—Stagnation Temperature compared with Pitot Traverse in the wake of an Aerofoil (N.A.C.A. 0020, 2-in. chord).

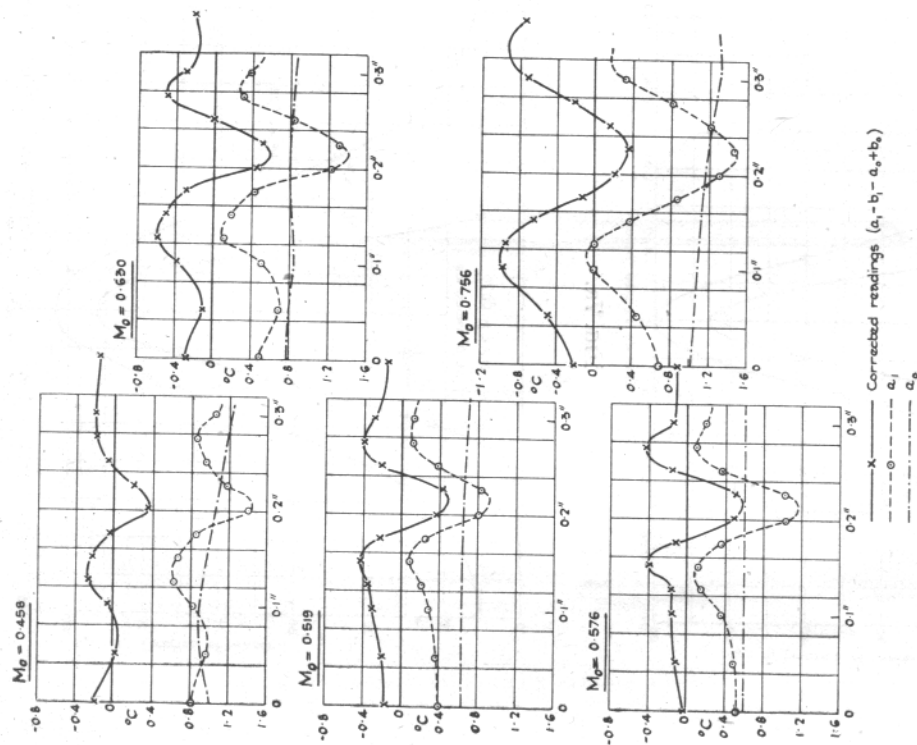


FIG. 10.—Typical Pitot-Thermocouple Traverses behind N.A.C.A. 0020, showing Cooling Effect against Micrometer Setting.

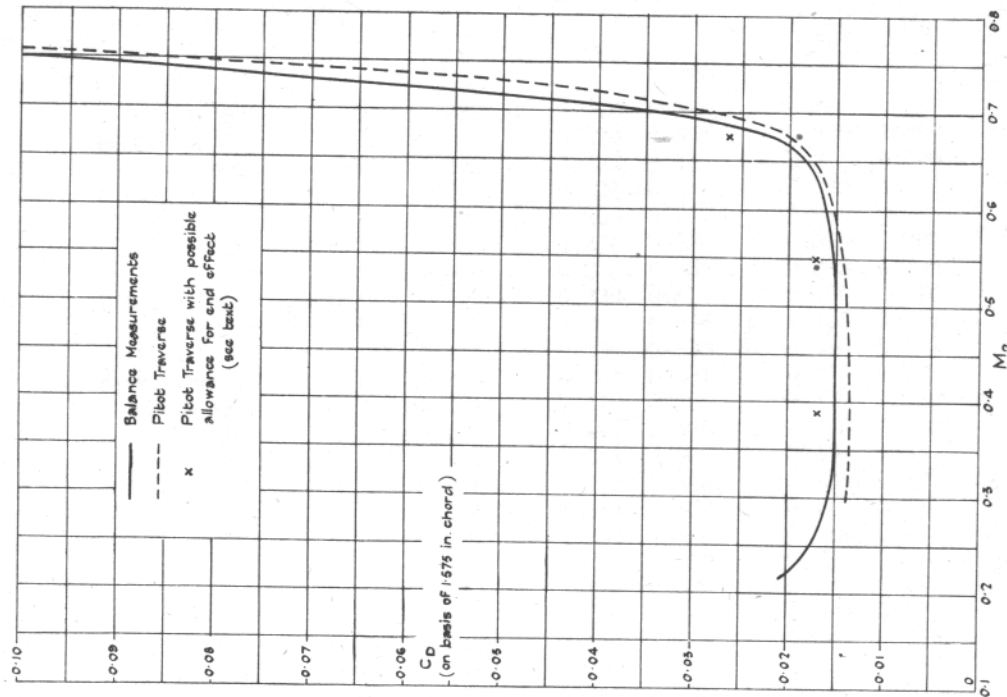


FIG. 13.—Comparison with Balance for a Tapered Aerofoil at 0° Incidence.

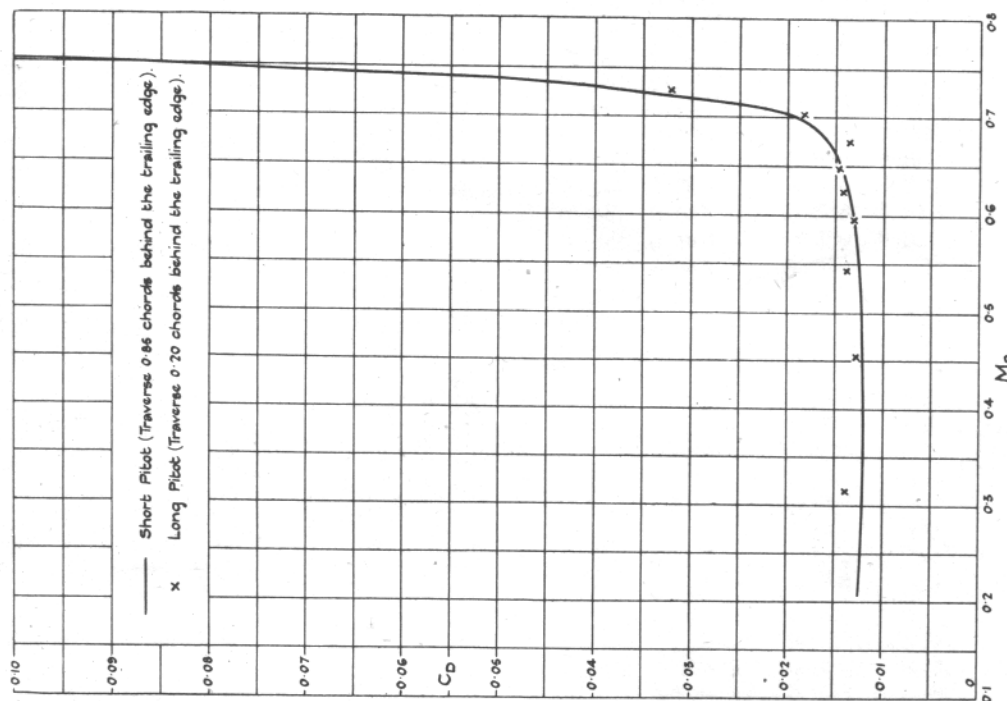


FIG. 12.—Drag Coefficient of N.A.C.A. 0020 (2-in. chord) at 0° Incidence deduced from Traverses at two Distances behind the Trailing Edge.

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